

# 1 Halogen-Specific Total Organic Halogen Analysis: Assessment by Recovery of Total 2 Bromine

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15

16 **Abstract:** Determination of halogen-specific total organic halogen (TOX) is vital for  
17 studies of disinfection of waters containing bromide, since total organic bromine (TOBr) is  
18 likely to be more problematic than total organic chlorine. Here, we present further halogen-  
19 specific TOX method optimisation and validation, focusing on measurement of TOBr. The  
20 optimised halogen-specific TOX method was validated based on the recovery of model  
21 compounds covering different classes of disinfection by-products (haloacetic acids,  
22 haloacetonitriles, halophenols and halogenated benzenes) and the recovery of total bromine  
23 (mass balance of TOBr and bromide concentrations) during disinfection of waters containing  
24 dissolved organic matter and bromide. The validation of a halogen-specific TOX method  
25 based on the mass balance of total bromine has not previously been reported. Very good  
26 recoveries of organic halogen from all model compounds were obtained, indicating high or  
27 complete conversion of all organic halogen in the model compound solution through to halide  
28 in the absorber solution for ion chromatography analysis. The method was also successfully  
29 applied to monitor conversion of bromide to TOBr in a groundwater treatment plant. An  
30 excellent recovery (101%) of total bromine was observed from the raw water to the post-  
31 chlorination stage. Excellent recoveries of total bromine (92-95%) were also obtained from  
32 chlorination of a synthetic water containing dissolved organic matter and bromide,  
33 demonstrating the validity of the halogen-specific TOX method for TOBr measurement. The  
34 halogen-specific TOX method is an important tool to monitor and better understand the

35 formation of halogenated organic compounds, in particular brominated organic compounds,  
36 in drinking water systems.

37

38 **Keywords:** total organic bromine, dissolved organic matter, bromide, chlorination, drinking  
39 water, health effects

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## 41 **1. Introduction**

42 Natural processes, such as salt water intrusion, high evaporation conditions in arid  
43 watersheds and natural salt deposits from ancient seas, as well as pollution from industrial  
44 activities, can result in elevated bromide and iodide concentrations in natural waters (Agus et  
45 al., 2009; von Gunten, 2003). Bromide is usually detected in natural waters in the range of  
46  $\sim 10$  to  $>1000 \mu\text{g L}^{-1}$  (Heeb et al., 2014), while iodide is found at much lower concentrations  
47 ( $\sim 50 \mu\text{g L}^{-1}$ ) (Agus et al., 2009). We have found that many source waters in Western  
48 Australia (WA) contain moderate to extremely high concentrations of bromide (up to  $8.5 \text{ mg}$   
49  $\text{L}^{-1}$ ) (Gruchlik et al., 2014), likely demonstrating all three natural processes of salt water  
50 intrusion, arid climate and ancient sea deposits, and leading to our focus on studies of the  
51 impact of bromide in drinking water treatment (e.g. Allard et al. 2013a; Allard et al. 2013b;  
52 Allard et al. 2015; Criquet et al. 2012; Criquet et al. 2015; Tan et al. 2016; Langsa et al.  
53 2017). Conventional coagulation/flocculation drinking water treatment processes do not  
54 effectively remove bromide (Kristiana et al., 2015; Tan et al., 2016), leading to bromide  
55 being present during the disinfection process. Bromide is rapidly oxidised by oxidants such as  
56 chlorine to produce hypobromous acid (HOBr), which can then react with natural organic  
57 matter (NOM) in the water to form brominated disinfection by-products (DBPs), in a similar  
58 way to chlorine (hypochlorous acid, HOCl) forming chlorinated DBPs. These DBPs may lead  
59 to potential adverse health effects (Hua and Reckhow, 2006). In fact, brominated DBPs have  
60 been reported to be hundreds of times more toxic than their chlorinated analogues in cell  
61 bioassays (Richardson and Kimura, 2016; Richardson et al., 2007; Yang et al., 2014).

62 Total organic halogen (TOX) represents all the chlorinated, brominated and iodinated  
63 organic compounds in a water sample. In drinking water treatment, TOX is generally used as  
64 a measure of the total halogenated DBP formation in disinfected water. In chlorinated waters,  
65 the measured individual DBPs have been reported to account for only 16-70% of TOX  
66 (Pressman et al., 2010; Richardson and Ternes, 2011; Tan et al., 2016), while in  
67 chloraminated waters, less than 20% of TOX can reportedly be assigned to individually  
68 measured species of DBPs (Hua and Reckhow, 2007; Li et al., 2002). Therefore, the

69 measurement of TOX includes both known DBPs and the significant fraction of TOX which  
70 remains unidentified and uncharacterised. Analysis of TOX offers the water industry and  
71 regulators a method to quantify all halogen incorporation into DBPs to better protect the  
72 public against the potential adverse health risks (e.g. bladder cancer (Richardson et al., 2007)  
73 from chlorinated or chloraminated drinking water. This is in contrast to the existing focus on  
74 two sets of individual DBPs (the trihalomethanes (THMs) and haloacetic acids (HAAs))  
75 which are not believed to be causative for the health risks (Bull et al., 2011). Moreover,  
76 recent studies have found that TOX not only represents the total concentration of all  
77 halogenated DBPs but is also an indicator of the overall toxicity of these halogenated DBPs  
78 (e.g. Yang et al., 2014).

79 Analytical methods used to identify and measure TOX in water systems involve:  
80 adsorption of dissolved organic matter (DOM), including halogenated organic compounds,  
81 onto activated carbon; combustion of the activated carbon; collection of resultant hydrogen  
82 halide gases in an absorber solution; determination of the concentration of halide ions in the  
83 absorber solution; and calculation of the concentrations of halogen originally incorporated  
84 into DOM in the water sample. While a method for the analysis of bulk TOX has long been  
85 standardised (APHA et al., 1995), more recently, it has become apparent that determination  
86 of the three specific TOX species, total organic chlorine (TOCl), total organic bromine  
87 (TOBr) and total organic iodine (TOI), is vital for studies of disinfection of waters containing  
88 bromide and iodide. This is because TOI is likely to be of greater health concern than TOBr,  
89 which itself is likely to be more problematic than TOCl (Plewa et al., 2004). Ion  
90 chromatography (IC) is the preferred detection method due to instrumentation costs and  
91 availability (Brandt and Kettrup, 1987; Hua and Reckhow, 2006; Li et al., 2011; Oleksy-  
92 Frenzel et al., 2000), and it enables the quantification of TOCl, TOBr and TOI in the original  
93 water sample by separation of chloride, bromide and iodide ions present in the absorber  
94 solution.

95 Brandt and Kettrup (1987) first reported the use of IC to separate between TOCl,  
96 TOBr and sulphur compounds in water samples. In their method, the combustion was  
97 conducted at 1050°C in the presence of oxygen at a flow rate of 300 mL min<sup>-1</sup>. Hydrogen  
98 peroxide solution was chosen to collect the resultant gases in the absorber, followed by off-  
99 line IC detection of halides in the absorber solution. Recoveries of model compounds  
100 containing chlorine and bromine varied from 3 to 109%. Chloramin-T, a biocide chemical,  
101 exhibited the lowest recovery, while the highest recovery was obtained for trichloroacetic  
102 acid (Brandt and Kettrup, 1987). The poor recovery of Chloramin-T is likely due to its

103 decomposition in water to form hypochlorite, which would not be absorbed onto the activated  
104 carbon but rather oxidise the carbon surface (Potwora, 2009), forming chloride which would  
105 remain in the water phase and not be recovered in the TOX method. Oleksy-Frenzel et al.  
106 (2000) then developed a method of differential TOX analysis with IC detection which  
107 optimised the combustion conditions and the gas absorption system. The combustion  
108 temperature chosen was also 1050°C but the oxygen flow rate was 150 mL min<sup>-1</sup>. A sulphuric  
109 acid solution was used prior to the absorber for drying of the combustion gases, followed by  
110 collection of the gases in a sodium sulfide absorber solution. Recoveries of model compounds  
111 containing chlorine, bromine and iodine were reported to range from 14 to 103% (Oleksy-  
112 Frenzel et al., 2000). While the selection of model compounds by Brand and Kettrup (1987)  
113 focussed on halogenated non-phenolic based compounds, Oleksy-Frenzel et al. (2000)  
114 covered a wider range of halogenated compounds including iodinated X-ray contrast media.  
115 The lowest recoveries were found for chloro- and iodo-acetamide (14% and 37%,  
116 respectively), while the highest recovery corresponded to iodoacetic acid (103%) (Oleksy-  
117 Frenzel et al., 2000). Echigo *et al.* (2000) used a similar combustion system to the system  
118 described by Brandt and Kettrup (1987), except that ultrapure water was used as the absorber  
119 solution. Recoveries of chlorinated and brominated model compounds ranged from 76 to  
120 84%.

121 Hua and Reckhow (2006) developed a method for the analysis of halogen-specific  
122 TOX using a conventional Euroglass TOX analyser (similar to the combustion system  
123 reported by Oleksy-Frenzel et al. (2000)) and an off-line IC, and reported high recoveries  
124 (92-104%) of model compounds containing chlorine, bromine and iodine. Finally, in a more  
125 recent study, we established a halogen-specific TOX method using a state-of-the-art on-line  
126 TOX-IC system (Kristiana et al., 2015). In this study, a broad assessment of key analytical  
127 parameters for accurate measurement of halogen-specific TOX in waters was performed,  
128 including the use of different types of granular activated carbon, two different absorber  
129 solutions, and selected model compounds covering different classes of DBPs. The recoveries  
130 of the model compounds were all reported to be greater than 85% (Kristiana et al., 2015).

