# WA School of Mines: Minerals, Energy and Chemical Engineering Faculty of Science and Engineering

# Engineering of Perovskite Oxides for Electrochemical Water Splitting

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# Declaration

To the best of my knowledge and belief this thesis contains no material previously published by any other person except where due acknowledgment has been made.

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### Abstract

Electrochemical water splitting represents a viable process that can address humanity's growing concerns over climate change caused by the excessive use of conventional fossil fuels, because it can produce hydrogen as a cleaner fuel using electricity generated from renewable energy sources (e.g., solar and wind). However, the implementation of water electrolysis is often hindered by the energy losses associated with the slow kinetics of the two half-reactions involved, i.e., the hydrogen evolution reaction (HER) at the cathode and the oxygen evolution reaction (OER) at the anode. To make these processes more energy-efficient and cost-effective, active electrocatalysts made of inexpensive, Earth-abundant elements are urgently needed. Among many candidates, ABO<sub>3</sub> perovskite oxides have recently emerged as promising low-cost alternatives for catalyzing both the HER and OER. This study centers on the engineering of perovskite oxides towards increased electrocatalytic HER/OER performance. Novel perovskite oxides consisting of non-precious elements are synthesized using facile chemical approaches such as sol-gel process and hightemperature reduction. Their physicochemical properties are investigated using a set of materials characterization techniques based on diffraction, microscopy, spectroscopy, and others. The electrocatalytic performance is assessed in a rotating disk electrode-based, three-electrode configuration using electrochemical testing methods ranging from cyclic voltammetry, linear sweep voltammetry, to chronopotentiometry. By fine-tuning the chemical compositions and structures, perovskite oxides with improved HER/OER catalytic performance are developed. Of importance, correlations are established between the electrocatalytic activity and the perovskite electronic structure (e.g., crystal symmetry, transition metal oxidation state, oxygen vacancy, and metal-oxygen covalency). This thesis is expected to offer a deepened understanding of the structure-activity relationship of the perovskite oxide electrocatalysts in the water-splitting reactions.

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## List of publications

#### Published papers and book chapters:

- Xiaomin Xu, Yangli Pan, Yijun Zhong, Lei Ge, San Ping Jiang, Zongping Shao\*, From scheelite BaMoO<sub>4</sub> to perovskite BaMoO<sub>3</sub>: Enhanced electrocatalysis toward the hydrogen evolution in alkaline media, Composites Part B: Engineering, 198 (2020): 108214.
- Yangli Pan<sup>#</sup>, Xiaomin Xu<sup>#</sup> (<sup>#</sup> Equal contribution), Yijun Zhong, Lei Ge\*, Yubo Chen, Jean-Pierre Marcel Veder, Daqin Guan, Ryan O'Hayre, Mengran Li, Guoxiong Wang, Hao Wang, Wei Zhou, Zongping Shao\*, Direct evidence of boosted oxygen evolution over perovskite by enhanced lattice oxygen participation, Nature Communications, 11 (2020): 2002.
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#### **Manuscripts in preparation:**

- 1. Xiaomin Xu, Zongping Shao\*, et al., Fe-based perovskites for catalyzing the hydrogen evolution reaction in alkaline solutions, In Preparation.
- 2. Xiaomin Xu, Zongping Shao\*, et al., An unusually stabilized Co-based perovskite for highly efficient oxygen evolution, In Preparation.
- 3. Xiaomin Xu, Zongping Shao\*, et al., Alkali-metal-doped perovskites for efficient oxygen evolution in alkaline solutions, In Preparation.

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## **Chapter 1 Introduction**

#### 1.1 Background\*

Moving into the 2020s, humanity continues to face formidable challenges from energy and the environment. According to the International Energy Agency,<sup>1</sup> world primary energy demand in 2017 reached  $5.8 \times 10^8$  TJ (terajoule, 1 TJ =  $10^{12}$  J), of which fossil fuels (oil, coal, and natural gas) have a major share of more than 80% (about 81%). Projections indicate that with the growth in population and economy, this energy demand will further increase to 7.4 or  $8.1 \times 10^8$  TJ in 2040 under the "New Policies Scenario" or "Current Policies Scenario", respectively, with a corresponding increase in carbon dioxide (CO<sub>2</sub>) emissions from 32.6 Gt (gigatonne, 1 Gt =  $10^9 t = 10^{12}$  kg) in 2017 to 35.9 or 42.5 Gt in 2040.<sup>1</sup> As a consequence, great concerns have been raised regarding the environmental issues associated with the continued use of fossil fuels, for example, global warming.

One way to address the energy and environmental problems is to utilize renewable energy sources, such as solar and wind, to power our planet.<sup>2</sup> For instance, solar power is by far the most abundant source of renewable energy. It is approximated that the Earth's surface receives  $1.2 \times 10^5$  TJ of solar energy at every second,<sup>3</sup> meaning that with just 1–2 hours of direct sunlight, one could collect enough energy to satisfy the global energy demand for one entire year. However, solar or wind supplies power only when the sun shines or wind blows. To overcome the problem of energy supply intermittency, energy storage technologies will be required.

\* This Background section contains text extracts form published works of the author. These text extracts are reprinted (adapted) with permission from Xiaomin Xu, Yangli Pan, Yijun Zhong, Ran Ran, Zongping Shao, Ruddlesden–Popper perovskites in electrocatalysis, Materials Horizons, 2020, 7, 2519–2565. Copyright (2020) The Royal Society of Chemistry; and Xiaomin Xu, Wei Wang, Wei Zhou, Zongping Shao, Recent advances in novel nanostructuring methods of perovskite electrocatalysts for energy-related applications, Small Methods, 2018, 2, 1800071. Copyright (2018) WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim. The existing energy storage technologies, with many commercial installations worldwide, are largely based on mechanical energy storage, such as pumped-storage hydroelectricity (i.e., pumped hydro),<sup>4</sup> compressed air energy storage,<sup>5</sup> and flywheels.<sup>6</sup> According to statistics, the world's total installed capacity of pumped hydro was about  $1.3 \times 10^5$  MW (megawatt, 1 MW =  $10^6$  W) in 2010, accounting for 99% of the worldwide storage capacity.<sup>7,8</sup> When coupled with the renewable energy sources, these mechanical energy storage technologies, in particular pumped hydro, can bring about reduced emissions.<sup>9</sup> Nonetheless, these currently available technologies can be dependent on limited resources or geographic locations and thus may not be affordable for or accessible to all users.<sup>10</sup> As an alternative, electrochemical energy storage represents an excellent platform for the integration of renewable resources. For example, battery technologies including sodium-sulfur batteries, redox-flow batteries, and lithium-ion batteries have been commercialized in grid storage, stationary storage, and portable electronics and electric vehicles, respectively.<sup>8</sup> Despite their different operational characteristics, these battery technologies face several common challenges for further development, including the enhancement in performance, reduction in cost, and improvement in safety.

Recently, electrochemically storing renewable energy in chemical products of global importance has been proposed to be a feasible and promising option.<sup>11</sup> For instance, the electrochemical reduction of water (H<sub>2</sub>O), nitrogen (N<sub>2</sub>), and CO<sub>2</sub>,<sup>12-14</sup> which are universal feedstocks provided by the Earth's atmosphere, can produce a large variety of energy carriers (hydrogen (H<sub>2</sub>), ammonia (NH<sub>3</sub>), and carbon-containing species such as carbon monoxide (CO), hydrocarbons, and alcohols) that enable the storage of renewables-derived electricity in the form of chemical energy. These electrochemical transformations can be facilely realized using an electrolysis cell under (near) ambient conditions, allowing the on-site production of chemicals at a reduced capital cost. Furthermore, the chemicals produced can be employed as sustainable fuels in electrochemical devices such as fuel cells to generate electrical energy,<sup>15,16</sup> which offers a cleaner alternative for power generation compared to the combustion of fossil fuels.

Among the various electrochemical conversions, the electrochemical reduction of water, which is more often called the electrochemical water splitting or water electrolysis, is considered a key approach for renewable energy conversion and storage

because it can convert the electricity generated from renewable energy sources into hydrogen as a carbon-neutral fuel. In water splitting, water is split into oxygen and hydrogen according to the equation  $H_2O \rightarrow 1/2O_2 + H_2$ . This reaction is a thermodynamically uphill process that necessitates an energy input of 286 kJ mol<sup>-1</sup> at room temperature and pressure. As an equivalent of this energy input, a minimum theoretical voltage of 1.229 V (often approximated to 1.23 V) is required to drive the water splitting at room temperature.<sup>12</sup> However, the practical operation of water electrolysis is often hampered by the slow kinetics of the two half-reactions, namely the hydrogen evolution reaction (HER) at the cathode and the oxygen evolution reaction (OER) at the anode. To further accelerate these reactions, additional energy input, which manifests as a need for a potential larger than their equilibrium potential (i.e., 0 and 1.23 V vs. the reversible hydrogen electrode for HER and OER, respectively), is required. This gap of potential applied is normally termed the overpotential  $(\eta)$ . In order to lower this overpotential and make the water-splitting process more energy-efficient, electrocatalysts have to be introduced to the water electrolysis system, on both the anode and the cathode. The state-of-the-art electrocatalysts for the OER and HER often involve noble metals, for example, platinum for the cathodic HER,<sup>17</sup> and iridium or ruthenium (or their oxides) for the anodic OER.<sup>18</sup> Due to the low abundance and prohibitive cost of these catalysts, increasing research efforts are focusing on nonprecious metal-based alternatives.

Among many candidates, perovskite oxides have emerged as a large family of functional materials that show great potential for catalyzing the OER,<sup>19-22</sup> as well as the HER in alkaline media.<sup>23-25</sup> **Figure 1.1** gives a schematic representation of the perovskite oxide structure in an ideal cubic symmetry. With a formula generally expressed as ABO<sub>3- $\delta$ </sub>, the A-site is typically a rare-earth or an alkali whereas the B-site is often a transition metal, occupying the 12-fold and 6-fold coordination sites, respectively. Compared to other catalytic materials, perovskite oxides feature low cost, facile synthesis, and easiness for scale-up. More importantly, perovskite oxides are known for their compositional and structural tunability. The perovskite structure can allow the incorporation of almost 90% of the elements within the "Periodic Table of Elements" by partial substitution of elements at A- or/and B-, or O-site.<sup>26</sup> Meanwhile, the oxygen nonstoichiometry ( $\delta$ ) can vary within a large range. Such flexibility in composition and structure gives rise to the tunable electronic structure of perovskites,

exhibiting diverse physical and chemical properties that can be utilized to design highly efficient electrocatalysts toward both the OER and HER.



**Figure 1.1** A schematic showing the crystalline structure of the ABO<sub>3</sub> perovskite with an ideal cubic symmetry.

#### **1.2 Research objectives**

While recent years have witnessed great progress in the development of perovskitebased water splitting electrocatalysts, there is much room for further advances in terms of activity improvement, stability enhancement, and cost reduction. This thesis aims to develop non-precious metal-based perovskite oxides as the electrocatalysts for facilitating the HER and OER kinetics in electrochemical water splitting. Taking advantage of the compositional and structural diversity, strategies are adopted to tune the chemical composition and engineer the crystal structure of perovskites oxides, which serve as useful means to modify their electronic structures. Based on these strategies, perovskites with new compositions, reduced costs, and improved performance are designed and fabricated. Their functionality in the electrocatalytic HER/OER is evaluated and the structure–activity relationship is investigated. The specific objectives of this thesis are listed as follows.

- To summarize the current research status of perovskite oxides as the electrocatalysts for electrochemical water splitting.
- To expand the compositional space of perovskite oxides and to investigate the efficacy of molybdenum-based perovskite oxides as electrocatalysts for the HER.

- To explore iron-based perovskite oxides as alternatives to cobalt-based ones for catalyzing the HER and to study their structure–activity correlations.
- To boost the electrocatalytic OER performance of an existing cobalt-based perovskite oxide through stabilizing an unusually obtained phase structure and to investigate the structural effects on the OER electrocatalysis.
- To improve the activity and stability of iron-based OER perovskite catalysts by alkali-metal substitution and to understand the origins of the enhanced performance.

#### 1.3 Thesis organization

This thesis consists of eight chapters. Chapter 1 introduces the research background and outlines the thesis structure. Chapter 2 provides a literature review on the recent progress of perovskite-based water-splitting catalysts. Chapter 3 details the experimental methodologies used in this thesis. Chapters 4–7 offer the results and discussion of the experimental studies. Chapter 8 presents the conclusions and provides perspectives for future research. The specific contents of these chapters are also summarized as follows.

#### Chapter 1: Introduction

This chapter provides the global energy context under which the research in this thesis is conducted. It also briefly introduces the background of electrochemical water splitting, the two half-reactions involved, and the perovskite oxides. The thesis objectives and organization are also provided.

#### Chapter 2: Literature review

This chapter presents a thorough review on the fundamentals and applications of perovskite oxides as the electrochemical water splitting catalysts. The materials design strategies to tune the perovskite structure are also discussed.

#### Chapter 3: Methodologies and characterizations

This chapter summarizes the materials synthesis, characterizations, and electrochemical measurements used throughout the experimental studies involved in this thesis.

Chapter 4: From scheelite BaMoO<sub>4</sub> to perovskite BaMoO<sub>3</sub>: Enhanced electrocatalysis toward the hydrogen evolution in alkaline media

This chapter evaluates the use of a molybdenum based BaMoO<sub>3</sub> perovskite oxide, synthesized from the conversion of a BaMoO<sub>4</sub> scheelite oxide under a reductive condition, as the HER electrocatalyst in alkaline media. The activity improvement is discussed based on considerations of structural changes.

Chapter 5: Fe-based perovskites for catalyzing the hydrogen evolution reaction in alkaline solutions

This chapter focuses on iron-based perovskites as the HER electrocatalysts, using an alkaline-earth metals Ba and Sr co-doped La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> series (x = 0.0, 0.2, 0.5, 0.8, and 1.0) as the research target. The effect of the Ba/Sr substitution on the phase structure, Fe oxidation state, and Fe–O bond covalency is discussed and correlated with the catalytic activity.

# Chapter 6: An unusually stabilized Co-based perovskite for highly efficient oxygen evolution

This chapter reports a new methodology for the stabilization of a cobalt-based cubicstructured perovskite from a hexagonal-structured perovskite and evaluates their electrocatalytic activity for the OER in alkaline solutions. The influence of this phase transformation on the perovskite electronic structure and the OER activity is explored.

# Chapter 7: Alkali-metal-doped perovskites for efficient oxygen evolution in alkaline solutions

This chapter concerns a new doping strategy using alkali metals as the dopants and addresses the unsatisfactory performance of iron-based perovskite OER electrocatalysts. Utilizing a model catalyst of LaFeO<sub>3</sub>, monovalent Na<sup>+</sup> was doped into the system to partially replace trivalent La<sup>3+</sup>. The changes induced by the Na-doping, including Fe valence, Fe–O covalency, and oxygen vacancy content, are discussed and related to the electrocatalytic performance.

#### Chapter 8: Conclusions and perspectives

This chapter concludes with the major achievements of this thesis and proposes some interesting topics of further research.

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## **Chapter 2 Literature review\***

#### 2.1 Abstract

Electrocatalysis-based technologies are central to enabling the vision of a sustainable energy future. One major challenge is to develop nonprecious, high-efficient electrocatalysts that can promote the electrocatalytic processes. Perovskite materials have recently been extensively studied as alternative electrocatalysts to noble metalbased materials owing to their low cost, tunable structure, and high catalytic activity. This chapter discusses perovskite materials in electrocatalysis for several important reactions, including the oxygen reduction reaction, oxygen evolution reaction, and hydrogen evolution reaction. The electrocatalytic mechanisms are first introduced to offer a fundamental understanding of the electrocatalysis occurring on the surface of perovskite catalysts. Following this is a detailed description of the rational design of perovskite materials toward efficient electrocatalysis. Several activity descriptors for theoretically guiding the catalyst design are presented while many other practical parameters that can influence the catalyst behavior are also highlighted. In addition, concerns for the catalyst stability under realistic electrochemical conditions are expressed. In an effort to realize global energy sustainability, several key applications of perovskite materials in electrocatalysis-related energy devices, for example, metalair batteries and water electrolyzers, are presented, with an emphasis on how to enable the widespread penetration of these energy technologies.

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#### **2.2 Introduction**

Driven by pressing concerns over the growing energy demands, depleting fossil fuels, and impending climate change, one grand challenge facing humanity today is how to power the planet with renewable energy sources (e.g., wind and solar). Renewable energy is plentiful but tends to be intermittent in nature as the wind is not always blowing and the sun is not always shining. One prospective option to address the issue of energy supply intermittency is to develop electrochemical devices that can utilize electricity produced from renewable energy to enable the transformations between electrical energy and chemical energy. For example, in water electrolyzers, water molecules are split into hydrogen, which is a clean energy carrier that can be used in fuel cells to generate electricity. In fuel cells or metal-air batteries, the oxidation of hydrogen or metals is coupled with the reduction of oxygen to convert chemical energy into electrical energy. Unfortunately, these energy conversion technologies have low efficiency because of the sluggish kinetics of several key reactions involved. For instance, the overall efficiency of water electrolysis is dominated by the hydrogen evolution reaction (HER) at the cathode and the oxygen evolution reaction (OER) at the anode [1]. Likewise, the efficiency of rechargeable metal-air batteries is strongly dependent on the oxygen reduction reaction (ORR) during discharge and the OER during charge [2]. Increasing the efficiency of these devices would therefore necessitate the role of electrocatalysis to modify the rate of the relevant chemical reactions via the assistance of electrocatalysts that are active and stable.

The term "electrocatalysis" is generally referred to as a type of catalysis that leads to the change of the rate of an electrochemical reaction taking place at the interface between an electrode and an electrolyte. Despite its high relevance to renewable energy technologies, our current knowledge about the fundamental mechanisms underlying electrocatalysis is still inadequate. For instance, mechanistic insights into the OER is limited to theoretical understanding only, due to the complexity in this multi-step four-electron reaction which lacks experimental observation on the details of electrode interfaces under realistic operating conditions. Nonetheless, years of intense academic research have seen significant breakthroughs in the development of electrocatalysts that can substantially lower the overpotential associated with the electrochemical reactions. While noble metal-based materials (e.g., Pt-, Ir-, and Rubased materials) normally show optimum catalytic activity [3,4], their widespread penetration into clean energy devices is hindered by their low abundance and high cost, which does not conform to the vision of a sustainable energy future. Hence tremendous efforts have been devoted to the search for a wide range of inexpensive alternatives that consist of Earth-abundant elements. These include metals [5], oxides [6-8], (oxy)hydroxides [9,10], chalcogenides [11], non-metal carbon materials [12], and metal-organic frameworks [13], to name just a few.

Of all the candidates, perovskite materials have recently emerged as a new family of low-cost, high-efficient nonprecious metal catalysts for catalyzing relevant reactions including the ORR, OER, and HER [14]. Perovskites are known for their versatility in chemical, crystal, and electronic structures [15]. With a nominal formula generally expressed as ABO<sub>3</sub>, the perovskite chemical structure can accommodate nearly 90% of the elements within the "Periodic Table of Elements" by partial substitution of elements at A or/and B sites, while also allowing a changeable stoichiometry at the O site [16]. In addition, a range of perovskite derivatives with varied crystal structures, including double perovskite, layered perovskite, and quadruple perovskite, further add to the diversity of the perovskite family. This flexibility gives rise to the tunability in the electronic structure of perovskites, making them ideally suited for the study of the structure-performance relationship in electrocatalysis. In oxygen electrocatalysis, a veritable explosion of research activity targeting the development perovskite catalysts has been observed. On the other hand, the role of perovskites in the field of hydrogen electrocatalysis is less explored and has been gaining growing attention until recently. In this chapter, we mainly focus on perovskite materials for the electrocatalysis toward the ORR, OER, and HER reactions. Considering that perovskite oxides are typically stable in alkaline media and can dissolve in acids, this chapter will primarily deal with those that work in alkaline environments unless otherwise stated. The electrocatalytic mechanisms are first introduced to offer a clear picture of the reactions taking place on perovskite catalysts. This is followed by a detailed discussion on the rational design of perovskite materials toward efficient electrocatalysis, which focuses on both catalytic activity and stability. In the context of the pursuit of a sustainable future of energy, we also present applications of perovskite materials in electrocatalysis-related energy devices which can enable efficient use of renewable energy.

#### 2.3 Mechanisms in electrocatalysis on perovskite materials

Fundamental insights into the reaction mechanisms is a vital step toward understanding electrocatalysis on catalyst surfaces. Due to the complex interaction at the electrode interface, there is no single governing mechanism that unifies all electrocatalytic reactions. Even for the same reaction of interest, the mechanisms can differ with catalyst chemistries. Taking the OER in alkaline media as an example, onemetal-site mechanisms have been proposed for noble metals [17], dimeric molecules [18], and perovskite oxides [19], whereas distinct two-metal-site mechanisms have been introduced for the oxygen evolving complex of photosystem II [20] and electrodeposited oxides [21]. In this section, only the conventional mechanisms (which are considered the most favorable) underlying the oxygen and hydrogen electrocatalysis on perovskite surfaces are highlighted.

#### 2.3.1 Oxygen electrocatalysis

Conventionally, the ORR reaction in alkaline solutions can be written as  $O_2 + 2H_2O +$  $4e^- \rightarrow 4OH^-$ . Previous experimental and computational studies show that the ORR on perovskite oxides is a consecutive, four-step, proton-coupled electron transfer process taking place on single surface metal sites [22,23]. These four sequential steps are 1, hydroxide displacement; 2, peroxide formation; 3, oxide formation; and 4, hydroxide regeneration as shown in Figure 2.1a [22]. In these reaction pathways, molecular O<sub>2</sub> or H<sub>2</sub>O from the electrolyte and electron interact with surface metal sites to generate four different oxygenated adsorbates including OO\*, OOH\*, O\*, and OH\* (\* denotes a reactive site on the catalyst surface), which is accompanied by the oxidation and reduction (redox) of surface metal sites whose oxidation state changes between n+ and n+1. Energetically, the ORR reaction kinetics are largely determined by the binding energy of oxygen and the surface metal sites; too weak of an oxygen binding energy leads to the first OH\*-to-OO\* displacement step being the rate-determining step (RDS), whereas too strong of an oxygen binding energy renders the last O\*-to-OH\* transition step being rate-limiting [23]. An optimal perovskite catalyst binds to oxygen neither too weakly nor too strongly, which is commonly referred to as the Sabatier principle. For perovskite oxide surfaces that follow the same one-metal-site mechanism, the binding energies of the different reactive oxygen adsorbates involved in the ORR are highly correlated due to scaling relations [24,25], which is the origin of the nonzero theoretical overpotential observed among many catalysts.



**Figure 2.1** (a) Four-step ORR mechanism on the surface of perovskite oxide catalysts in alkaline solutions. (b) Four-step OER mechanism on the surface of perovskite oxide catalysts in alkaline solutions. (Reprinted with permission from Ref. [22]. Copyright 2017 Elsevier Inc.)

In a similar vein, the OER reaction on perovskite oxides in alkaline media, which can be written as  $4OH^- \rightarrow O_2 + 2H_2O + 4e^-$ , proceeds via four proton-coupled electron transfer steps including 1, hydroxide deprotonation; 2, peroxide formation; 3, peroxide deprotonation; and 4, hydroxide regeneration (Figure 2.1b) [22]. In this mechanism, hydroxyl ions (OH<sup>-</sup>) from the electrolyte interacts with surface metal sites, resulting in the redox of the metal (with the oxidation state switching between n+ and n+1). The reactive intermediates generated for the OER in base are the same as those for the ORR, which are however in a different sequence of O\*, OOH\*, OO\*, and OH\*. Similar to the ORR, the OER reaction kinetics are primarily controlled by the oxygen binding strength on surface metal sites. For metal sites that bind oxygen too weakly, the second O\*-to-OOH\* peroxide formation step is rate-limiting. On the other hand, for metal sites that bind oxygen too strongly, the RDS may be the third OOH\*-to-OO\* peroxide deprotonation step [26]. The binding strength of the surface oxygen adsorbates is found to obey a scaling relation [27], analogous to the case of perovskites for the ORR, again hampering the development of a perovskite OER catalyst with zero overpotential. While the conventional OER mechanism considers surface metal as the sole reactive site, novel mechanisms that involve the participation of lattice oxygen have recently been proposed [28-32].

Note that the intermediate adsorbates on perovskite oxide surfaces in the abovementioned ORR/OER mechanisms are not identical to those on metal surfaces in relevant mechanisms proposed based on density functional theory (DFT) calculations. Despite having similar elementary reaction steps, the ORR on metal surfaces involves a series of intermediates in the order of O<sub>2</sub>\*, OOH\*, O\*, and OH\* [24], whereas the OER on metal surfaces involves a sequence of intermediates of OH\*, O\*, OOH\*, and  $O_2^*$  [17]. This difference can be rationalized from the different surface properties of metal surfaces and perovskite oxide surfaces, the latter being able to adsorb negatively charged species (such as OH<sup>-</sup>) in alkaline conditions at the initial stage of electrocatalysis [33]. Such difference also points to the diversity in reaction mechanisms that have been proposed for oxygen electrocatalysis, which again highlights the complexity of the oxygen chemistries on catalyst surfaces. To date, due to the underdeveloped time-resolved techniques, experimentally accessing the reaction intermediates on perovskite oxide surfaces remains a formidable challenge. Theoretically, to gain a better mechanistic understanding of the oxygen electrocatalysis, interested readers can resort to the pioneering DFT works by Rossmeisl et al. [17,27,34] and Nørskov et al. [24,35,36].