131 The accuracy of the halogen-specific TOX measurement depends on the performance  
132 of each step of the process, which includes several analytical challenges, such as the activated  
133 carbon adsorption process. Previous studies applied different types of activated carbon for the  
134 enrichment of organic halogen compounds. Brandt and Kettrup (1987) used sugar activated  
135 carbon (ZAK, Merck, FRG), Oleksy-Frenzel et al. (2000) chose Mitsubishi's activated  
136 carbon (Japan), and Hua and Reckhow (2006) selected CPI and Calgon activated carbon.

137 Kristiana et al. (2015) tested different commercially available activated carbons, including  
138 Acticarb GC1200N, Filtrasorb<sup>®</sup>, Carbon 437, Carboxen<sup>™</sup>572, CPI International, Darco<sup>®</sup>,  
139 Ecologix, and Mitsubishi, for release of inorganic contaminants before and after the nitrate  
140 wash. It was found that CPI International and Darco<sup>®</sup> were the two types of activated carbon  
141 which released the minimum amount of inorganic contaminants (Kristiana et al., 2015).  
142 Using Mitsubishi activated carbon columns, (Li et al., 2010; Li et al., 2011) found that the  
143 activated carbon can also act as a reductant, reducing up to 20% of TOCl and 10% of TOBr  
144 to their respective halides. Li et al. (2011) also reported that 3-10% of polar brominated  
145 DBPs formed from chlorinated reference NOM standards penetrated through the Mitsubishi  
146 activated carbon column, although ozonation of the activated carbon minimised this loss of  
147 TOBr. Kristiana et al. (2015) investigated the CPI International activated carbon in terms of  
148 acting as a reducing agent and potential breakthrough of TOX. With careful examination of  
149 the effluent collected after adsorption of a halophenol mixture (2,4,6-trichlorophenol, 2,4,6-  
150 tribromophenol, and 2-iodophenol; up to 1000  $\mu\text{g L}^{-1}$  each) with two activated carbon  
151 columns in series, it was found that there was no breakthrough of analytes. In addition, each  
152 halophenol standard, measured as TOCl, TOBr and TOI, respectively, was fully recovered  
153 (104 $\pm$ 4%, 102 $\pm$ 4% and 96 $\pm$ 4%, respectively) (Kristiana et al., 2015). This indicates that two  
154 activated carbon columns in series effectively adsorbed all of the halophenol standards,  
155 without reduction to the halides, thus suggesting minimal errors in the adsorption process  
156 using CPI International activated carbon.

157 Our on-line TOX-IC system was also applied to study the mechanisms of TOBr  
158 formation (Langsa et al., 2017) and for measurement of halogen-specific TOX concentrations  
159 in a WA drinking water treatment plant. This plant treated source water containing a  
160 moderate bromide concentration (346  $\mu\text{g L}^{-1}$ ) and a very low DOC concentration (0.3  $\text{mg L}^{-1}$ )  
161 by a water softening/filtration process followed by chlorination (Kristiana et al., 2015). In this  
162 system, a total bromine recovery (concentrations of TOBr and bromide (after quenching of  
163 the oxidant residual)) of 89% was measured in the disinfected water compared to the raw  
164 water bromide concentration (Kristiana et al., 2015). The same halogen-specific TOX method  
165 was used in a subsequent study of two WA water treatment plants treating raw waters with  
166 moderate (400  $\mu\text{g L}^{-1}$ ) to high (754  $\mu\text{g L}^{-1}$ ) bromide concentrations and corresponding DOC  
167 concentrations of 3.5 and 1.2  $\text{mg L}^{-1}$  by chlorine disinfection only (Tan et al., 2016). Full  
168 bromine recoveries (109 and 103%, respectively) were observed in the distribution system  
169 samples (Tan et al., 2016). The recovery of total bromine in the distribution system of a WA

170 treatment plant treating raw water of again moderate bromide concentration ( $415 \mu\text{g L}^{-1}$ ) and  
171 DOC concentration of  $3.7 \text{ mg L}^{-1}$  by a conventional coagulation/flocculation process  
172 followed by chlorine disinfection was 82% (Tan et al., 2016). Thus, very good recoveries of  
173 total bromine have been observed in water treatment systems containing moderate to high  
174 bromide in the raw water, using the TOBr method.

175 Since brominated DBPs are generally accepted to be of greater health concern than  
176 their chlorinated analogues (Plewa et al., 2004; Richardson and Kimura, 2016), it is likely  
177 that TOBr will be of greater health concern than TOCl, however, there are only limited  
178 studies of the relationship between TOBr and toxicity. Echigo et al. (2004) separately treated  
179 standard humic acid with HOBr and HOCl and found that the activity inducing chromosomal  
180 aberrations (mutagenicity) per unit of TOX was two to six times higher in the case of TOBr  
181 than TOCl, concluding that TOBr was more mutagenic than TOCl. The TOX (and TOBr)  
182 concentration was found to increase throughout the treatment train in an Eastern Australian  
183 conventional drinking water treatment plant, correlating with the trend in nonspecific  
184 toxicity measured in a laboratory bioassay up until the final chloramination stage (Neale et  
185 al., 2012). Neale et al. (2012) suggested that the high TOBr/TOCl ratio may have contributed  
186 to the high nonspecific toxicity observed. Yang et al. (2014) disinfected a source water  
187 (treated to the pre-disinfection stage) with added bromide ( $500 \mu\text{g L}^{-1}$ ) and iodide ( $100 \mu\text{g L}^{-1}$ )  
188 by chlorination and chloramination in the laboratory. In these experiments, both  
189 cytotoxicity and genotoxicity were found to be highly correlated with TOBr and TOI. Pan et  
190 al. (2014) found that TOX and TOBr concentrations and mammalian cell cytotoxicity all  
191 decreased after boiling simulated chlorinated tap water (with no chlorine residual) for 5  
192 minutes. These studies highlight the application and growing importance of TOBr as an  
193 indicator of potential toxicity in chlorinated drinking waters.

194 The objectives of our study were to expand the optimisation and validation of the  
195 halogen-specific TOX method previously developed in our laboratory (Kristiana et al., 2015),  
196 with a focus on analysis of the potentially problematic TOBr fraction. This was first achieved  
197 through optimisation of the absorber solution and the gas line washing process, and  
198 expansion of the study of the recoveries of model compounds to include 8 haloacetic acids, 6  
199 haloacetonitriles and a total of 6 new halogenated compounds (4 brominated compounds).  
200 Then, the method was applied to measurement of halogen-specific TOX concentrations in a  
201 drinking water treatment plant treating source water containing a very high bromide  
202 concentration ( $1350 \mu\text{g L}^{-1}$ ) and a high DOC concentration ( $9.4 \text{ mg L}^{-1}$ ), with the focus on  
203 understanding the fate and recovery of total bromine. Finally, laboratory chlorination of a

204 standard NOM sample in the presence of a moderate ( $500 \mu\text{g L}^{-1}$ ) concentration of bromide  
205 allowed study of the fate and recovery of the initial bromide through analysis of the TOBr  
206 formed. This is the first report of the use of such a mass balance approach for halogen-  
207 specific TOBr method validation.

208

## 209 **2. Materials and Methods**

### 210 **2.1 Chemicals and Standard Solutions**

211 All inorganic reagents, organic solvents and organic compounds were of analytical  
212 grade purity or higher, and were used without further purification. Specific details on  
213 chemicals and preparation of solutions are provided in the Supporting Information (Text SI1  
214 and SI2, **Table S1**).

215

### 216 **2.2 Halogen-Specific TOX Analysis using an On-Line TOX-IC System**

217 Standard solutions and water samples (50 mL) were analysed using an on-line TOX-  
218 IC system according to the method of Kristiana et al. (2015) (**Figure S1**). Additional details  
219 are that the activated carbon columns were washed with aqueous nitrate solution (5 mL,  $5 \text{ g}$   
220  $\text{L}^{-1}$ ) to remove inorganic halides, the combustion of the activated carbon was conducted at  
221  $1000^\circ\text{C}$  and a small amount of water was passed through the gas lines leading into the gas  
222 absorption tube to ensure all halide gases were collected, before an aliquot of the absorption  
223 solution was automatically injected into the IC system with the injection volume loop being  
224  $100 \mu\text{L}$ . In a separate experiment, an alternative aqueous absorbing solution containing  
225 approximately  $0.5 \text{ g L}^{-1} \text{ Na}_2\text{S}$  was also trialled in order to compare the effectiveness of the  
226 collection of halide gases. The effect of different parameter settings for washing of the gas  
227 line (number of washes and duration of washes) on the concentration factor was also studied.  
228 The concentration factor of TOX in the initial solution to halide in the absorber solution  
229 allows calculation of the TOX concentrations in samples. The total volume of the absorber  
230 solution (ultrapure water) was measured by weight (five replicates).