#### 2.3.2 Hydrogen electrocatalysis

The overall reaction of the HER in basic solutions can be written as  $2H_2O + 2e^- \rightarrow H_2 + 2OH^-$ . Generally, the alkaline HER is a two-step electron transfer process, and may occur via either the Volmer-Heyrovsky mechanism or the Volmer-Tafel mechanism [37,38]:

Volmer reaction:	$* + H_2O + e^- \rightarrow H^* + OH^-$	(1)
Heyrovsky reaction:	$\mathrm{H}^{*} + \mathrm{H}_{2}\mathrm{O} + \mathrm{e}^{-} \rightarrow \mathrm{H}_{2} + \mathrm{O}\mathrm{H}^{-} + *$	(2)
Tafel reaction:	$2H^* \rightarrow H_2 + 2^*$	(3)

Both reaction pathways include the same Volmer reaction, which involves adsorption of molecular  $H_2O$  on the empty reactive sites, electrochemical reduction of adsorbed  $H_2O$  into adsorbed hydrogen atoms (H\*) and OH<sup>-</sup>, desorption of OH<sup>-</sup> to refresh the catalyst surface and formation of H\* for  $H_2$  evolution.

While the conventional HER mechanism has been well established based on experimental and theoretical results on metal catalysts [39], little is known about the HER process on oxide surfaces, especially in alkaline environments [40,41]. Back in the 1990s, Goodenough et al. first experimentally observed the evolution of hydrogen on  $Sr_{1-x}NbO_{3-\delta}$  (0.05  $\leq x \leq 0.3$ ) perovskite oxides in strong acids [19]. Based on

electrochemical measurements, they proposed a possible HER reaction pathway and pointed out that the reactive site for the HER on perovskite oxides appears to be not the surface metal, but rather the surface oxygen anion. This is not unexpected considering that binding with positively charged metal cations would be kinetically unfavorable for H atoms. Very recently, Xu et al. showcased the efficacy of a  $Pr_{0.5}(Ba_{0.5}Sr_{0.5})_{0.5}Co_{0.8}Fe_{0.2}O_{3-\delta}$  perovskite oxide in catalyzing the HER in bases, and proposed a reaction mechanism for the alkaline HER as shown in **Figure 2.2** [42], similar to that for the HER in acids [19]. Note that the O site at the initial reaction state is not protonated here for the sake of simplicity. In this pathway, molecular H<sub>2</sub>O from the electrolyte and electron interact with a bridging oxygen site to form an adsorbed H\* intermediate, where one adjacent surface metal can be reduced or oxidized (with the oxidation state switching between n+1 and n). However, it remains difficult to determine whether the second step proceeds via the Heyrovsky reaction or the Tafel reaction.



**Figure 2.2** Two-step HER mechanism on the surface of perovskite oxide catalysts in alkaline solutions. (Reprinted with permission from Ref. [42]. Copyright 2016 John Wiley and Sons)

Unlike in the case of the ORR/OER with multiple reaction intermediates, the twoelectron HER involves only one intermediate (H\*). Thus, no scaling relation is observed and an ideal zero overpotential can be achieved on advanced catalysts (e.g., Pt) [11], which represents a goal for optimizing the perovskite electrocatalysts. The rate of the overall HER reaction is mainly dependent on the binding strength of the H\* intermediate, which is more commonly referred to as the hydrogen adsorption free energy ( $\Delta G_{\rm H}$ ) [43]. An optimal HER catalyst should bind to hydrogen neither too weakly nor too strongly, having a  $\Delta G_{\rm H}$  value close to zero.

#### 2.4 Rational design of perovskite materials toward efficient electrocatalysis

While the proposed reaction mechanisms can offer a fundamental understanding of the electrochemical processes occurring on perovskite materials, they do not have the power to screen perovskites with remarkable catalytic effects ("activity"). Given the large number of perovskite candidates and their many physical properties influencing the catalytic activity, it is necessary to realize the rational design of perovskite materials toward efficient electrocatalysis. Generally, the activity of an electrocatalyst can be improved by either increasing the intrinsic activity of each reactive site or increasing the number of reactive sites (extrinsic activity) [44]. A combination of these two strategies can lead to further enhancement in activity. To rationalize the design of improved perovskite catalysts, property-activity relationships that govern the intrinsic activity, which are often referred to as "activity descriptors", have been developed [45]. This section describes several important activity descriptors that have shown predictive power in discovering advanced perovskite catalysts, with a special emphasis on descriptors for the OER. Nonetheless, these descriptors have their limitations and do no hold universally for all perovskite materials across all catalytic reactions. Thus, specific design strategies that aim to increase the intrinsic or extrinsic activity (or both) are discussed, focusing on a range of parameters that can be tuned in perovskite oxides to promote the catalytic performance of the ORR, OER, and HER. In addition to high activity, robust stability represents another important issue for efficient electrocatalysts. To facilitate improved catalyst design, major concerns over the stability of perovskite materials during electrocatalytic processes are included in this section.

#### 2.4.1 Activity descriptors

As mentioned earlier, the reaction rate of the OER is primarily determined by the strongly correlated binding energy of oxygen intermediates. Based on this understanding, Rossmeisl et al. utilized DFT calculations to establish the difference

between the adsorption free energy of the O\* and OH\* intermediates ( $\Delta G_{O*} - \Delta G_{OH*}$ ) as a universal activity descriptor for the OER on perovskite oxide surfaces [27], with highest activity expected at a moderate binding of the oxygen intermediates. However, because of the experimental challenge in unambiguously distinguishing reaction intermediates, it is not straightforward to identify active perovskite catalysts using this descriptor. Directly related to the term  $\Delta G_{O*} - \Delta G_{OH*}$  is the redox potential of transition metal cations prior to the catalytic OER, which has recently been proposed as a simpler activity descriptor [22]. Unfortunately, this approach is limited by the difficulty in the assignment of the redox transition in perovskite oxides preceding the OER. Alternatively, activity descriptors from both molecular orbital theory and band theory have proved fruitful in guiding the design of perovskite materials as efficient electrocatalysts [23,26,46].

#### 2.4.1.1 Activity descriptors from molecular orbital theory

In the perovskite oxide structure, the B-site transition metal is six-fold coordinated to the oxygen to form an octahedron. In this octahedral environment, the transition metal d orbitals hybridize with the O 2p orbitals, forming  $\pi$ -bonding and  $\pi^*$ -antibonding (called  $t_{2g}$  orbital) where  $d_{xy}$ ,  $d_{yz}$ , and  $d_{xz}$  orbitals have a weak spatial overlap with adjacent O 2p orbitals, and  $\sigma$ -bonding and  $\sigma$ \*-antibonding (called eg orbital) where  $d_{x^2-y^2}$  and  $d_{z^2}$  orbitals have a strong spatial overlap with nearby O 2p orbitals. Molecular orbitals depicting the metal-oxygen electronic states can be used to explain the electrocatalytic phenomena in perovskite materials. Bockris and Otagawa were the first to use the d-electron number (both t<sub>2g</sub> and eg electrons) of transition metal cations as an activity descriptor to clarify the OER activity observed on  $ABO_3$  (B = Ni, Co, Fe, Mn, Cr, V) perovskites [47,48]. They found an inverse trend between the OER overpotential and the number of transition metal d electrons, which was concluded to play a major role in determining the binding strength of the OH\* adsorbate via the filling of the metal-OH antibonding orbitals. Similar to this finding, recent DFT calculations showed that the binding energy of possible OER adsorbates has a scaling relationship with the transition metal d-electron number and oxidation state of perovskite oxides [49].

In contrast to the d-electron descriptor from Bockris and Otagawa, a more appropriate activity descriptor from molecular orbital principles is the filling of eg orbital of surface

transition metal cations reported by Shao-Horn and co-workers [26]. Based on the consideration that the eg orbital has a higher overlap with a surface-anion adsorbate than does the t<sub>2g</sub> orbital, the occupancy of eg orbital can more directly influence the binding of adsorbed oxygen intermediates on surface transition metals and thus the OER activity. Through a systematic evaluation of more than 10 perovskite oxides with varying B-site elements in basic solutions, they demonstrated a volcano relationship between the OER activity (in terms of the overpotential needed to afford a 50  $\mu$ A cm<sup>-2</sup><sub>ox</sub> specific current density) and the eg filling of B-site ions (Figure 2.3a) [26,45]. For the left/right branch of the volcano, perovskites having too little/much eg orbital occupancy can result in too strong/weak interaction with oxygen intermediates, both leading to unfavorable OER activity. Sitting at the top of the volcano plot are perovskites with eg filling close to unity, offering optimum binding of reaction intermediates and high OER performance. This observation is consistent with the Sabatier principle. The volcano trend is observed on a number of perovskite oxides, over a voltage span of 0.3 V, and across four orders of magnitude, rendering eg-filling as a universally applicable descriptor of OER activity. This descriptor has allowed the identification of a range of active perovskite OER catalysts, including Ba0.5Sr0.5Co0.8Fe0.2O<sub>3- $\delta$ </sub> (BSCF) [26], SrNb0.1Co0.7Fe0.2O<sub>3- $\delta$ </sub> [50], Ca2Mn2O<sub>5</sub> [51],  $Ca_{0.9}Yb_{0.1}MnO_{3-\delta}$  [52], and  $CaCu_3Fe_4O_{12}$  [53]. More recently, the application of the eg-filling descriptor has been successfully extended to the screening of oxides with structures other than perovskite, for example, spinel [54] and rock salt [55] structures, for efficient OER electrocatalysts.



**Figure 2.3** The volcano relationship between (a) the OER activity or (b) the ORR activity in alkaline solutions, defined by the overpotential at a 50  $\mu$ A cm<sup>-2</sup><sub>ox</sub> specific current density, and the transition metal e<sub>g</sub> electron occupancy on perovskites. (Reprinted with permission from Ref. [45]. Copyright 2015 Royal Society of Chemistry)

In a similar fashion, plotting the ORR activity (in terms of the overpotential required to give a 50  $\mu$ A cm<sub>ox</sub><sup>-2</sup> specific current density) of 15 perovskite oxides in alkaline media versus the eg occupancy of surface transition metal cations can also obtain a volcano relationship as shown in **Figure 2.3b** [23,45]. Again, the perovskite ORR activity peaks at a near-unity filling of the eg orbital for LaNiO<sub>3</sub>, LaCoO<sub>3</sub>, and LaMnO<sub>3</sub>, outperforming LaCrO<sub>3</sub> (eg<sup>0</sup>) with too low an eg occupancy at the left branch of the volcano and LaFeO<sub>3</sub> (eg<sup>2</sup>) with too high an eg filling at the right branch. The eg-filling descriptor has seen success in discovering many efficient perovskite ORR catalysts, such as LaNi<sub>0.25</sub>CO<sub>0.75</sub>O<sub>3- $\delta$ </sub> [56], LaNi<sub>1-x</sub>Mg<sub>x</sub>O<sub>3</sub> [57], LaNi<sub>1-x</sub>Fe<sub>x</sub>O<sub>3</sub> [58], and La<sub>0.8</sub>Sr<sub>0.2</sub>Mn<sub>0.6</sub>Ni<sub>0.4</sub>O<sub>3</sub> [59]. In the case where an identical eg occupancy of B-site cations is observed in different perovskite materials, the transition metal–oxygen covalency is found to serve as a secondary activity descriptor [23,26]. For example, the ORR/OER activity of LaMnO<sub>3</sub>, LaCoO<sub>3</sub>, and LaNiO<sub>3</sub> (all having an electronic state of eg<sup>1</sup>) increases with the extent of the covalent mixing between transition metal ions and oxygen atoms in the order of LaMnO<sub>3</sub> < LaCoO<sub>3</sub> < LaNiO<sub>3</sub>.

Despite the usefulness of the molecular orbital-based  $e_g$ -filling as a universal descriptor for picking perovskite ORR/OER catalysts, this descriptor has its own limitations. On the one hand, molecular orbital theory only considers the transition metal as the reactive site, thus cannot efficiently capture the metal–oxygen covalency of highly covalent perovskite systems where both metal and oxygen can function as reactive sites [29,30]. On the other hand, the estimation of the  $e_g$  electron number, which is based on the transition metal oxidation state and spin state extracted from ex situ measurements, remains ambiguous. For instance, there has been an ongoing debate over the spin state of cobalt-based perovskites [60-64].

#### **2.4.1.2** Activity descriptors from band theory

The success of the eg-filling descriptor highlights the importance of catalyst electronic structure on the ORR/OER. In addition to molecular orbital theory, band theory can also offer insightful understanding of the electronic structure of catalyst materials. For example, previous theoretical works have correlated the catalytic activity of metal or alloy surfaces with the metal d-band center [65]. As for perovskite oxides, band descriptions (such as band width) have also been developed to describe the trend in oxygen electrocatalysis [66,67]. Very recently, Grimaud et al. reported a correlation between the computed O p-band center relative to the Fermi level and the OER activity of cobalt-based perovskites [46]. As depicted in Figure 2.4a, the electronic structure characteristics of perovskite oxides are more accurately captured by the more delocalized O p-band while the transition metal d-character is still reflected through hybridized density of states. The O p-band center of several double perovskite and single perovskite oxides, which was obtained from DFT calculations, was found to scale linearly with the OER performance (Figure 2.4b) [45,46]; the closer the O pband center to the Fermi level, the greater the OER activity. Despite acting as an alternative activity descriptor, the computed O p-band center remains to be verified by experimental investigations into the metal and oxygen states. Moreover, the universality of this activity descriptor needs to be testified on perovskite systems beyond cobalt-containing ones.



**Figure 2.4** (a) A schematic representation of the density of states for perovskite oxides, illustrating the O 2p and transition metal 3d bands. (Reprinted with permission from

Ref. [46]. Copyright 2013 Springer Nature) (b) The relationship between the OER activity in alkaline solutions, defined by the potential at a 0.5 mA cm<sub>ox</sub><sup>-2</sup> specific current density, and the O p-band center relative to the Fermi level for cobalt-based perovskite oxides including PrBaCo<sub>2</sub>O<sub>5+ $\delta$ </sub> (PBCO), HoBaCo<sub>2</sub>O<sub>5+ $\delta$ </sub> (HBCO), SmBaCo<sub>2</sub>O<sub>5+ $\delta$ </sub> (SBCO), GdBaCo<sub>2</sub>O<sub>5+ $\delta$ </sub> (GBCO), La<sub>0.4</sub>Sr<sub>0.6</sub>CoO<sub>3- $\delta$ </sub> (LSC46), and LaCoO<sub>3</sub> (LCO). (Reprinted with permission from Ref. [45]. Copyright 2015 Royal Society of Chemistry)

#### **2.4.2 Design strategies**

In spite of the success in the establishment of activity descriptors, they appear to be not explicit enough in guiding catalyst design and could present a challenge in transforming into more practical design strategies toward active perovskite electrocatalysts. In practice, the activity of a perovskite catalyst can be increased by two means. One is to take into account the electronic effects, aiming to intrinsically increase the activity of each reactive site. This can be achieved by regulating the physical/chemical properties related to the perovskite electronic structures, such as composition, oxygen vacancy, and crystal structure. The other is to consider the geometric effects that can extrinsically increase the number of reactive sites. This involves the search for novel methods to synthesize perovskite nanostructures or composites. This section covers catalyst design strategies based on these parameters, with special attempts to illustrate how each parameter can be separately tuned in perovskites for improved electrocatalysis. Note that these parameters are actually correlated to one another. For instance, changing the composition could affect the oxygen vacancy or crystal structure [29]. Moreover, there are cases when the intrinsic and extrinsic activity can be increased simultaneously. One example is that downsizing the perovskite oxides could also bring about changes in their electronic structure [68]. Considering the huge quantity of perovskites that have been studied thus far, it appears to be impractical to mention them all and thus only typical examples are given here. Other catalyst design parameters, such as strain [69-71] and conductivity [52,71-74], can also influence the electrocatalytic performance of perovskites. However, they are not included here given that they are currently less explored.

#### 2.4.2.1 Composition

Perovskite materials are known for their flexibility in chemical compositions. Elemental substitution on the A- or/and B-site can alter the electronic structure of the B-site transition metal, thereby modifying the electrocatalytic activity. Generally, a complex doped perovskite oxide can be described using the formula of  $A_{1-x}A'_{x}B_{1-y}B'_{y}O_{3}$ , where A' and B' represent the A- and B-site dopants at a doping level of x and y, respectively. For the A-site substitution, A' is typically a rare-earth or an alkaline-earth metal. Hyodo et al. investigated the effect of rare-earth elements on the ORR activity of  $LnMnO_3$  (Ln = lanthanides) in alkaline solutions, and found an activity order of La > Pr > Nd > Sm > Gd > Y > Dy > Yb, consistent with the decreasing order of the Ln<sup>3+</sup> ionic radius [75]. Partial replacement of lanthanides by alkaline-earth metals can further change the catalytic performance. For example, the ORR activity of  $Pr_{0.8}A'_{0.2}MnO_3$  (A' = Ca, Sr, Ba) perovskites was reported to increase in the order of  $PrMnO_3 < Pr_{0.8}Ba_{0.2}MnO_3 < Pr_{0.8}Sr_{0.2}MnO_3 < Pr_{0.8}Ca_{0.2}MnO_3$  [76]. The effects of Asite doping on the ORR activity were also observed in other perovskite systems, such as La<sub>1-x</sub>Ca<sub>x</sub>MnO<sub>3</sub> [77], La<sub>1-x</sub>Sr<sub>x</sub>MnO<sub>3</sub> [78,79], and La<sub>1-x</sub>Ca<sub>x</sub>CoO<sub>3</sub> [80]. Similar studies have also been conducted in the OER (e.g., La1-xSrxCoO<sub>3</sub> [29,73,81], and La1-xSrxFeO<sub>3</sub> [82]) and HER (e.g.,  $Pr_x(Ba_{0.5}Sr_{0.5})_{1-x}Co_{0.8}Fe_{0.2}O_{3-\delta}$  [42]).

Compared to the A-site doping, the B-site doping can more directly affect the catalytic activity of perovskite oxides because the B-site transition metal is considered the reactive site in conventional ORR/OER mechanisms. Sunarso et al. studied the influence of transition metals on the ORR activity of LaBO<sub>3</sub> (B = Cr, Mn, Fe, Co, and Ni) in alkaline media, and found that the diffusion-limited current density of the ORR decreases in the order of LaCoO<sub>3</sub> > LaMnO<sub>3</sub> > LaNiO<sub>3</sub> > LaFeO<sub>3</sub> > LaCrO<sub>3</sub> [83], analogous to that reported by Shao-Horn et al. [26]. For the B-site substitution, B' can be a redox-active transition metal or a redox-inert element or both. For instance, partial substitution of Ni in LaNiO<sub>3</sub> with Fe [58] or Mg [57] could give rise to LaNi<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3</sub> or LaNi<sub>0.85</sub>Mg<sub>0.15</sub>O<sub>3</sub> with improved ORR activity. In particular, incorporating catalytically inactive components into the B-site can help tune the electronic structure of the original redox-active metal and thus contribute to enhanced catalytic performance. Notably, this aspect has been extensively studied on a multitude of perovskite systems involving a range of elements as dopants, such as Sc [84,85], Ti [86], Nb [50,84,87], Mo [87], W [88], Sn [89], Bi [85], Si [90], P [91-93], S [91].

Moreover, the accommodation of multiple dopants in the B-site can also alter the catalytic behavior [84,85,89]. For example, Xu et al. evaluated the OER activity of a series of iron and tin co-doped BaCo<sub>0.9-x</sub>Fe<sub>x</sub>Sn<sub>0.1</sub>O<sub>3- $\delta}$  (x = 0.2, 0.3, 0.4, denoted as BCFSn-721, BCFSn-631, and BCFSn-541, respectively) [89]. Having negligible variance in physicochemical properties like surface area, morphology, crystal structure, oxygen nonstoichiometry, and surface Co oxidation state, the BaCo<sub>0.9-x</sub>Fe<sub>x</sub>Sn<sub>0.1</sub>O<sub>3- $\delta}$  series offer a good activity comparison in terms of the concentration of different dopants. As shown in **Figure 2.5**, the OER activity increases with a higher amount of Co occupying the B-site. This indicates the intrinsically better OER performance of transition metal Co ions relative to Fe ions in a perovskite structure, similar to the finding observed on SrB<sub>0.9</sub>Ti<sub>0.1</sub>O<sub>3- $\delta}$  (B = Co, Fe) perovskites [86]. A much improved OER activity was also found on the most active BaCo<sub>0.7</sub>Fe<sub>0.2</sub>Sn<sub>0.1</sub>O<sub>3- $\delta}$  compared to the non-doped and the Fe or Sn single-doped counterparts, suggesting that a synergistic effect of the two dopants may be at work.</sub></sub></sub></sub>



**Figure 2.5** The OER activity of a series of  $BaCo_{0.9-x}Fe_xSn_{0.1}O_{3-\delta}$  perovskites (x = 0.2, 0.3, 0.4, denoted as BCFSn-721, BCFSn-631, and BCFSn-541, respectively) evaluated by cyclic voltammograms in 0.1 M KOH solution. The negligible OER activity of a carbon background is shown for reference. (Reprinted with permission from Ref. [89]. Copyright 2015 John Wiley and Sons)

The effect of composition can be more complicated where both the A and B sites are doped with foreign elements [94-96]. In this scenario, a systematic investigation, more often case-by-case, is needed to study the relationship between composition and activity before locating an optimal composition. Apart from cation doping, the composition of perovskites can be further altered by introducing A-site cation deficiency [97-99]. For example, Zhu et al. synthesized several A-site-deficient  $La_{1-x}FeO_{3-\delta}$  perovskites and obtained the optimal OER activity at a deficiency of x =0.05 [97].

#### 2.4.2.2 Oxygen vacancy

A stricter way of describing the formula of perovskite oxides would actually be ABO<sub>3 $\pm\delta$ </sub> because many perovskite oxides have an oxygen stoichiometry that deviates from the nominal value of 3. While the effect of oxygen excess (i.e., oxygen stoichiometry of  $3+\delta$ ) in perovskites is merely studied in electrocatalysis, that of oxygen vacancy (i.e., oxygen stoichiometry of  $3-\delta$ ) has attracted plenty of research interest. Mefford et al. found that the OER activity of the  $La_{1-x}Sr_xCoO_{3-\delta}$  series correlated strongly with the oxygen vacancy concentration ( $\delta$ ), with the highest activity obtained on SrCoO<sub>2.7</sub> with the largest vacancy content (Figure 2.6a) [29]. Based on this, they proposed a lattice oxygen-mediated (LOM) OER mechanism that takes into consideration the involvement of lattice oxygen species and the role of surface oxygen vacancies (Figure 2.6b). The validity of this LOM mechanism was further supported by DFT modelling. Later, the participation of lattice oxygen in the OER was experimentally verified by in situ <sup>18</sup>O isotope labelling mass spectrometry [30]. Different from the classically studied mechanism which only concerns surface metal sites, the LOM mechanism considers the importance of transition metal-oxygen covalency in triggering the reaction [29,30]. These studies thus point to the critical role of oxygen vacancy, which cannot be ignored in the fundamental understanding of reaction mechanisms as well as the rational design of advanced perovskite electrocatalysts.



**Figure 2.6** (a) Correlation of the OER activity of  $La_{1-x}Sr_xCoO_{3-\delta}$  with the oxygen vacancy concentration ( $\delta$ ), where  $La_{1-x}Sr_xCoO_{3-\delta}$  is denoted as LSCO(1-x)x, that is, LSCO82 for La<sub>0.8</sub>Sr<sub>0.2</sub>CoO<sub>3- $\delta$ </sub>. (b) Lattice oxygen-mediated (LOM) OER mechanism for perovskites in alkaline solutions. (Reprinted with permission from Ref. [29]. Copyright 2016 Springer Nature)

Normally, oxygen vacancy is inherent in most of the perovskite oxides, and often varies accordingly with any compositional change in order to maintain charge neutrality within the perovskite structure. For perovskites with a specific composition, there are generally two approaches to creating oxygen vacancy. One is to control the synthetic procedures, in which thermal reduction during the formation of perovskite crystallinity may be crucial to the generation of oxygen vacancy. For example, flame spray method was reported to synthesize BSCF perovskite with an oxygen deficiency up to  $\sim 0.75$  [100], much higher than that synthesized from other methods such as sol-gel process ( $\delta \approx 0.44$ ) [42] and solution combustion method ( $\delta \approx 0.4$ ) [26]. The highly oxygen-deficient BSCF was found to show a 55-fold enhancement in the OER current density relative to the sol-gel produced BSCF. The other route to increase the amount of oxygen vacancy is to conduct post-treatment on an existing perovskite, typically via reduction in H<sub>2</sub> or vacuum. For instance, oxygen-stoichiometric CaMnO<sub>3</sub> was converted into oxygen-deficient CaMnO<sub>2.5</sub> ( $\delta = 0.5$ ) after a low-temperature reductive annealing process in 5% H<sub>2</sub>/Ar while the orthorhombic crystal structure was preserved [51]. With the introduction of oxygen defects, CaMnO<sub>2.5</sub> displayed a significantly improved OER activity compared to CaMnO<sub>3</sub>. Under a much harsher reductive treatment in vacuum, Chen et al. prepared BaTiO<sub>3-δ</sub> perovskite with
abundant oxygen vacancies, showing enhanced performance in both the OER and ORR [101].