231 The concentrations of halogen-specific TOX (i.e. TOCl, TOBr and TOI) in the  
232 absorber solution were measured as chloride, bromide and iodide, respectively, and the  
233 concentrations of halogen-specific TOX in the initial standard solution or water sample were  
234 calculated by dividing the concentrations measured in the absorber solution by the  
235 concentration factor (6.16; based on TOX in 50 mL of sample being concentrated into 8.12

236 mL of the final absorber solution; **Table S2**). The quantification limit was  $3 \mu\text{g L}^{-1}$  for  
237 chloride,  $2 \mu\text{g L}^{-1}$  for bromide, and  $1 \mu\text{g L}^{-1}$  for iodide.

238

### 239 **2.3 Measurement of Halogen-Specific TOX in Drinking Water Treatment Plant** 240 **Samples**

241 Water samples from sampling points in a WA drinking water groundwater treatment  
242 plant (GWTP1) were collected for application of the halogen-specific TOX measurement to a  
243 drinking water system. GWTP1 raw water contained a very high bromide concentration  
244 ( $0.42\text{-}1.35 \text{ mg L}^{-1}$ ; **Table S3**). The water treatment process at GWTP1 is comprised of pre-  
245 chlorination, alum coagulation/flocculation, filtration, fluoridation, pH adjustment and  
246 chlorination for disinfection. Free chlorine equivalent concentrations of the water samples  
247 were measured at the sampling locations using a portable pocket colorimeter (HACH,  
248 Loveland, CO, USA; *N,N*-diethyl-phenylene-1,4-diamine (DPD)). For water samples to be  
249 analysed for TOX, any chlorine equivalent residual remaining in the water samples was  
250 quenched immediately with aqueous sodium sulphite solution (10x excess based on chlorine  
251 equivalent concentration). In the laboratory, the samples were filtered through a  $0.45 \mu\text{m}$   
252 membrane filter and stored at  $4^\circ\text{C}$  prior to analysis for bromide, dissolved organic carbon and  
253 halogen-specific TOX. Dissolved organic carbon concentrations were measured using a  
254 Shimadzu TOC- $V_{\text{ws}}$  Total Organic Carbon Analyser according to the Standard Method  
255 5310C (APHA et al., 1995). Bromide concentrations were analysed according to the method  
256 of Salhi and von Gunten (1999) using a Dionex ICS 3000 IC system (UV detector). The  
257 quantification limit was  $2.8 (\pm 0.9) \mu\text{g L}^{-1}$ .

258

### 259 **2.4 Measurement of Halogen-Specific TOX from a Chlorinated Synthetic Water** 260 **containing Bromide and DOM**

261 An aqueous solution (2 L, pH 8) containing Nordic Reservoir DOM (NR-DOM) ( $4$   
262  $\text{mgC L}^{-1}$ ) and bromide ( $500 \mu\text{g L}^{-1}$ ,  $6.26 \mu\text{M}$ ) was treated with chlorine ( $75 \mu\text{M}$ ,  $\sim 5.3 \text{ mgCl}_2$   
263  $\text{L}^{-1}$ ) for contact times of 5, 10, 15, 30, 45 and 60 minutes. The residual oxidant (sum of HOCl  
264 and HOBr, expressed as a free chlorine equivalent concentration in  $\text{mg L}^{-1}$ ) in each sample  
265 was quenched with sodium sulphite solution ( $750 \mu\text{M}$  or 10x excess based on initial chlorine  
266 concentration) prior to analysis of halogen-specific TOX and bromide ion.

267

## 268 **3. Results and Discussion**



### 269 3.1 Further Optimisation of the Halogen-Specific TOX Method

270 The first objective of our study was to optimise the absorber solution and the gas line  
271 washing process. The gas absorber (GA-100) unit is a part of the AQF-IC system that  
272 receives the reaction gas containing hydrogen halides (HX) from the combustion unit. The  
273 hydrogen halide gases dissolve in the ultrapure water in the absorber and the halide ions ( $X^-$ )  
274 are separated and detected by IC. A mixed halogenated organic compound standard solution  
275 (2,4,6-trichlorophenol, 2,4,6-tribromophenol, 2-iodophenol, bromobenzene, 1,4-  
276 dibromobenzene; each halogenated organic compound at  $100 \mu\text{g L}^{-1}$ , unless otherwise stated)  
277 was used in these optimisation studies. Halophenol standards were chosen due to their  
278 frequent previous use for this purpose (e.g. APHA et al., 1995; Oleksy-Frenzel et al., 2000;  
279 Kristiana et al., 2015), while mono- and dibromobenzenes representing brominated benzene  
280 compounds were used in addition to the halophenol standards. The concentration of each  
281 halogenated organic compound was  $100 \mu\text{g L}^{-1}$ , a mid-range concentration that can be easily  
282 detected.

#### 283 284 3.1.1 Optimisation of Absorber Solution

285 The use of an aqueous sodium sulphide solution as an absorber solution was  
286 recommended by Oleksy-Frenzel et al. (2000) since they proposed that oxyhalogen species  
287 may be formed along with hydrogen halides during the combustion step and sodium sulphide  
288 can reduce these oxyhalogen species to halide ions. However, since Oleksy-Frenzel et al.  
289 (2000) only used aqueous sodium sulphide solution as an absorber solution and did not  
290 compare this to the simpler option of ultrapure water, it was important to compare the use of  
291 both of these absorber solutions in the current halogen-specific TOX method using the AQF-  
292 IC instrumentation. The recoveries of the mixed halogenated organic compound standards  
293 when ultrapure water and aqueous sodium sulphide solution ( $0.5 \text{ g L}^{-1}$ ) were separately used  
294 as the absorber solutions are presented in **Figure 1**.

295 Use of ultrapure water, rather than aqueous sodium sulfide solution, resulted in higher  
296 recoveries for all of the selected halogenated organic compounds (**Figure 1**), possibly due to  
297 the effect of ionic strength. The higher concentration of ionic species in the sodium sulphide  
298 solution compared to the ultrapure water may have resulted in lower absorption of hydrogen  
299 halide gases. The recoveries of the three individual halophenol standards with the use of  
300 ultrapure water were 87-107%, while only 68-93% of these compounds were found to be  
301 recovered with the use of aqueous sodium sulfide solution. For the bromobenzenes, the

302 recoveries were again higher with the use of ultrapure water. Calibration studies (using  
303 halides calculated as Cl<sup>-</sup>, Br<sup>-</sup>, I<sup>-</sup>) showed negligible difference between the use of ultrapure  
304 water and sodium sulphide solution as the solvent for analysis (results not shown). The higher  
305 recoveries from the use of ultrapure water in the absorber indicate that formation of  
306 oxyhalogen species in the combustion process was not significant and that sodium sulphide  
307 solution in the absorber was not necessary, in contrast to the hypothesis of Oleksy-Frenzel et  
308 al. (2000). Oleksy-Frenzel et al. (2000) used a different set of model compounds (4-chloro-,  
309 4-bromo-, and 4-iodo-phenol), which were essentially fully recovered, to verify their method  
310 using sodium sulfide solution in the absorber. However, their recoveries of a wider range of  
311 halogenated organic compounds were very variable (14-103%) and their recovery of the only  
312 compound present in both studies, 1,4-dibromobenzene, was 49% (Oleksy-Frenzel et al.  
313 (2000)) compared to 77% using sodium sulphide as the absorber solution and 94% using  
314 ultrapure water as the absorber solution in the current study. Thus, ultrapure water has been  
315 found to be superior to sodium sulphide as the absorber solution and therefore ultrapure water  
316 was chosen as the solvent for the absorber solution in this analytical method.

317

### 318 **3.1.2 Effect of Gas Line Washing Time**

319 In our previous study, a key to understanding the halogen-specific TOX method was  
320 the realisation that the plug of water used to rinse the gas line from the combustion unit to the  
321 absorber unit just prior to injection of the absorber solution into the IC added 3.34 mL of  
322 water to the volume of absorber solution (5 mL) (Kristiana et al., 2015). The purpose of  
323 washing the gas line is to ensure that there is no carryover between the samples. This 67%  
324 increase in volume of the absorber solution (total 8.34 mL) affects the concentration factor in  
325 the calculation of the measured halogen-specific TOX concentration, and therefore the  
326 recovery of model compounds. Taking this increased volume of absorber solution into  
327 account resulted in recoveries of studied model compounds ranging from 85 ( $\pm 0.4$ ) to  
328 126 ( $\pm 20$ )% (Kristiana et al., 2015).

329 Following on from the work of Kristiana et al. (2015), the influence of different gas  
330 line washing parameters to the total volume of the absorber solution, and thus the impact on  
331 the recoveries of the halophenol standard compounds, was assessed. The volume of absorber  
332 solution dispensed from the GA-100 unit to the gas absorber tube was set constant at 5 mL.  
333 The AQF-100 system program has a setting range for the number of gas line washes from 0  
334 to 99, with the duration of washing time being varied from 0.1 to 2.0 s. In these experiments,  
335 the number of washes and the time for each wash was varied. One or two washes, for 0.1, 0.5

336 or 1.0 s, were selected, as the maximum capacity of the gas absorber tube is only 10 mL  
337 (flow rate was 1 mL min<sup>-1</sup>). The results are presented in **Table S2**.

338         Increasing the number of washes and the time of washing consistently increased the  
339 measured total absorber volume, as expected. The minimum washing volume (0.37 mL) was  
340 added with one wash for 0.1 s. The maximum washing volume (3.12 mL) was added with  
341 two washes of 1.0 s each.

342         There was little difference in the recoveries of the halophenol standard compounds  
343 with the exception of the smallest volume increase experiment (one wash for 0.5 s) where  
344 slightly lower recoveries were observed (**Figure S2**). Most likely, under these conditions, not  
345 all of the halides remaining in the gas line were washed into the absorber solution, resulting  
346 in incomplete recoveries. A statistical analysis using a Kruskal-Wallis rank sum test ( $\alpha=0.05$ ,  
347  $H_{\text{stat}} > X^2_{\text{crit}}$ ) showed that there were significant differences between the recoveries of  
348 halophenol standard compounds and the number of washes and the time of washing. The  
349 setting of two washes at 1.0 s was found to produce the optimum recoveries of the halophenol  
350 standards, therefore, these gas line setting parameters were selected for this halogen-specific  
351 TOX method.

352

## 353 **3.2 Further Validation of the Halogen-Specific TOX Method**

### 354 **3.2.1 Recoveries of Organic Halogen in Model Compounds**

355         Recoveries of organic halogen in model compounds have been previously reported as  
356 TOX method validation approaches (e.g. Brandt and Kettrup (1987); Oleksy-Frenzel et al.  
357 (2000), Hua and Reckhow (2006); Kristiana et al. (2015)), where several halogenated organic  
358 compounds have been selected for validation of the optimised method. Brandt and Kettrup  
359 (1987) selected one or two organic chlorine, bromine and sulphur compounds, representing  
360 different organic functional groups, for their method validation. Oleksy-Frenzel et al. (2000)  
361 focused on chloro- and bromo-benzenes and included several X-ray contrast media as model  
362 compounds. Hua and Reckhow (2006) and Kristiana et al. (2015) chose HAAs and THMs,  
363 respectively, as their main model compounds. In the current study, the recoveries of organic  
364 halogen from a wide range of halogenated organic compounds, representing major classes of  
365 DBPs (i.e. HAAs, haloacetonitriles (HANs), halophenols and halogenated benzenes) were  
366 investigated. The list of model compounds included 6 model compounds not previously studied  
367 (**Table S4**). The THMs were not studied as the recoveries from this class of DBPs have been  
368 previously reported (e.g. ten THMs studied by Kristiana et. al., (2015)).

369 The recoveries of organic halogen from 26 model compounds, along with their  $pK_a$ ,  
370 molecular weight, and octanol/water partition coefficient ( $\log K_{ow}$ ), are presented in **Table**  
371 **S4**. Very good recoveries of organic halogen from all model compounds were obtained,  
372 indicating high or complete conversion of all organic halogen in the model compound  
373 solution through to halide in the absorber solution for IC analysis. The recoveries ranged  
374 from 78 to 135% for organochlorine compounds, with only monochloroacetic acid found to  
375 be recovered less than 80% (78%). The TOX-IC method performed particularly well for the  
376 organobromine compounds, where the range of recoveries was slightly better than the  
377 organochlorine compounds, being 83 to 118%, with most of the organobromine model  
378 compounds exhibiting recoveries around 100%. 2-Iodophenol represented the only  
379 organoiodine compound studied and its recovery was 85%.

380 Since the recoveries were consistently high across all chemical classes studied,  
381 functional groups did not appear to affect the recoveries achievable in the halogen-specific  
382 TOX method. The recoveries were also consistently high across different molecular weight,  
383  $pK_a$ , and  $\log K_{ow}$  values. Likewise in several previous studies, there has been no observable  
384 significant trend between molecular weight or octanol-water partition coefficient and  
385 recovery of TOX from model compounds (e.g. Brandt and Kettrup (1987); Hua and Reckhow  
386 (2006); Kristiana et al (2015); Oleksy-Frenzel et al. (2000).

387 In the current study, the recoveries of 1,2-dichlorobenzene and 1,4-dibromobenzene  
388 were 94 and 98%, respectively, while Brandt and Kettrup (1987) and Oleksy-Frenzel et al.  
389 (2000) both reported low recoveries ( $< 49\%$ ) for these benzenes. The excellent recovery  
390 observed currently for 1,4-dibromobenzene was consistent with the recovery (93%) for this  
391 compound reported by Kristiana et al. (2015). The recoveries of the dihalobenzenes obtained  
392 from the current study were  $> 94\%$ , indicating that the CPI activated carbon may offer  
393 superior adsorption of the dihalobenzenes compared to the Mitsubishi activated carbon and  
394 “Sugar Activated Carbon” used by Oleksy-Frenzel et al. (2000) and Brandt and Kettrup  
395 (1987), respectively.

396 In terms of the recoveries of the HAAs, Oleksy-Frenzel et al. (2000) reported a low  
397 recovery of 2-chloroacetic acid (35%) and proposed that this compound did not fully adsorb  
398 onto the Mitsubishi activated carbon. They suggested that molecular weight could affect the  
399 recoveries of the HAAs, since HAAs with increasing molecular weight had increasing  
400 recoveries (83% recovery for trichloroacetic acid). The excellent recoveries of all of the  
401 HAAs in the current study ( $> 80\%$ , **Table S4**) are in contrast to the findings of Oleksy-  
402 Frenzel et al. (2000) and suggest superior adsorption of these model compounds onto the CPI

403 activated carbon. In our study, CPI activated carbon was chosen due to its minimal or low  
404 release of TOX contamination compared to the Mitsubishi activated carbon used by Oleksy-  
405 Frenzel et al. (2000) as reported by Kristiana et al. (2015). The very good recoveries of model  
406 compounds achieved in our study indicate that the CPI activated carbon appears to offer the  
407 added benefit of an improved enrichment process of TOX from waters containing organic  
408 halogen compounds.

409 In conclusion, this model compound study across a wide range of functional groups  
410 and molecular weights, including the three types of organohalogen compounds  
411 (organochlorine, organobromine and organoiodine), demonstrates very good method  
412 performance in terms of recovery of organic halogen in the halogen-specific TOX method.

413

### 414 **3.2.2 Validation of Improved Halogen-Specific TOX Method in Drinking Water** 415 **Treatment Plant Samples**

416 The optimised halogen-specific TOX method was applied to study the formation of  
417 halogen-specific TOX and the fate and recovery of total bromine in a WA groundwater  
418 treatment plant treating water containing a very high bromide concentration ( $1350 \mu\text{g L}^{-1}$ )  
419 and a high DOM concentration ( $9.4 \text{ mg L}^{-1}$  as DOC) (GWTP1). **Figure 2** shows a schematic  
420 of the GWTP1 conventional treatment process and the concentrations of various water quality  
421 parameters at the two sampling points: raw water inlet and after final chlorination. Some  
422 historical concentrations of bromide and DOM in the raw water for GWTP1, as well as the  
423 concentrations measured in the current study (28 May 2012), are presented in **Table S3**  
424 (WCWA, 2009). The DOM concentration of the raw water sample collected for the current  
425 study was similar to the historical average concentration, while the bromide concentration  
426 was almost twice the historical average concentration. This is likely due to the input, from  
427 December 2009, to GWTP1 of a new bore into a deep artesian aquifer, where the water  
428 typically contains lower concentrations of DOM ( $\sim 1 \text{ mg L}^{-1}$ ) but much higher concentrations  
429 of bromide ( $[\text{Br}^-] > 2 \text{ mg L}^{-1}$ ) than the shallow aquifer (Gruchlik et al., 2014).

430 In the post-chlorination sample, final disinfection with chlorine ( $3 \text{ mgCl}_2 \text{ L}^{-1}$ ) resulted  
431 in high TOBr formation, with 79% of initial bromide ( $1350 \mu\text{g L}^{-1}$ ,  $16.9 \mu\text{M}$ ) being converted  
432 to TOBr ( $1072 \mu\text{g L}^{-1}$ ,  $13.4 \mu\text{M}$ ), while about 22% of the initial bromide was detected as  
433 bromide after quenching (**Figures 2 and 3a**). The TOBr formed in 2 steps. First, chlorine  
434 (from pre- and final-chlorination additions) oxidised bromide in the raw water to bromine,  
435 then bromine reacted with reactive functional groups in the DOM through electrophilic

436 addition or substitution to form TOBr. The total bromine, calculated as a sum of TOBr and  
437 bromide (after quenching), was fully recovered in the post-chlorination sample ( $1372 \mu\text{g L}^{-1}$ ;  
438  $17.1 \mu\text{M}$ ) when compared to the initial bromide concentration in the raw water inlet. In  
439 contrast to TOBr, TOCl was detected at a low concentration ( $100 \mu\text{g L}^{-1}$ ,  $2.8 \mu\text{M}$ ) in the post-  
440 chlorination sample (**Figures 2 and 3b**), indicating that only 12% of the added chlorine ( $3$   
441  $\text{mgCl}_2 \text{L}^{-1}$ ) was incorporated into the DOM moieties to form chlorinated organic compounds  
442 (measured as TOCl). The DOM concentration was also observed to decrease for a total of  
443 48% reduction across the treatment plant (**Figure 2**).