It should be noted, however, that increasing the number of oxygen defect sites does not necessarily lead to increased catalytic activity. This is because oxygen vacancy is not the sole factor that influences electrocatalysis. When oxygen vacancy changes, the metal electronic states (e.g., oxidation state and coordination) and metal–oxygen covalency change concomitantly. Wang et al. studied the HER activity of a series of H<sub>2</sub>-redution treated NdBaMn<sub>2</sub>O<sub>6– $\delta$ </sub> double perovskites with various oxygen vacancy contents ( $\delta = 0.35$ , 0.54, and 0.80) [102]. The best activity was obtained for the sample with a moderate oxygen vacancy of  $\delta = 0.54$ , which they attributed to a combination of several factors including a distorted structure, a near-unity e<sub>g</sub> occupancy, and an optimized O p-band center. This suggests that optimized catalytic activity may be achieved on perovskites with a moderate number of oxygen vacancy. A similar trending was also found in the CaMnO<sub>3– $\delta$ </sub> perovskites ( $0 < \delta \le 0.5$ ) in the electrocatalysis of ORR/OER [103]. Therefore, caution needs to be exercised in the development of oxygen-deficient perovskite catalysts.

# 2.4.2.3 Crystal structure

The crystal structure of perovskite oxides, both bulk and surface, is closely related to the electrocatalytic activity. For a perovskite with a specific nominal composition, its bulk crystal structure can vary with the synthesis conditions. For example, heattreating a La<sub>0.7</sub>Sr<sub>0.3</sub>MnO<sub>3</sub> precursor at 650, 750, and 850 °C led to the formation of tetragonal, cubic, and orthorhombic phase structure, respectively [104]. Electrochemical measurements indicated that the tetragonal La<sub>0.7</sub>Sr<sub>0.3</sub>MnO<sub>3</sub> exhibited the highest ORR activity. Another way to alter the bulk crystal structure is via posttreatment. For instance, crystalline LaNiO<sub>3- $\delta$ </sub> perovskite, which has a rhombohedral phase at room temperature, transformed into a cubic-phase LaNiO<sub>3- $\delta$ </sub> after being quenched from 800 °C to room temperature [105]. Such a phase transition contributed to a significant improvement in the ORR/OER catalytic activity. Apart from the quenching process, reductive annealing in H<sub>2</sub> can also change the perovskite bulk structure. In this respect, a cubic-phase Pr<sub>0.5</sub>Ba<sub>0.5</sub>MnO<sub>3- $\delta$ </sub> perovskite was reported to convert into a tetragonal-phase PrBaMn<sub>2</sub>O<sub>5+ $\delta$ </sub> layered perovskite after H<sub>2</sub> treatment, showing greatly enhanced activity toward both the ORR and OER [106]. While conventional research has mostly focused on crystalline perovskites for electrocatalysis, it has recently been shown that amorphous perovskites also exhibit considerable catalytic performance. For example, Trudel and co-workers developed a photochemical thin-film deposition technique to synthesize a series of amorphous perovskite oxides such as LaCoO<sub>3-δ</sub> [107], La<sub>0.7</sub>Ca<sub>0.3</sub>CoO<sub>3-δ</sub> [108], and BSCF [109], all showing favorable OER activity. In addition, magnetron sputtering deposition was used by Chen et al. to obtain amorphous BSCF nanofilms with exceptional OER performance [110]. The good catalytic activity may originate from the coordinately unsaturated surface metal sites of amorphous perovskites [111]. More research efforts are required to gain a better understanding of the origin of the catalytic activity of perovskite materials with an amorphous structure.

The surface crystal structure of perovskite materials can also influence the electrocatalytic performance. BSCF perovskite, which was crystallized from a conventional sol–gel process by calcination at 950 °C for 5 h, was found to have a surface amorphous oxide layer with a thickness of around 20 nm [112]. After heat-treatment in argon (Ar) atmosphere, this amorphous layer gigantically grew to a thickness of 180–200 nm, deactivating the catalytic performance of BSCF toward the ORR. However, a same Ar-treatment to pristine Ba<sub>0.5</sub>Sr<sub>0.5</sub>Co<sub>0.2</sub>Fe<sub>0.8</sub>O<sub>3- $\delta$ </sub> with also a  $\approx$ 20 nm thick amorphous layer did not lead to further amorphization while offering an increased amount of oxygen vacancy, which resulted in a notable improvement in ORR activity. This suggests a composition-dependent behavior upon treatment in Ar between the changes in perovskite surface structure and catalytic activity.

The surface crystal structure of perovskites with an identical composition can differ with the calcination conditions. For example, the BSCF perovskite calcined at 1050 °C for 5 h exhibited a nanoscale-thick spinel-phase layer between the bulk particle and the amorphous layer on the outermost surface [113]. This spinel layer could be removed by an oxygenation process via heat-treatment in oxygen atmosphere (**Figure 2.7**), giving rise to enhanced ORR/OER performance of the BSCF catalyst.



**Figure 2.7** A schematic representation of the effect of heat treatment in oxygen on the BSCF perovskite. (Reprinted with permission from Ref. [113]. Copyright 2014 John Wiley and Sons)

These studies highlight the tunability of perovskite structures in both the bulk and surface, which is achieved using experimental procedures that are performed ex situ. It should also be noted that perovskite structures can undergo in situ changes under realistic electrochemical conditions. For example, the structure transformation from BaNiO<sub>3</sub> to BaNi<sub>0.83</sub>O<sub>2.5</sub> over the OER testing in alkaline media led to an improved catalytic performance [114]. To some extent, this is more of a stability issue, and thus will be discussed later in more detail in the section of stability concerns.

### 2.4.2.4 Nanostructure

Previous understanding of the electrocatalytic role of perovskites is mainly gained from bulk-sized materials, which are prepared from conventional sol–gel process [115], solid-state reaction [116], and high-pressure synthesis [117]. These bulk perovskites normally have a large particle size, a small surface area, and a featureless morphology, which can only offer limited catalytic capability. This is because a substantial proportion of inactive atoms in the bulk of perovskites are often not catalytically active toward reactions occurring at the surface. To address this issue, nanostructuring has been proposed as a technically viable approach [14]. Once a perovskite material is downsized to the nanoscale, an increase in surface area and also the number of reactive

sites can be expected. Although a linearly increased number of reactive sites may not be necessarily achievable considering the accessibility issue of reactive sites, the increase in surface area does provide a greater number of reactive sites, thus contributing to an improved catalytic activity, more often on a catalyst mass basis. This has already been proved by the increased OER activity observed on the ballmilled BSCF catalyst [26], which has a particle size much reduced compared to the bulk BSCF.

Perovskite nanostructures can be attained by tailoring the synthetic parameters of conventional preparation methods. For example, Cho and co-workers developed an intriguing pattern of perovskite phase existence and particle growth by altering the calcination temperatures and lanthanum-dopant concentrations during the sol-gel synthesis of  $La_x(Ba_{0.5}Sr_{0.5})_{1-x}Co_{0.8}Fe_{0.2}O_{3-\delta}$  perovskites [118]. At a reduced temperature calcination of 700 °C and a La doping content of x = 0.7, La0.7(Ba0.5Sr0.5)0.3Co0.8Fe0.2O3- $\delta$  perovskite with a particle size as small as 50 nm was obtained, showing a substantial improvement in the alkaline ORR/OER activity. This approach, however, requires the perovskite A-site to contain a lanthanide component, and thus may not be broadly extended to other perovskite oxides. Alternatively, a range of synthetic methods have been used to synthesize nanostructured perovskites, including precipitation method, hydrothermal synthesis, templating approach, and electrospinning [14]. In addition, several deposition-based techniques, such as physical vapor deposition (PVD), chemical vapor deposition (CVD), and electrodeposition, have also been developed to fabricate nanosized perovskite materials. The as-obtained perovskites possess plenty of morphological features, including nanowire [119], nanofiber [120], nanorod [121], nanotube [122], nanosphere [123], nanocube [124], among others. These morphologies can lead to the different catalytic behaviors of nanostructured perovskites. For instance, compared to LaCoO3 dense particles synthesized by a sol-gel route, LaCoO<sub>3</sub> porous particles and hollow nanospheres synthesized by a hydrothermal method showed an increased OER activity in an alkaline electrolyte (Figure 2.8).



**Figure 2.8** Scanning electron micrographs of LaCoO<sub>3</sub> (a) dense particles, (b) porous particles, and (c) hollow nanospheres. (d) The OER activity of LaCoO<sub>3</sub> dense particles, porous particles, and hollow nanospheres evaluated by cyclic voltammograms in 0.1 M KOH solution. (Reprinted with permission from Ref. [123]. Copyright 2017 American Chemical Society)

Note that the improved catalytic performance of nanostructured perovskites may not be just a surface area effect. While LaCoO<sub>3</sub> porous particles and hollow nanospheres had a higher surface area than the dense particles, their increased OER activity was also attributed to the presence of amorphous surface structures formed during the hydrothermal synthesis [123]. Moreover, nanostructuring can further bring about a nanosize effect, that is, reducing the nanostructure size can tune the electronic state of perovskites. For example, Zhou et al. obtained LaCoO<sub>3</sub> nanoparticles with sizes of 60, 80, and 200 nm, and bulk LaCoO<sub>3</sub> particles by annealing a sol–gel precursor at 600, 700, 800, and 1000 °C, respectively [68]. Surprisingly, the best OER activity was observed on the 80 nm LaCoO<sub>3</sub>, which was ascribed to its optimal  $e_g$  filling of Co ions (~1.2) based on Shao-Horn's activity descriptor [26]. The nanosize effect can still be at play when the perovskite size is further reduced. For instance, Zhao et al. found that the OER activity of an electrospun double perovskite nanofiber with a diameter as low as 20 nm is intrinsically higher than those with larger diameters, which was presumably due to the favorable surface electronic structure and the possible presence of heterostructures [125]. It is therefore important to understand the electrocatalytic processes on nanostructured perovskites, both experimentally and theoretically. Such understanding, combined with that gained from bulk perovskite materials, can better guide the development of improved perovskite electrocatalysts.

#### 2.4.2.5 Composite

Forming composites with other materials, including carbons, metals, and metal oxides, among others, can also extrinsically increase the catalytic activity of perovskite materials. In particular, perovskite/carbon composites have attracted the most research interest [126]. The inclusion of carbon into a perovskite oxide was first used to remove any possible electrical conductivity limitations within some intrinsically insulating or semiconducting perovskites [127]. However, recent investigations have suggested that carbon could serve more than just the role of a conductive support [128-134]. For example, in the electrocatalytic ORR, carbon in perovskite/carbon composites was found to participate in the ORR mechanistic pathway by catalyzing the reduction of  $O_2$  to  $HO_2^-$  [128-133]. In addition, carbon could act as a reducing agent to modify the electronic structure of perovskites. For example, acetylene black (a type of conductive carbon), when composited with BSCF, was found to reduce the cobalt cations to a lower oxidation state, which contributed to a greatly improved ORR/OER activity [134]. These observations highlight the important roles of carbon in perovskite/carbon composites, which can be utilized to design improved perovskite-based hybrid catalysts.

Perovskite/carbon composites can be simply obtained using physical mixing, showing enhanced bifunctional activity toward the ORR and OER [135-138]. A more intimate combination between perovskites and carbons is expected to further improve the ORR/OER bifunctionality. This can be realized by means of advanced chemical synthesis, such as the CVD process [139-143], hydrothermal method [144,145], and electrospinning [146]. However, due to the inherent incompatibility between the reductive carbon materials and the oxidative perovskite oxides, it remains challenging to obtain perovskite/carbon composites with a pure-phase perovskite component. For instance, the perovskite structure may not be preserved during the high-temperature CVD process [143]. To address this, modification to the current synthetic conditions are required. In addition, novel fabrication techniques should be developed to synthesize intact perovskite/carbon composites to achieve improved electrocatalysts.

Understanding the origin of enhanced catalytic activity on perovskite/carbon composites is important to the rational design of efficient perovskite catalysts. While conventional research has pointed to a "synergistic effect" between the perovskite and carbon, that is, two is better than one, it does not clarify the true reason behind the improved activity. Recently, Zhu et al. proposed three possible origins to explain the increased activity observed on perovskite/carbon composites (Figure 2.9) [126]. First, the ligand effect at the interface can modify the electronic structure and thus lead to increased activity as mentioned earlier [134]. Second, the formation of interfacial heterostructures, in the form of covalent bonds or a new phase, can contribute to enhanced catalytic activity. This can be understood from the fact that strongly coupled perovskite/carbon composites made from chemical synthesis outperformed not only each individual component but also their physical mixtures. Third, the spillover effect can be at work for the improved bifunctionality of perovskite/carbon composites. In the composite, perovskites are considered to be more active toward the OER whereas carbons are more active toward the ORR. During the ORR process, the OH<sup>-</sup> generated on the carbon surface spills over to the perovskite surface, which promotes the ORR by releasing more reactive sites on the carbon surface, leading to increased ORR activity. In a similar way, during the OER process, O<sub>2</sub> produced on the perovskite surface spills over to the carbon surface, which facilitates the OER by releasing more reactive sites on the perovskite surface, giving rise to enhanced OER activity.