444 The lower chlorine incorporation into DOM compared to high bromine incorporation,  
445 from raw water to post-chlorination water, despite the lower concentration of bromine than  
446 chlorine, is consistent with many previous reports that bromine is more reactive and faster to  
447 react than chlorine towards DOM reactive sites for electrophilic addition and substitution  
448 (Acero et al., 2005; Criquet et al., 2015; Westerhoff et al., 2004). Therefore, bromine is a  
449 better substitution/addition agent for halogenation compared to chlorine. A chlorine  
450 equivalent residual was still detected ( $2.2 \text{ mg Cl}_2 \text{L}^{-1}$ ) in the post-chlorination sample and  
451 residual bromide ( $300 \mu\text{g L}^{-1}$ ,  $3.8 \mu\text{M}$ ) was measured after quenching the chlorine equivalent  
452 residual. Our previous studies of bromine recoveries in drinking water treatment plants  
453 receiving moderate to high bromide concentrations demonstrated similarly good to excellent  
454 recoveries of bromine from raw water to disinfected water (82-109% for moderate bromide  
455 concentrations; 103% for high bromide concentration) (Kristiana et al., 2015; Tan et al.,  
456 2016). By comparing the formation of TOBr in the post-chlorination sample with the initial  
457 bromide concentration in the raw water inlet, there was about 79% bromide conversion into  
458 TOBr, along with the excellent mass balance of total bromine across the plant (101%). These  
459 good to excellent mass balances of bromine following the fate and transformation of bromide  
460 from the raw water through the treatment process support the validity of the halogen-specific  
461 TOX method as an important tool to monitor and better understand the formation of  
462 halogenated organic compounds, in particular the potentially more problematic brominated  
463 organic compounds, in drinking water systems.

464

### 465 **3.2.3 Measurement of Halogen-Specific TOX during Halogenation of DOM Extract** 466 **Solutions: Accuracy of TOBr Method**

467 The halogen-specific TOX method was finally used to study the fate and recovery of  
468 bromide after chlorination of a DOM sample in the presence of a moderate concentration of  
469 bromide, through analysis of the TOBr formed. An aqueous solution of NR-DOM ( $4 \text{ mgC}$

470 L<sup>-1</sup>) was treated with chlorine (75 μM, ~ 5 mg Cl<sub>2</sub> L<sup>-1</sup>) in the presence of bromide ion (6.26  
471 μM, 500 μg L<sup>-1</sup>) at pH 8, and the formation of halogen-specific TOX and the total amount of  
472 bromine and bromide (measured as bromide after quenching the oxidant residual) was  
473 measured over 1 h.

474 TOCl and TOBr, as well as the reduced bromine (measured as bromide after  
475 quenching) and the total bromine (calculated as the sum of TOBr and bromide), are shown in  
476 **Figure 4**. Only 6% of the added chlorine (75 μM) was incorporated into NR-DOM and  
477 measured as TOCl (4.1 μM) in the first 5 min. Thereafter, TOCl continuously increased,  
478 albeit more slowly, for the rest of the experimental period (9% Cl-incorporation, 7 μM, after  
479 1 h). In contrast, 44% of the initial bromide was incorporated into NR-DOM to form TOBr  
480 (2.6 μM) in the first 5 min and bromide incorporation appeared to plateau after 30 min (57%,  
481 3.3 μM). The higher percentage of bromide incorporation (≥44%) after only 5 min of reaction  
482 confirms the fast reaction of bromine with DOM reactive sites (Criquet et al., 2015;  
483 Westerhoff et al., 2004).

484 To evaluate the recovery of the initial bromide, as TOBr or bromine/bromide, the total  
485 bromine represented by these three species was calculated (**Figure 4**). The recovery of the  
486 initial bromide was excellent at all times over the 1 hour period (≥ 95%), giving an excellent  
487 mass balance of bromine in the system. This result indicates that the halogen-specific TOBr  
488 method provides an accurate measure of the TOBr formed in the system. This is the first  
489 report of the use of such a mass balance approach for halogen-specific TOBr method  
490 validation. The high recovery of the initial bromide in this approach is also consistent with  
491 the very good recoveries of model compounds demonstrated above for the halogen-specific  
492 TOX method.

493

#### 494 **4. Conclusions**

495 Optimisation of the instrumental conditions of the gas absorber module of the AQF-  
496 IC system was conducted. Very good recoveries (78-135%) of a wide range of halogenated  
497 organic model compounds (as TOCl, TOBr and TOI) were achieved, indicating very good  
498 method performance in converting organic halogen in the model compound solution through  
499 to halide in the IC detector.

500 Studies of the flow and transformation of bromide in a groundwater treatment plant  
501 with a very high concentration of bromide and DOM in the inlet water showed good bromine  
502 recovery (mass balance of TOBr and bromide concentrations compared to initial bromide

503 concentration). This supports the validity of the halogen-specific TOX method, especially for  
504 TOBr measurement, in drinking water systems. The application of this analytical method to  
505 study the formation of TOBr upon chlorination of an aqueous solution of a standard DOM  
506 extract and bromide was successful in monitoring the conversion of bromide to TOBr  
507 through electrophilic substitution and addition reactions. The recovery of the initial bromide  
508 as the total measured bromine (sum of TOBr and bromide) was excellent (92-95%) over the 1  
509 hour reaction period, indicating that the halogen-specific TOBr method provided an accurate  
510 measure of the TOBr formed in the solution.

511 Due to the potential health impacts of brominated organic compounds (TOBr) in  
512 drinking waters, minimisation of TOBr in drinking water treatment plants and distribution  
513 systems is essential. The halogen-specific TOX method provides an important tool to monitor  
514 and better understand the formation and fate of halogenated organic compounds, in particular  
515 the potentially more problematic TOBr, in drinking water systems. The halogen-specific  
516 TOX method provides comprehensive information about the overall incorporation of halogen  
517 into organic compounds, rather than the incorporation of halogen into a few small individual  
518 DBP molecules (e.g. THMs and HAAs), as are currently monitored and regulated. It is  
519 recommended that drinking water utilities consider inclusion of halogen-specific TOX  
520 analysis in their monitoring regimes. Further studies of halogen-specific TOX formation in  
521 drinking water systems as related to health impacts (e.g. epidemiological studies) would  
522 allow governments and health regulators to consider developing new guideline values for  
523 TOX concentrations in drinking waters.

524

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532

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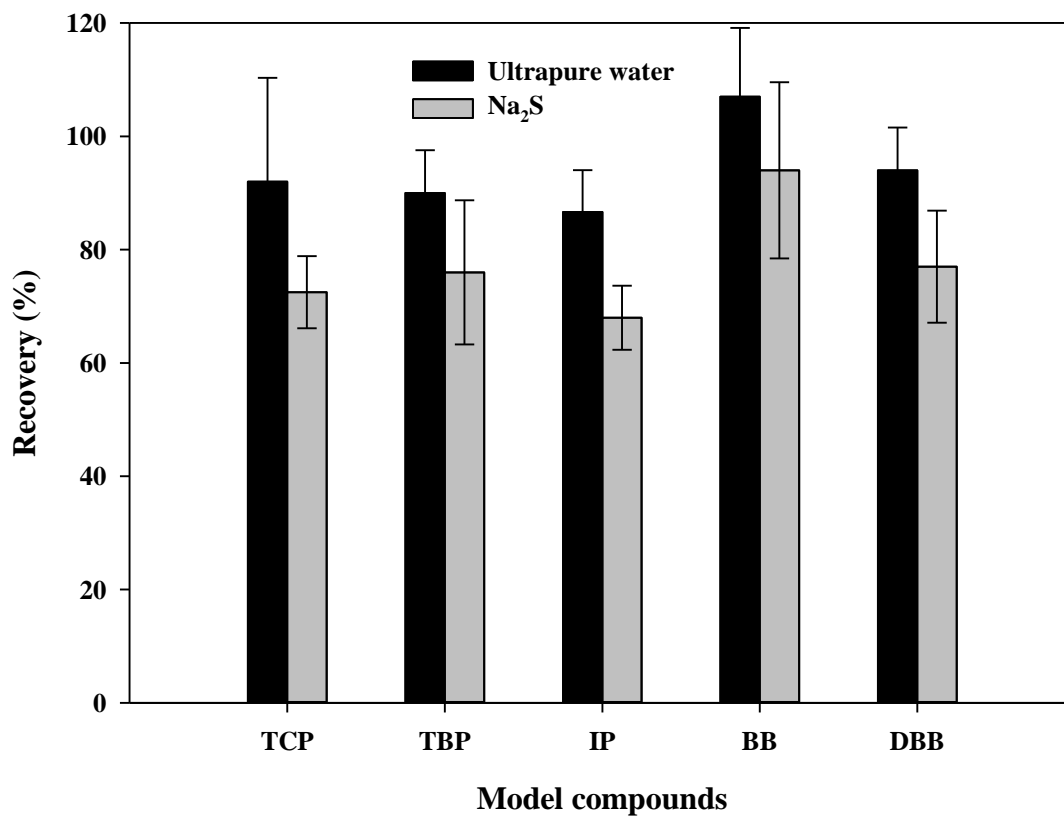
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641 **List of Figures**

642

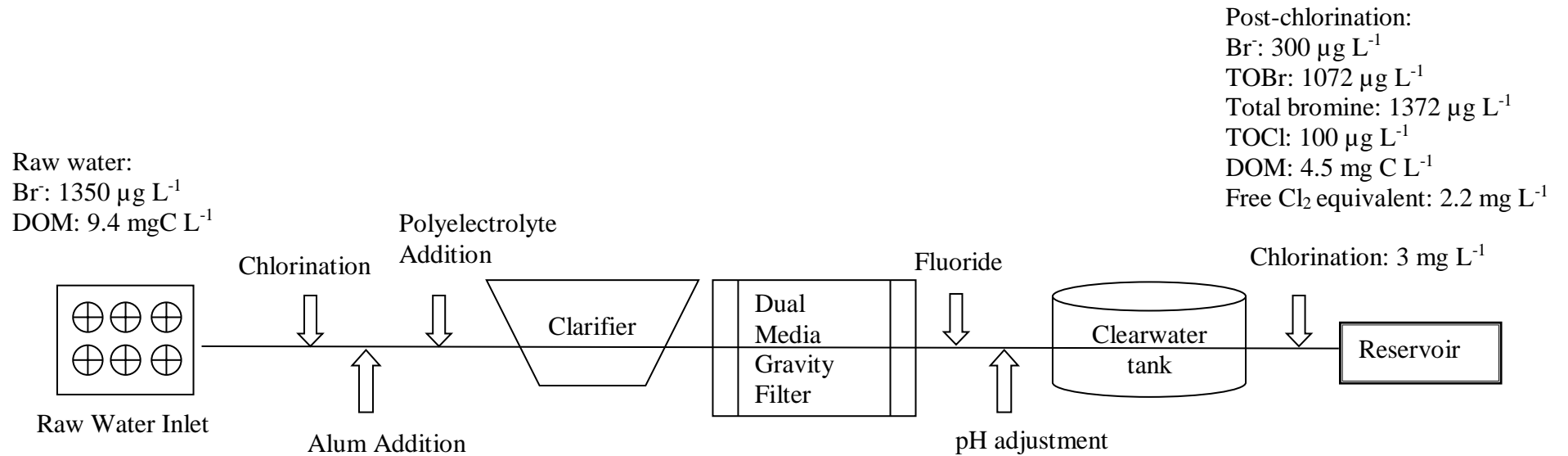


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645 **Figure 1** The effect of different absorber solutions (ultrapure water and aqueous sodium  
646 sulphide solution) on the recovery of selected standard compounds. TCP: 2,4,6-  
647 trichlorophenol; TBP: 2,4,6-tribromophenol; IP: 2-iodophenol; BB: bromobenzene; DBB:  
648 1,4-dibromobenzene (concentration of each halogenated organic compound in the sample  
649 was 100 µg L<sup>-1</sup>).

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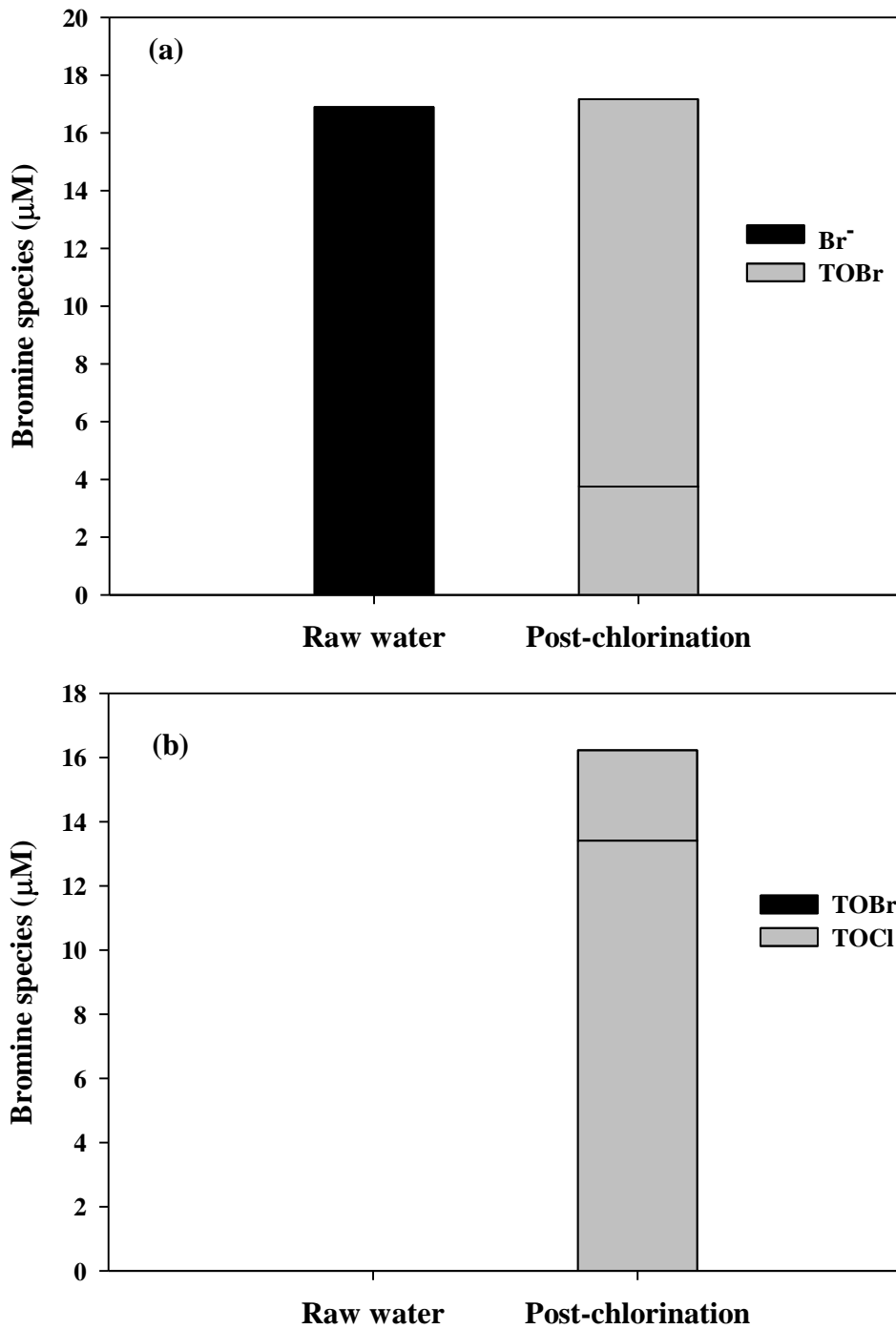
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671 **Figure 2** Schematic of the treatment process at GWTP1. Concentrations of bromide, dissolved organic matter, halogen-specific TOX, total  
672 bromine (calculated as the sum of bromide and TOBr concentrations) and free chlorine equivalents at the two sampling points are shown.

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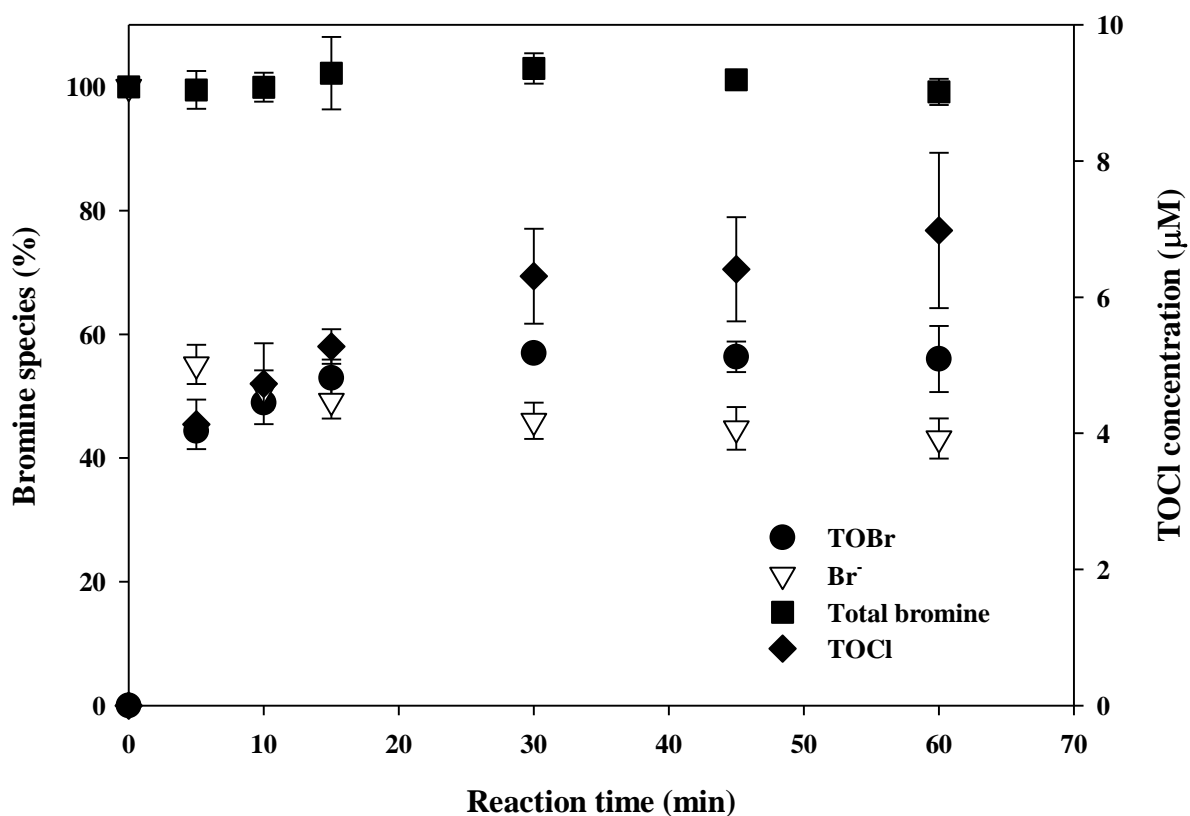
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677 **Figure 3** Halogen-specific TOX formation showing (a) conversion of  $\text{Br}^-$  to TOBr and (b)

678 TOCl vs TOBr through the water treatment train at GWTP1.

679



680

681 **Figure 4** Concentrations of halogen-specific TOX (TOCl and TOBr with TOBr  
 682 concentrations expressed as Br-incorporation (%)) and the inorganic bromine species  
 683 (measured as Br<sup>-</sup> after quenching the oxidant residual) over time. Experimental conditions:  
 684 NR-DOM (4 mgC L<sup>-1</sup>), bromide (500 μg L<sup>-1</sup>, 6.26 μM), phosphate buffer (1.0 mM), pH = 8,  
 685 chlorine (75 μM, ~ 5 mg Cl<sub>2</sub> L<sup>-1</sup>), Na<sub>2</sub>SO<sub>3</sub> (750 μM) for quenching. The “black squares”  
 686 represent the total bromine measured in the system at the sampling times, being the sum of  
 687 measured TOBr and bromide. Lines are shown as a guide.