**Figure 2.9** A schematic illustration of three possible origins that may clarify the improved activity on perovskite/carbon composites. (a) Ligand effect. (b) Formation of interfacial heterostructures. (c) Spillover effect. (Reprinted with permission from Ref. [126]. Copyright 2017 John Wiley and Sons)

Despite the contribution to improved electrocatalysis, perovskite/carbon composites might suffer from carbon corrosion, a common issue for carbon-based materials especially in the case of the OER. This issue, although less severe in alkaline media as compared to acidic media [147], can still lead to the reduction of reactive sites and even degradation of catalysts under elevated potentials during the OER testing. One way to mitigate the carbon corrosion is by using graphitized carbon or nitrogen-doped carbon with improved corrosion resistance [148,149].

Very recently, perovskites have also been hybridized with other conducting substrates, for example, Ni foam, via advanced synthetic methods such as hydrothermal method [150] and electrodeposition [151]. Similarly, due to the reductive nature of Ni foam, the difficulty in fabricating perovskite/Ni foam composites lies in the acquisition of pure oxidative perovskites in a high-temperature annealing process. Annealing under nonoxidative atmosphere can stabilize the Ni foam while also facilitating the formation of a perovskite phase if the precursor of perovskites is finely tuned. For example, Li et al. used electrodeposition to deposit a perovskite hydroxide precursor on Ni foam,

which could convert into crystallized perovskite oxide upon a moderate annealing treatment in Ar [151]. Taking advantage from both the catalytically active perovskites and the 3D porous, highly conductive Ni foam, perovskite/Ni foam composites possess great potential in practical applications.

In addition to forming composites with conductive materials, perovskites can also be coupled with metal nanoparticles. Such hybrid materials are often synthesized by exsolution, a chemical process that is almost exclusive to perovskite oxides. Under heat treatment in a reductive atmosphere (e.g., H<sub>2</sub>), an active metal initially incorporated in the perovskite lattice can go through a reduction process and then exsolve in the form of metal nanoparticles on the surface of the perovskite [152]. These metal nanoparticles can act as additional catalytic sites while also changing the original perovskite electronic structure, thus leading to a different behavior in electrocatalysis. For example, Ni nanoparticle-decorated La0.4Sr0.4Ti0.9O3-& composite, which was constructed from the La<sub>0.4</sub>Sr<sub>0.4</sub>Ti<sub>0.9</sub>Ni<sub>0.1</sub>O<sub>3-δ</sub> parent perovskite using a facile exsolution process, can synergistically catalyze the alkaline HER at a significantly improved efficiency [153]. In the hybrid catalyst, La<sub>0.4</sub>Sr<sub>0.4</sub>Ti<sub>0.9</sub>O<sub>3- $\delta$ </sub> facilitates water dissociation whereas Ni nanoparticles favors hydrogen adsorption for the recombination into H<sub>2</sub>. In a similar fashion, a Ag nanoparticle-modified (PrBa)0.95Mn2O5+8 double perovskite obtained from exsolution exhibited favorable ORR activity in alkaline electrolytes, which is due likely to the strong coupling between the perovskite and Ag nanoparticles [154]. Apart from metal nanoparticles, other nanomaterials, such as metal alloys [155-158], metal/metal oxide hybrids [159,160], can also exsolve from the perovskite lattice by carefully tuning the perovskite composition and H2-reduction condition. These advantages of the exsolution process can bring about ample opportunities for making perovskite derived composites with increased electrocatalytic performance.

Other catalytically active materials, such as hydroxides [161] and metal oxides [162-165], can also composite with perovskite oxides using either an infiltration process or chemical synthesis. These composite materials showed enhanced catalytic performance with respect to the sole perovskite component. To obtain optimized activity, both the perovskite oxide and the additive functional material should be cautiously selected. For example, BSCF, which is considered the benchmark perovskite OER catalyst, was composited with the benchmark ORR catalyst, commercial Pt/C, and obtained a substantially improved catalytic activity in both the ORR and OER [166]. However, these two components were physically mixed, which may not be able to unleash the full potential of their high activity. Future efforts should be devoted to the design of strongly coupled perovskite-based materials, either through experimentally developed synthetic methods or through theoretically established modelling approaches.

# 2.4.3 Stability concerns

Compared to the significant advances in the establishment of design principles for improvement in catalytic activity, much less attention is placed on the stability of an electrocatalyst, which is actually of more relevance to realistic device-based applications. This is especially the case when it comes to perovskite OER catalysts. Even under ambient conditions, most of perovskite oxides will become amorphous during the OER, which is often accompanied by the leaching of A- or B-site cations into the electrolyte. For instance, amorphization was observed in the bulk and surface of highly active perovskite catalysts (e.g., BSCF), leading to the structural evolution from corner-sharing octahedra to edge-sharing octahedra [167,168]. This phenomenon is more pronounced near the catalyst surface region than in the bulk, as evidenced from ex situ X-ray absorption spectroscopic measurements (XAS) [168].

Understanding the changes occurring at the catalyst surface is therefore critical for the design of enduring perovskite electrocatalysts. This can be partially achieved through an improved understanding of the interaction between perovskite oxides and water electrolytes under a modelling system similar to the OER. For example, using in situ environmental transmission electron microscopy, Shao-Horn et al. observed structural oscillations on BSCF upon its interaction with water vapor under electron irradiation [169]. A more direct and viable way to access the changes on perovskite oxides is to use operando XAS measurements during realistic OER conditions, which was first reported by Fabbri and co-workers. **Figure 2.10** shows an anodic polarization of a flame spray-synthesized BSCF nanocatalyst (BSCF-FS), where shift of the Co K-edge position, which was extracted from operando X-ray absorption near-edge structure (XANES) spectra, is recorded in line with the OER current [100]. It is noticeable that upon the onset of the oxygen evolution at 1.425 V versus the reversible hydrogen electrode (RHE), the Co K-edge shifts toward higher energy, corresponding to an increase in the Co oxidation state. Such change was not observed in a reverse cathodic

polarization scan, indicating that the oxidation of Co is mostly an irreversible process. Further operando extended X-ray absorption fine-structure (EXAFS) tests revealed the formation of a self-assembled surface layer consisting of OER-active metal (oxy)hydroxides, which is considered to be the origin of the significantly enhanced OER performance (in both activity and stability) based on an OER mechanism coupled with lattice oxygen participation.



**Figure 2.10** OER current and shift of the Co K-edge position (taken from Operando XANES spectra) collected in situ during an anodic polarization of the BSCF-FS perovskite catalyst in 0.1 M KOH alkaline solution. (Reprinted with permission from Ref. [100]. Copyright 2017 Springer Nature)

These operando observations point to an important conclusion with respect to both catalyst activity and stability. Active perovskite OER catalysts can experience drastic changes in local chemical/electronic structures. This is substantially different from the previously mentioned activity descriptors which rely on ex situ physical properties (e.g., eg-filling number) to guide catalyst design. On the other hand, a perovskite oxide initially considered to be 'instable' could actually evolve into a 'stable' catalyst through operando changes, in which case the original perovskite can be seen as a 'precursor' (or 'pre-catalyst') of a real active catalyst [100]. A similar phenomenon was also found in acidic electrolytes on a SrIrO<sub>3</sub> perovskite, which transformed in situ during electrochemical testing into a highly active and stable IrO<sub>x</sub>/SrIrO<sub>3</sub> catalyst [170].

It is noteworthy that the extent of changes on perovskite surfaces varies with different materials compositions and chemistries, which may relate to the different concentrations of oxygen vacancy in perovskites [100]. Shao-Horn et al. has earlier correlated the computed O p-band center with the perovskite stability under alkaline OER conditions, and arrived at the conclusion that an optimum position of the O pband center leads to high catalyst stability [46]. It is also important to note that not all perovskites are capable of evolving into active and durable catalysts. For example, several nickel-based and iron-based perovskite materials were found to lose activity upon prolonged OER tests under alkaline media [82,171]. Based on these considerations, a case-by-case investigation into the stability (and activity) of a specific perovskite material can be necessary in the evaluation of its electrocatalytic performance.

Sometimes the stability issue is of more interest to the industry than to the academia. The research community currently tends to report 'stable' perovskite catalysts, more often simply from the viewpoint of electrochemical stability, without looking further into the catalyst structure either ex situ or in situ. Also, the catalyst degradation phenomena under OER testing and their origins are less explored [172-174]. In industrial settings, more rigid requirements are placed on the catalyst stability. For instance, the alkaline water electrolysis would require a catalyst to stably operate at temperatures of around 80 °C, under which condition perovskite OER catalysts may undergo changes even harsher than those at room temperature. To bridge this gap between the fundamental and applied research, more efforts should be devoted to understanding the changes in perovskites (e.g., degradation mechanisms) during the OER, which will also aid the establishment of an improved catalyst design principle that combines both catalytic activity and stability. The same holds true for perovskites in the ORR and HER electrocatalysis, although attention to these fields is still lacking.

# 2.5 Perovskite materials for electrocatalysis-related applications

The ORR/OER reactions are technologically relevant to metal–air batteries, whereas the OER/HER reactions hold key to the overall efficiency of a water electrolyzer. Over the years, a plethora of perovskite materials have been used in these devices [14,175]. While conventional mechanistic understanding of electrocatalysis is gained mostly from bulk perovskite materials, they may not favor practical applications because of

their rather low catalytic activity, which is due to their huge particle sizes, low surface areas, and few morphological features. Comparatively speaking, nanosized and nanostructured perovskites are more suited for practical use because they offer increased reactive sites, improved accessibility of reactive sites, and better diffusion of gas reactants/products. In addition, the cost of an electrocatalyst can be more of concern for real-world devices. Also of importance is the catalyst stability, and very often a compromise has to be made between stability and activity. This section discusses the use of perovskite nanocatalysts made of Earth-abundant elements in metal–air batteries and water electrolyzers.

## 2.5.1 Metal-air batteries

Metal–air batteries are efficient energy conversion devices that can offer a theoretical specific energy even higher than that of the commercially available Li-ion batteries [176]. In general, a metal–air battery is composed of a metal anode, an electrolyte, and an air cathode. Among various anode candidates, Li and Zn are two of the most widely studied anode materials. The corresponding metal–air batteries are typically referred to as Li–air batteries and Zn–air batteries, respectively. Despite a major difference in electrolyte (i.e., normally nonaqueous electrolyte for Li–air batteries and aqueous electrolyte for Zn–air batteries), these two types of metal–air batteries suffer from one common scientific issue, that is, the slow kinetics of the ORR/OER reactions that determine the overall energy efficiency. At the cathode of a metal–air battery, oxygen is reduced upon discharge (ORR) and is evolved upon charge (OER). Therefore, an efficient, rechargeable metal–air battery would necessitate a bifunctional electrocatalyst that promotes both the ORR and OER.

Porosity is an important factor for achieving the practical use of perovskite catalysts in metal–air batteries. Zhang and co-workers reported the application of a threedimensionally ordered macroporous LaFeO<sub>3</sub> perovskite (3DOM-LFO) as a cathode catalyst in a nonaqueous Li–air battery (**Figure 2.11a**) [177]. The 3DOM-LFO catalyst had an interconnected, well-ordered, honeycomb-like pore structure (**Figure 2.11b**), which was inherited from the polystyrene sphere template during a templating synthesis. Such a porous nanostructure could facilitate the diffusion of O<sub>2</sub>/electrolyte during discharge/charge processes while offering significantly enhanced surface area for catalytic ORR/OER reactions, both contributing to improved performance and cycle stability of the rechargeable Li–air battery compared to the nanoparticulate LaFeO<sub>3</sub> catalyst. Porous one-dimensional (1D) nanostructures possess high surfaceto-volume ratios and abundant porosity, which can favor the availability of catalytic sites as well as the diffusion of O<sub>2</sub> gas when used as cathode catalysts for Li–air batteries. For example, a porous nanotubular La<sub>0.75</sub>Sr<sub>0.25</sub>MnO<sub>3</sub> perovskite fabricated by electrospinning was found to show a significant increase in both ORR/OER electrocatalysis and battery performance in a nonaqueous electrolyte [178]. Another useful way to obtain a porous cathode catalyst is via the growth of perovskites on 3D porous substrates (e.g., Ni foam). Pham et al. used hydrothermal synthesis to grow perovskite LaNi<sub>0.9</sub>Cu<sub>0.1</sub>O<sub>3</sub> nanosheet arrays on the surface of a 3D microporous Ni foam [150]. This composite was directly applied as a binder-free cathode, and exhibited notable ORR/OER activity and cycling performance in a nonaqueous Li–air battery.



**Figure 2.11** (a) A schematic representation of the synthesis of a 3DOM-LFO perovskite and its application as a cathode catalyst in a rechargeable Li–air battery. (b) Scanning electron micrographs of the 3DOM-LFO catalyst, showing an interconnected, well-ordered, honeycomb-like pore structure. (Reprinted with permission from Ref. [177]. Copyright 2013 Royal Society of Chemistry)

It should be noted that the oxygen electrocatalysis in nonaqueous Li–air batteries, which follows the reaction of  $O_2 + 2Li^+ + 2e^- \leftrightarrow Li_2O_2$ , is quite different from that in aqueous solutions. Therefore, the design principles for advanced perovskite catalysts working in alkaline water may not be able to extend to the system of nonaqueous Li– air batteries. Despite the success of several perovskite nanocatalysts, little understanding is gained about the reaction mechanisms in nonaqueous electrolytes. While some attempts were made to evaluate the ORR/OER in nonaqueous solutions [119,124,150,177,178], more systematic investigations, rather than trial-and-error approaches, are needed in order to design better perovskite catalysts for nonaqueous Li–air batteries. By contrast, Zn–air batteries commonly adopt an aqueous alkaline electrolyte considering the stability of zinc anode and the manufacturing cost of the battery configuration. Although a higher concentration of potassium hydroxide solution (e.g., 6 M KOH) is used in Zn–air batteries, the oxygen electrocatalysis at the cathode follows the same reaction of  $O_2 + 2H_2O + 4e^- \leftrightarrow 4OH^-$  as that in fundamental research. Therefore, the conventionally studied ORR/OER on perovskite materials in alkaline media is considered more relevant to the application in Zn–air batteries.

Recent years have witnessed the development of a myriad of perovskite nanomaterials for use in Zn–air batteries. Among the many candidates, perovskite/carbon composites have received more research attention, due primarily to their significantly increased electrical conductivity compared to the sole perovskites. For instance, a LaNiO<sub>3</sub> nanorod/reduced graphene oxide hybrid synthesized using a hydrothermal method showed much enhanced conductivity relative to the LaNiO<sub>3</sub> nanorod, thereby leading to higher ORR/OER activity in alkaline solutions and also better cycle performance in rechargeable Zn–air batteries [144]. Prabu et al. reported perovskite LaTi0.65Fe0.35O<sub>3</sub>– $\delta$  nanoparticles embedded both at the surface of and within nitrogen-doped carbon nanorods, which were prepared via electrospinning followed by calcination under Ar atmosphere [146]. Compared to LaTi0.65Fe0.35O<sub>3</sub>– $\delta$  nanotubes without carbon, which were obtained after calcination under air, the LaTi0.65Fe0.35O<sub>3</sub>– $\delta$ /carbon nanocomposite afforded increased catalytic sites, improved electrical conductivity, and highly promoted kinetics toward both the ORR and OER, resulting in an exceptionally higher Zn–air battery performance.

Although the above-mentioned perovskite/carbon composites can give rise to an improvement in Zn–air battery performance, they are produced at a small scale using bench-based hydrothermal method or electrospinning technique, which may present a hurdle toward their widespread application. Recently, CVD has emerged as a versatile process to achieve scaled-up production of nanohybrids of perovskites and carbons (especially carbon nanotubes (CNTs)), in which transition-metal-containing perovskites are applied as substrates for the catalytic growth of CNTs. Chen and co-workers reported the CVD synthesis of a core–corona structured bifunctional catalyst

(CCBC) and its application as a cathode catalyst in a rechargeable Zn-air battery (Figure 2.12a) [139]. This CCBC composite is comprised of a highly OER-active LaNiO<sub>3</sub> derived core component and a highly ORR-active nitrogen-doped CNTs (NCNTs) corona with a bamboo-like structure (Figure 2.12b). Owing to the strong coupling effect between these two active components, an optimized CCBC-2 catalyst, which was obtained by tuning the CVD synthetic parameters, exhibited outstanding discharge and charge performance comparable to that of the benchmark catalysts in the ORR (i.e., Pt/C) and OER (i.e., LaNiO<sub>3</sub>) (Figure 2.12c). In addition, the CCBC-2 catalyst showed excellent cycling stability for 75 charge-discharge cycles (Figure 2.12d). Using a similar CVD method, the same researchers also obtained an intertwined core-corona structured bifunctional catalyst composed of LaNiO3 nanoparticles encapsulated by NCNTs, showing bifunctionality toward the ORR/OER in rechargeable Zn-air batteries [140]. The CVD process was further extended to the synthesis of perovskite/CNTs composites involving other perovskite oxides, such as LaMn0.9C00.1O3 [141] and La0.5Sr0.5C00.8Fe0.2O3 [142], and good Zn-air battery performance was achieved. However, the physcial origin of the catalysts' high activity and stability is less understood. Moreover, the crystalline structure of the perovskite oxides might be destroyed after the CVD synthesis because of the presence of carbon serving as a reducing agent [143], which calls for more research inputs into the preparation of intact perovskites hybridized with conductive carbons.



**Figure 2.12** (a) A schematic representation of a Zn–air battery and the reactions taking place on the electrodes. (b) Scanning electron micrograph and transmission electron micrograph images of the CCBC catalyst. (c) Discharge and charge polarization curves of the CCBC-2 catalyst in comparison to Pt/C and LaNiO<sub>3</sub>. (d) Charge–discharge cycling performance of the CCBC-2 catalyst. (Reprinted with permission from Ref. [139]. Copyright 2012 American Chemical Society)

While much progress has been made experimentally in fabricating perovskite catalysts for metal–air batteries, theoretically less is known about the relationship between structure, morphology, and performance under operational conditions. This gap has to be bridged if perovskites are to be developed as practical electrocatalysts in real-world batteries. Stability remains to be another concern. Currently, lab-based metal–air batteries that adopt perovskite cathode catalysts can only sustain around 100 cycles of charge–discharge tests, which is far from the requirement of battery technologies. Another long-term goal would be to develop metal–air batteries that can work in ambient air [179], as the present catalyst performance is recorded in laboratory pure oxygen environment. This, however, could take more efforts from scientists, engineers, and the industry.

### 2.5.2 Water electrolyzers

A water electrolyzer is one of the simplest systems for generating high-purity hydrogen. It is also a key component for the 'indirect' solar-to-hydrogen production, converting the electricity generated from renewable solar energy (via solar panels) into chemical energy in hydrogen [180]. In water electrolysis, water is split into hydrogen and oxygen following the equation of  $H_2O \rightarrow H_2 + 1/2O_2$ . This reaction is a thermodynamically uphill process that necessitates an energy input of 286 kJ mol<sup>-1</sup> at room temperature and pressure, corresponding to a theoretical minimum cell voltage of 1.23 V. However, the two half reactions of water splitting, namely the OER at the anode and the HER at the cathode, have sluggish kinetics and can cause large energy losses. For example, commercial water electrolyzers generally operate at a much higher cell voltage of 1.8–2.0 V [181]. The implementation of the water electrolysis technology would thus require highly active and stable OER/HER electrocatalysts to lower the large water-splitting overpotentials and to make the whole process more energy-efficient. While the state-of-the-art Ir-/Ru-based compounds [4] and Pt-group metals [3] offer the highest OER and HER activity, respectively, they suffer from low Earth abundance and high capital cost, hampering their commercial viability. It is thus appealing to develop perovskite materials as alternatives that contain Earth-abundant, low-cost transition metals while still offering high catalytic activity. In addition, industrial electrolyzers work in strong alkaline electrolytes in order to avoid the corrosion from acids and reduce the total cost [182], where perovskites appear to be readily suited given the fundamental understanding of their electrocatalytic roles in alkaline media.

Ever since the first report by Xu. et al. [42], showing that perovskite oxides can catalyze the HER in basic solutions, several works have focused on using perovskites as bifunctional catalysts toward both the HER and OER and the overall water splitting. A typical example was given by Zhu et al. [183], who reported the electrospinning synthesis of perovskite  $SrNb_{0.1}Co_{0.7}Fe_{0.2}O_{3-\delta}$  nanorods (SNCF-NR) and their application as HER/OER catalysts in an alkaline water-splitting cell (**Figure 2.13a**). Owing to the porous 1D nanostructure, SNCF-NR showed significantly enhanced HER and OER activity compared to the bulk-sized SNCF. When loaded on a Ni foam substrate (mass loading: 3 mg cm<sup>-2</sup>) and used as the cathode and anode in a water electrolyzer containing 1 M KOH electrolyte, the SNCF-NR/SNCF-NR couple delivered a voltage of  $\sim 1.68$  V to reach a geometric current density of 10 mA cm<sup>-2</sup>  $(\eta_{10})$  (Figure 2.13b), a figure of merit associated with solar-to-hydrogen production [184]. Although inferior to the state-of-the-art Pt/C cathode and IrO<sub>2</sub> anode couple at this voltage, the SNCF-NR//SNCF-NR couple began to overtake at elevated voltages (> 1.78 V). The alkaline water electrolysis performance can be increased by coupling perovskite materials with nanocarbons. For instance, Hua et al. ultrasonically attached electrospun La<sub>0.5</sub>(Ba<sub>0.4</sub>Sr<sub>0.4</sub>Ca<sub>0.2</sub>)<sub>0.5</sub>Co<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3-δ</sub> perovskite nanorods to reduced graphene oxide nanosheets and obtained a comparable  $\eta_{10}$  value of ~1.66 V in an overall water splitting test [185]. Further improvement in performance can be attained by introducing additional reactive sites other than perovskites. For example, Hua et al. conducted H<sub>2</sub> treatment on A-site-deficient double perovskite nanowires,  $(PrBa_{0.8}Ca_{0.2})_{0.95}(Co_{1.5}Fe_{0.5})_{0.95}Co_{0.05}O_{5+\delta}$ , and obtained Co/CoO<sub>x</sub> nanoparticles exsolved on the surface [159]. Since metal/metal oxide components are expected to show catalytic activity [38,186], their synergistic coupling to perovskite oxides gave rise to a significantly enhanced performance for the HER/OER electrocatalysis and the overall water electrolysis ( $\eta_{10} = 1.62$  V).



**Figure 2.13** (a) A schematic representation of a water electrolyzer using  $SrNb_{0.1}Co_{0.7}Fe_{0.2}O_{3-\delta}$  nanorods (SNCF-NR) as both the cathode and anode. (b) Polarization curves of SNCF-NR//SNCF-NR, SNCF//SNCF, Ni foam//Ni foam, and  $Pt/C(-)//IrO_2(+)$  for overall water splitting in 1 M KOH. (Reprinted with permission from Ref. [183]. Copyright 2016 John Wiley and Sons)

Despite the attempts at developing bifunctional perovskite materials for catalyzing both the OER and HER, the currently available perovskites only show moderate catalytic activity toward the HER [42,102,159,183,185], posing an inevitable overpotential of around 0.2 V for the alkaline water electrolysis. One straightforward way to circumvent this issue is to replace the perovskite-based cathode with the stateof-the-art Pt metal. For example, Chen et al. used magnetron sputtering, which is one popular type of PVD synthesis, to deposit amorphous BSCF nanofilms onto Ni foam substrates (mass loading: 38.7  $\mu$ g cm<sup>-2</sup>) as highly active OER catalysts [110]. When combined with a Pt-Ni foam cathode, which was also obtained by magnetron sputtering deposition at a Pt mass loading of 38.7  $\mu$ g cm<sup>-2</sup>, the BSCF//Pt couple showed significantly reduced voltage for overall water splitting compared to the BSCF//BSCF couple (Figure 2.14a). This is mainly attributed to the intrinsically higher HER activity of Pt relative to BSCF [42]. The cell voltage was further reduced to a  $\eta_{10}$  value of 1.57 V for the BSCF//Pt couple when the mass loading of BSCF on Ni foam was increased to 154.8  $\mu$ g cm<sup>-2</sup>. It is noteworthy that this high performance was achieved on electrodes with an ultralow catalyst mass loading, almost 20 times lower than that of SNCF-NR (3 mg cm<sup>-2</sup>), which may have strong implications for practical use.



**Figure 2.14** (a) Polarization curves of BSCF//BSCF (both at 38.7  $\mu$ g cm<sup>-2</sup>), BSCF//Pt (both at 38.7  $\mu$ g cm<sup>-2</sup>), and BSCF//Pt (BSCF at 154.8  $\mu$ g cm<sup>-2</sup> and Pt at 38.7  $\mu$ g cm<sup>-2</sup>) for overall water splitting in 1 M KOH. (Reprinted with permission from Ref. [110]. Copyright 2017 American Association for the Advancement of Science) (b) Voltage versus time at 50 °C and a steady-state current density of 200 mA cm<sup>-2</sup> obtained for membrane electrode assemblies (MEAs) having BSCF-FS and IrO<sub>2</sub> as the anode electrocatalyst. (Reprinted with permission from Ref. [100]. Copyright 2017 Springer Nature)

The aforementioned perovskite catalysts are evaluated in a simple, lab-based, roomtemperature electrolysis cell, without taking into consideration the configuration of water electrolyzers. A more rational practice was recently reported by Fabbri et al. [100], who employed an alkaline membrane water electrolysis cell to assess the performance of BSCF-FS as an anode OER catalyst in comparison to the state-of-theart IrO<sub>2</sub>. Membrane electrode assemblies (MEAs) containing Pt as the cathode, and BSCF-FS or commercial IrO<sub>2</sub> as the anode were assembled with a 3 mg cm<sup>-2</sup> catalyst loading. Compared to the IrO<sub>2</sub>-based MEA, the BSCF-FS-based MEA presented a lower and more stable cell voltage at steady-state conditions of more relevance to industrial settings, that is, a higher temperature of 50 °C and a larger current density of 200 mA cm<sup>-2</sup> (**Figure 2.14b**). Such measurement offers more solid evidence to the viability of perovskite BSCF-FS nanocatalyst as a low-cost alternative to IrO<sub>2</sub> for efficient water electrolysis.