688



## Supporting Information

### Halogen-Specific Total Organic Halogen Analysis: Assessment by Recovery of Total Bromine

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This section includes 2 texts, 4 tables and 2 figures.

20 **Text S11: Chemicals and solutions**

21 A list of all of the chemicals used in this study is given in Table S1 below.

22 **Table S1** Chemicals and standards used for validation of the halogen-specific TOX method

Chemicals*	Purity (%)	Number of halogen atoms		
		Chlorine	Bromine	Iodine
<b>Model compound</b>				
Chloroacetic acid	99	1		
Dichloroacetic acid	99.9	2		
Chlorodibromoacetic acid	94.6	1	2	
Trichloroacetic acid	99	3		
Bromoacetic acid	99		1	
Bromochloroacetic acid	99.9	1	1	
Bromodichloroacetic acid	99.9	2	1	
Dibromoacetic acid	98.7		2	
Bromoacetonitrile	97		1	
Dibromoacetonitrile	>90		2	
Chloroacetonitrile	99	1		
Dichloroacetonitrile	98	2		
Bromochloroacetonitrile	NA	1	1	
Trichloroacetonitrile	98	3		
2-Chlorophenol	>99	1		
4-Chlorophenol	>99	1		
2,6-Dichlorophenol	99	2		
Pentachlorophenol	97	5		
4-Bromophenol	99		1	
2,4-Dibromophenol	95		2	
Bromobenzene	>99.5		1	
1,2-Dichlorobenzene	99	2		
1,4-Dibromobenzene	98		2	
<b>Halophenol standards</b>				
2,4,6-Trichlorophenol	98	3		
2,4,6-Tribromophenol	99		3	
2-Iodophenol	98			1
<b>Halide standards</b>				
Potassium chloride	>99.5			
Potassium bromide	>99.5			
Potassium iodide	>99			
<b>Buffer</b>				
Dipotassium phosphate	>98			
Potassium di-hydrogen phosphate	>99			
<b>Quenching agent</b>				
Sodium sulphite	>98			

23 \* Purchased from Sigma-Aldrich (Castle Hill, NSW, Australia), except for dibromoacetonitrile  
 24 (Supelco) and bromochloroacetonitrile (Accustandard Inc. New Haven, CT, USA).

25

26

## 27 **Test SI2: Preparation of Solutions**

28           Ultrapurified water (ultrapure water) (resistivity of 18.2 mΩ), produced with a  
29 Purelab Ultra Analytic purification system (Elga, UK), was used for all experiments.

30           A mixed halophenol standard solution, as used in the Standard Method (APHA et al.,  
31 1995) and in the AQF-100 Mitsubishi combustion module manual for the measurement of  
32 halogen-specific TOX concentration in water samples, was prepared. This solution contained  
33 2,4,6-trichlorophenol, 2,4,6-tribromophenol and 2-iodophenol. A stock solution (50 mL; 2  
34 g L<sup>-1</sup> of the respective halogen) was prepared in methanol. A working solution of halophenols  
35 (100 mg L<sup>-1</sup>) was prepared by dilution of the stock solution in methanol. Aliquots of the  
36 working solution were further diluted into ultrapure water to achieve working standard  
37 solutions ranging in concentration from 0 – 1000 µg L<sup>-1</sup>.

38           A series of halogenated organic compounds were selected as model compounds for  
39 the evaluation of the use of different absorber solutions on the recoveries of the model  
40 compounds. These halogenated organic compounds included a mixed of halophenol  
41 compounds (2,4,6-trichlorophenol, 2,4,6-tribromophenol and 2-iodophenol) and 2 other  
42 brominated benzenes (bromobenzene and 1,4-dibromobenzene). Each halogenated organic  
43 compound was used at 100 µg L<sup>-1</sup>.

44           For calibration of the IC system, aqueous individual stock solutions (1000 mg L<sup>-1</sup>) of  
45 the three anions (chloride, bromide and iodide) were prepared from reagent grade potassium  
46 salts. These stock solutions were then diluted with water to make working standard solutions  
47 with concentrations varying from 10 to 1000 µg L<sup>-1</sup>.

48           Model organic compounds (26) containing chlorine, bromine and/or iodine,  
49 representing some major classes of DBPs, were selected to validate the optimised halogen-  
50 specific TOX method. The model compounds included haloacetic acids (HAAs),  
51 haloacetonitriles (HANs), chlorophenols, bromophenols and halogenated benzenes (Table  
52 S1). A stock solution of each organic halogen compound was prepared at a concentration of  
53 100 mg L<sup>-1</sup> in methanol. Final working solutions (100 µg L<sup>-1</sup> in water; 250 mL) were then  
54 prepared. All stock solutions were kept at -15 °C to avoid degradation. A commercial  
55 dissolved organic matter (DOM) extract from the International Humic Substances Society  
56 (IHSS) was used in this study (Nordic Reservoir DOM, NR-DOM, catalogue number:  
57 1R108N). The aromatic rich NR-DOM extract was selected for the halogenation of a DOM  
58 extract experiments. A NR-DOM stock solution (100 mg C L<sup>-1</sup>) was prepared by dissolving  
59 the NR extract powder in water and filtration through a 0.45 µm membrane filter. A series of

60 NR-DOM working solutions (approximately 1 to 8 mgC L<sup>-1</sup>) were prepared and their DOC  
 61 concentrations determined by the UV/persulfate oxidation method using a Shimadzu TOC-  
 62 V<sub>ws</sub> Total Organic Carbon Analyser. A stock aqueous bromide solution was 1 g L<sup>-1</sup> (12.5  
 63 mM). A stock aqueous sulphite solution for quenching of oxidant residuals was 1.3 g L<sup>-1</sup> (10  
 64 mM).

65  
 66  
 67 **Table S2** The impact of the number and repetitions of gas line washing on recoveries of  
 68 selected model compounds.

Gas Line Washing		Final Absorber Volume (mL)	Concentration Factor <sup>*)</sup>	Recovery (%)		
Number of Washes	Time (s)			TCP	TBP	IP
1x	0.1	5.37 ± 0.15	9.31	78 ± 2	80 ± 3	84 ± 4
1x	0.5	5.96 ± 0.08	8.39	89 ± 1	92 ± 4	86 ± 2
1x	1.0	6.71 ± 0.18	7.45	89 ± 4	91 ± 1	87 ± 4
2x	0.1	5.60 ± 0.00	8.93	88 ± 6	90 ± 3	86 ± 4
2x	0.5	6.82 ± 0.15	7.33	88 ± 1	89 ± 1	84 ± 2
2x	1.0	8.12 ± 0.13	6.16	91 ± 6	91 ± 4	85 ± 1

69 <sup>\*)</sup> Volume of sample (50 mL) divided by final absorber volume; TCP: 2,4,6-trichlorophenol;  
 70 TBP: 2,4,6-tribromophenol; IP: 2-iodophenol (concentration of each halophenol in the sample was 100 µg L<sup>-1</sup>).

71  
 72  
 73 **Table S3** Averages and ranges of some water quality characteristics of the raw groundwater  
 74 blends at GWTP1 over a time period of approximately 3 years (2006-2009) (WCWA, 2009),  
 75 and the concentrations of these water quality parameters on 28 May 2012.

Water sample	Raw water			
	Min	Max	Average	28 May 2012
DOM concentration (mgC L <sup>-1</sup> )	5.6	25.1	9.6	9.4
Bromide concentration (µg L <sup>-1</sup> )	420	1020	760	1350

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 78

79 **Table S4** Physical and chemical properties of selected model compounds, as well as their  
 80 recoveries through the optimised halogen-specific TOX method.

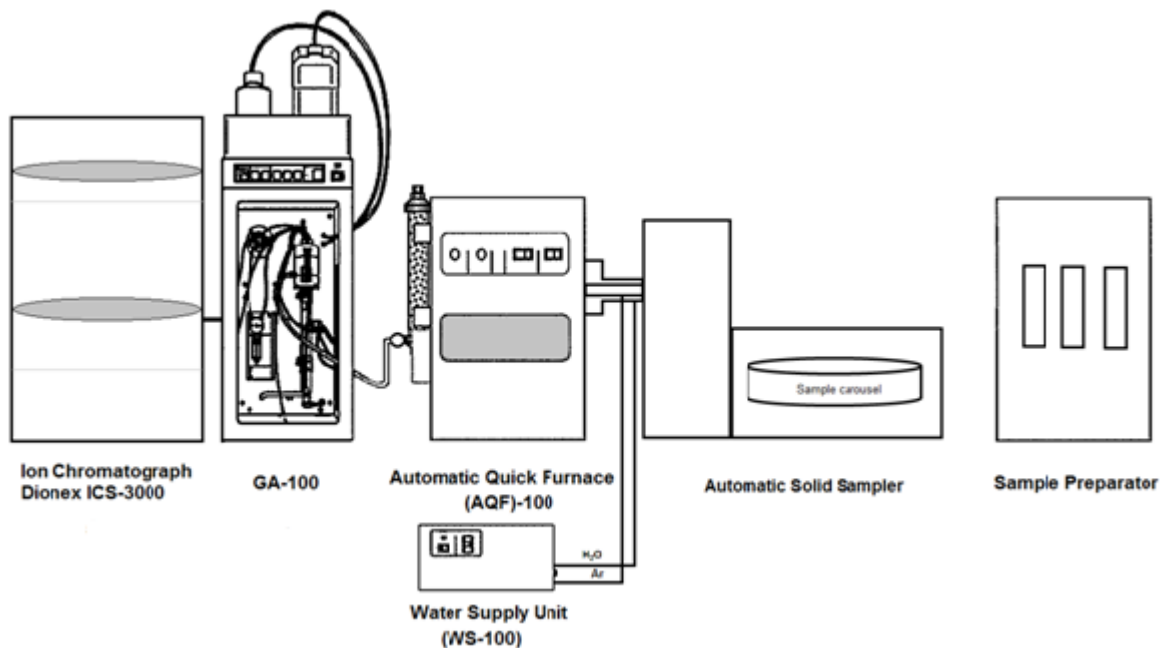
No.	Compound	MW (g mol <sup>-1</sup> )	log K <sub>ow</sub>	pK <sub>a</sub>	Recovery (%) <sup>**</sup>		
					TOCl	TOBr	TOI
<b>Haloacetic Acids</b>							
1	Chloroacetic acid	94.5	0.34	2.86	78 ± 6 (96 ± 2) <sup>a</sup> (92 ± 4) <sup>b</sup> (56) <sup>c</sup> (35) <sup>d</sup>		
2	Dichloroacetic acid	128.9	0.52	1.35	110 ± 12 (101 ± 5) <sup>b</sup>		
3	Chlorodibromoacetic acid	252.3	1.62		80 ± 10	97 ± 2	
4	Trichloroacetic acid	163.4	1.44	0.66	85 ± 4 (97 ± 4) <sup>b</sup> (109) <sup>c</sup> (83) <sup>d</sup>		
5	Bromoacetic acid	138.9	0.43	2.86		95 ± 4	
6	Bromochloroacetic acid	173.4	0.61		94 ± 4 (109 ± 2) <sup>a</sup> (100 ± 5) <sup>b</sup>	111 ± 4 (110 ± 0.6) <sup>a</sup> (100 ± 5) <sup>b</sup>	
7	Bromodichloroacetic acid	207.8	1.53		87 ± 6	92 ± 8	
8	Dibromoacetic acid	217.9	0.70			95 ± 6 (101 ± 4) <sup>b</sup>	
<b>Haloacetonitriles</b>							
9	Bromoacetonitrile	120.0	0.20			108 ± 2 (127 ± 2) <sup>a</sup>	
10	Dibromoacetonitrile	198.8				107 ± 6	
11	Chloroacetonitrile	75.0	0.11		80 ± 8 (85 ± 10) <sup>a</sup>		
12	Dichloroacetonitrile	109.9			105 ± 4		
13	Bromochloroacetonitrile	154.4			135 ± 15 (126 ± 20) <sup>a</sup>	118 ± 10 (113 ± 0.3) <sup>a</sup>	
14	Trichloroacetonitrile	144.4			115 ± 10 (124 ± 2) <sup>a</sup>		
<b>Chlorophenols</b>							
15	2-Chlorophenol	128.6	2.16	8.3	101 ± 6 89 ± 4		
16	4-Chlorophenol	128.6	2.16	9.2	(90.7) <sup>c</sup> (99) <sup>d</sup>		
17	2,6-Dichlorophenol	163.0	2.80	7.7	93 ± 8 91 ± 5		
18	2,4,6-Trichlorophenol <sup>*</sup> )	197.5	3.58	6.25	(104 ± 4) <sup>a</sup> (84) <sup>d</sup>		
19	Pentachlorophenol	266.3	4.74		82 ± 12		
<b>Bromophenols</b>							

20	4-Bromophenol	173.0	3.40		99 ± 2 (99.2) <sup>c</sup> (96) <sup>d</sup>
21	2,4-Dibromophenol	251.9	3.29	7.71	83 ± 6 (108 ± 0.9) <sup>a</sup>
22	2,4,6-Tribromophenol <sup>*)</sup>	330.8	4.18	5.97	91 ± 2 (102 ± 4) <sup>a</sup>
<b>Iodophenol</b>					
23	2-iodophenol <sup>*)</sup>	220.0	2.68	8.41	85 ± 1 (96 ± 4) <sup>a</sup> (98) <sup>d</sup>
<b>Halogenated benzenes</b>					
23	Bromobenzene	157.0	2.88		109 ± 6 (113 ± 6) <sup>a</sup> (79.8) <sup>c</sup>
24	1,2-Dichlorobenzene	147.0	3.28	94 ± 4 (40.6) <sup>c</sup>	
25	1,4-Dibromobenzene	235.9	3.77		98 ± 2 (93 ± 3) <sup>a</sup> (46.1) <sup>c</sup> (49) <sup>d</sup>

81 <sup>\*)</sup> Halophenol standards

82 <sup>\*\*) numbers in brackets refer to recovery values reported in references: <sup>a</sup>(Kristiana et al.,  
83 2015), <sup>b</sup>(Hua and Reckhow, 2006), <sup>c</sup>(Brandt and Kettrup, 1987), <sup>d</sup>(Oleksy-Frenzel et al.,  
84 2000).</sup>

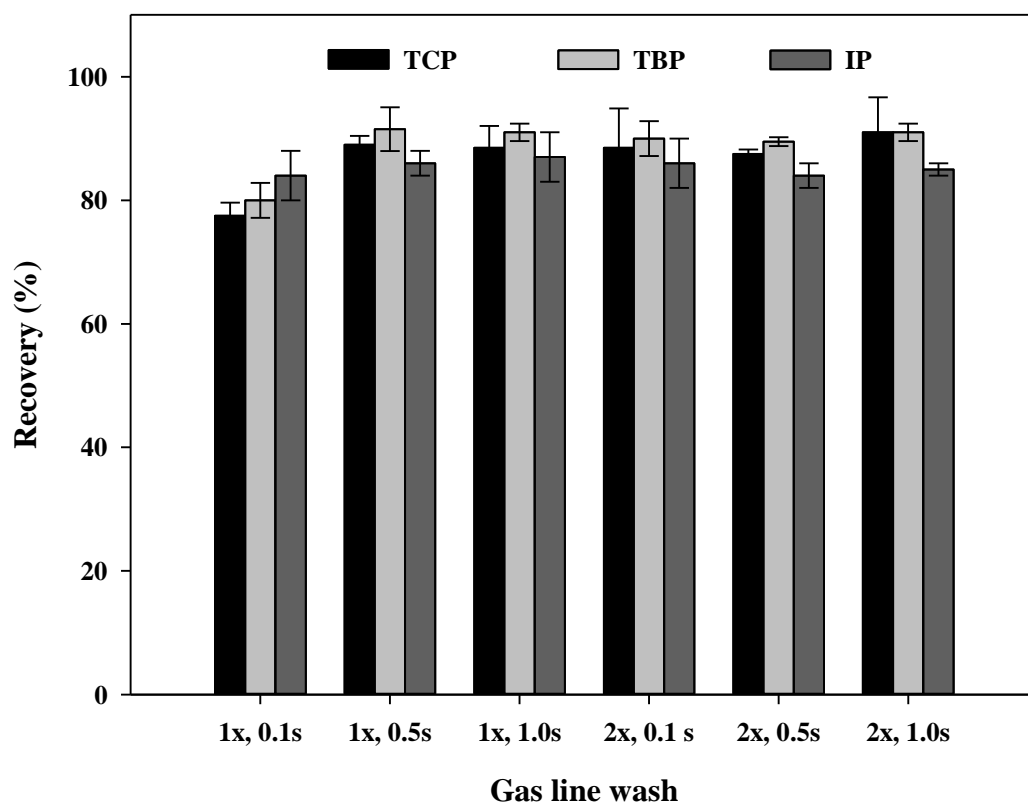
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87 **Figure S1** Schematic Diagram of Automatic Quick Furnace (AQF-100) with online Ion  
88 Chromatography and off-line Sample Preparator (after Kristiana et al. (2015)).

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90

91 **Figure S2** Recoveries of model compounds when different numbers of washes for different  
 92 lengths of time in the gas line between the combustion unit and the absorber unit were used.  
 93 TCP: 2,4,6-trichlorophenol, TBP: 2,4,6-tribromophenol, IP: 2-iodophenol (concentration of  
 94 each halophenol in the sample was 100  $\mu\text{g L}^{-1}$ ).

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