While much progress has been made in the application of perovskite materials as electrocatalysts for water electrolyzers, there is still room for activity increase, especially in the case of the HER. However, bifunctionality of perovskites for both the HER and OER may appear to be a formidable challenge considering the substantially different reaction processes on perovskite oxide surfaces. Nonetheless, it should be noted that the development of perovskite HER catalysts is still in its infancy. An improved understanding of the reaction mechanism on perovskite surfaces, together with optimized catalyst design strategies, may help facilitate the location of highly active perovskite HER catalysts. At present, a water electrolyzer based on a perovskite OER catalyst coupled with a Pt HER catalyst seems to be a more practical option. Once again, the major concern remains to be the operational stability. The current understanding of catalyst stability is based on short-term electrochemical testing for no more than tens of hours, which is far from satisfactory. In addition, the testing conditions in research laboratories are found to deviate from those in industry. In this sense, application-oriented research should be more extensively carried out for longer lifetimes at conditions more of industrial interest, for example, a temperature of 80 °C and a current density of  $\sim 0.5-2$  A cm<sup>-2</sup> [187]. Provided a combination of inputs into both fundamental and applied research, an operative water electrolyzer based on perovskite electrocatalysts can be expected.

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# **Chapter 3 Methodologies and characterizations\***

\* This chapter summarizes the materials synthesis, characterizations, and electrochemical measurements. Part of this chapter is reprinted (adapted) with permission from (Xiaomin Xu, Yangli Pan, Yijun Zhong, Lei Ge, San Ping Jiang, Zongping Shao, From scheelite BaMoO4 to perovskite BaMoO3: Enhanced electrocatalysis toward the hydrogen evolution in alkaline media, Composites Part B: Engineering, 2020, 198, 108214). Copyright (2020) Elsevier Ltd.

#### 3.1 Materials syntheses

#### 3.1.1 Mo-based perovskite

Scheelite-type oxide BaMoO<sub>4</sub> was synthesized by a co-precipitation method. Barium chloride dihydrate (BaCl<sub>2</sub>·2H<sub>2</sub>O, 99.0%, Chem-Supply Pty Ltd) and ammonium heptamolybdate tetrahydrate ((NH<sub>4</sub>)<sub>6</sub>Mo<sub>7</sub>O<sub>24</sub>·4H<sub>2</sub>O, 81.0–83.0% as MoO<sub>3</sub>, Chem-Supply Pty Ltd) were used as the metal sources, which were dissolved separately into ultrapure water (18.2 M $\Omega$  cm, Milli-Q) to a metal concentration of 1 M. Ammonium hydroxide solution (NH<sub>4</sub>OH, 28.0–30.0%, Chem-Supply Pty Ltd) was then added to both solutions to reach pH = 10. Afterwards, the Ba-containing solution was pipetted slowly into the Mo-containing solution with constant stirring at ambient temperature, during which the co-precipitation reaction occurs according to Equation 1. The resultant precipitate was digested for 24 h, filtered and washed with Milli-Q water, dried in vacuum at 80 °C, and finally heat-treated in air at 600 °C for 10 h to obtain the BaMoO<sub>4</sub> product with high crystallinity.

$$Ba^{2+}(aq) + MoO_4^{2-}(aq) \rightarrow BaMoO_4(s)$$
(1)

Perovskite-type oxide BaMoO<sub>3</sub> was prepared by a reduction process. The as-obtained BaMoO<sub>4</sub>, loaded into a quartz tube, was heated to 900 °C at a temperature ramping rate of 5 °C min<sup>-1</sup>, held at this temperature for 3 h, and then cooled to ambient temperature naturally to yield the BaMoO<sub>3</sub> product, during which high-purity H<sub>2</sub> (99.999%, BOC) was introduced at a flow rate of 150 ml min<sup>-1</sup> to serve as a reducing agent. The reduction reaction during this process can be expressed as below:

$$BaMoO_4(s) + H_2(g) \rightarrow BaMoO_3(s) + H_2O(g)$$
<sup>(2)</sup>

#### 3.1.2 Fe-based perovskites La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3-δ</sub>

Fe-based perovskites  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  (x = 0.0, 0.2, 0.5, 0.8, and 1.0) were prepared by a sol–gel process. In brief, lanthanum nitrate hexahydrate ( $La(NO_3)_3 \cdot 6H_2O, 99.99\%$ , Sigma-Aldrich), barium nitrate ( $Ba(NO_3)_2, \ge 99\%$ , Sigma-Aldrich), strontium nitrate ( $Sr(NO_3)_2, \ge 99.0\%$ , Sigma-Aldrich), and iron nitrate nonahydrate ( $Fe(NO_3)_3 \cdot 9H_2O, \ge 98\%$ , Sigma-Aldrich) were weighed at their stochiometric ratios and dissolved in Milli-Q water under constant stirring. Afterwards, ethylenediaminetetraacetic acid (EDTA,  $\ge 99\%$ , Sigma-Aldrich) and citric acid (CA, 99.5%, Chem-Supply Pty Ltd) were introduced as complexing agents into the solution at a molar ratio of 1:2:1 for EDTA/CA/total metal content. To guarantee complete complexation, an ammonium hydroxide solution (NH<sub>4</sub>OH, 28.0–30.0%, Chem-Supply Pty Ltd) was added to adjust the solution pH to a value close to 6. The mixed solution was then continuously stirred at 150 °C to allow for the evaporation of water and the formation of a clear gel. The gel was baked in a furnace at 250 °C (at a temperature ramping rate of 5 °C min<sup>-1</sup>) for 5 h to yield a solid precursor, which was further calcined in air at a furnace temperature of 1100 °C (at a temperature ramping rate of 5 °C min<sup>-1</sup>) for 5 h to obtain the final products. The calcined samples were finely ground using a mortar and pestle prior to use.

#### 3.1.3 Co-based perovskites BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3-δ</sub>

The hexagonal-structured BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ 1</sub> perovskite (denoted as *h*-BCF) and BaCo<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3- $\delta$ </sub> (BCF82) were prepared by a sol-gel process using procedures similar to those for  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$ , except that the metal sources used are barium (Ba(NO<sub>3</sub>)<sub>2</sub>, nitrate ≥99%, Sigma-Aldrich), cobalt nitrate hexahydrate >98%. Sigma-Aldrich),  $(Co(NO_3)_2 \cdot 6H_2O,$ and iron nitrate nonahydrate  $(Fe(NO_3)_3 \cdot 9H_2O_2) \ge 98\%$ , Sigma-Aldrich), and that the calcination was conducted in air at a furnace temperature of 1000 °C (at a temperature ramping rate of 5 °C min<sup>-1</sup>) for 10 h to obtain the final products.

The cubic-structured BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ 2</sub> perovskite (denoted as *c*-BCF) was prepared by reducing *h*-BCF in an inert nitrogen atmosphere. The as-prepared *h*-BCF was loaded into a quartz tube, heated to 900 °C at a temperature ramping rate of 5 °C min<sup>-1</sup>, held at this temperature for 0.5 h, and then cooled to ambient temperature naturally to yield the *c*-BCF product, during which high-purity N<sub>2</sub> (99.999%, BOC) was introduced at a flow rate of 150 ml min<sup>-1</sup> to serve as a reducing agent. The reduction reaction during this process can be expressed as below:

 $BaCo_{0.7}Fe_{0.3}O_{3-\delta I} \text{ (hexagonal)} \rightarrow BaCo_{0.7}Fe_{0.3}O_{3-\delta 2} \text{ (cubic)} + 1/2(\delta 2 - \delta I)O_2$ (3)

#### 3.1.4 Alkali-metal-doped perovskites La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3-δ</sub>

Alkali-metal-doped lanthanum ferrites (La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub>, *x* = 0, 0.05, 0.1, 0.2, and 0.3) were prepared by a modified sol–gel process with a reduced calcination temperature for phase formation. Most of the experimental procedures are similar to those for La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub>, except that the metal sources used are lanthanum nitrate hexahydrate (La(NO<sub>3</sub>)<sub>3</sub>·6H<sub>2</sub>O, 99.99%, Sigma-Aldrich), sodium nitrate (NaNO<sub>3</sub>, 99.0%, Chem-Supply Pty Ltd), and iron nitrate nonahydrate (Fe(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O, ≥98%, Sigma-Aldrich), and that the calcination was conducted in air at a furnace temperature

of 600 °C (at a temperature ramping rate of 2.5 °C min<sup>-1</sup>) for 3 h to obtain the final products.

#### **3.2 Materials characterizations**

**X-ray diffraction (XRD)**: The crystalline structure was investigated by X-ray diffraction (XRD, Bruker D8 Advance) using Cu K $\alpha$  radiation ( $\lambda = 0.15418$  nm) at a tube voltage of 40 kV and a tube current of 40 mA. All XRD patterns were collected under ambient conditions. Rietveld refinement of the XRD patterns was performed using the GSAS program and EXPGUI interface to obtain detailed information about the phase structure.<sup>1</sup>

In situ X-ray diffraction: The structural evolution of *h*-BCF in the temperature range from room temperature to 900 °C under an air atmosphere was investigated by *in situ* X-ray diffraction (Rigaku Smartlab 3kW) using Cu K $\alpha$  radiation ( $\lambda = 0.15418$  nm) at a tube voltage of 40 kV and a tube current of 40 mA. The sample was loaded on an alumina holder and data were first collected at room temperature. Afterwards, the sample was heated to 900 °C at a temperature ramping rate of 5 °C min<sup>-1</sup>, and data were collected in the 500–900 °C range with an interval of 50 °C after the sample was settled for 10 min at each temperature point. After data collection at 900 °C, the temperature program was reversed to allow the cooling of the sample and data were recorded at the same temperature range as that of the heating process. Data was also collected when the sample was cooled to room temperature.

**Transmission electron microscopy (TEM)**: The crystalline structure was also gleaned by high-resolution transmission electron microscopy (TEM, FEI Titan G2 80-200) at a 200 kV accelerating voltage. Fast Fourier transform (FFT) patterns were obtained using the Fiji (Fiji Is Just ImageJ) software.<sup>2</sup> High-angle annular dark-field scanning TEM (HAADF-STEM) imaging and energy-dispersive X-ray spectroscopy (EDS) mapping were also performed. The selected-area electron diffraction (SAED) patterns were collected for La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> (x = 0.8) sample. The TEM specimens were prepared by dripping a small portion of the sample powders dispersed in ethanol onto a carbon-coated Cu grid.

Scanning electron microscopy (SEM): The microstructure was studied by fieldemission scanning electron microscopy (SEM) using either a Zeiss 1555 or a Zeiss Neon 40EsB microscope. The SEM specimens were prepared by depositing the sample powders on a double-sided adhesive carbon tape attached to a SEM holder.

 $N_2$  sorption measurements: The specific surface area was calculated by the Brunauer–Emmett–Teller (BET) method using data from the nitrogen sorption measurements conducted at the nitrogen boiling point (-196 °C) on instruments of Micromeritics Tristar 3000, BELSORP-mini II, or Quantachrome AutoSorb-iQ3. The samples were outgassed under vacuum at 200 °C for 5–10 h prior to the measurements.

Inductively coupled plasma-optical emission spectrometry (ICP-OES): The atomic ratio for the sample  $La_{1-x}Na_xFeO_{3-\delta}$  (x = 0.2) was analyzed by performing inductively coupled plasma-optical emission spectrometry (ICP-OES) on a PerkinElmer Optima 8300 instrument. The as-prepared powdery sample was dissolved in concentrated nitric acid and then diluted to a certain concentration for the measurement.

**Thermogravimetric and differential scanning calorimetry analysis (TG-DSC)**: To investigate the reduction process from *h*-BCF to *c*-BCF, a combined thermogravimetric and differential scanning calorimetry analysis (TG-DSC) was performed under an argon (Ar) atmosphere on a PerkinElmer TGA 8000 instrument. About 30 mg of the *h*-BCF powder was loaded into an alumina crucible, heated to 900 °C at a temperature ramping rate of 5 °C min<sup>-1</sup>, and further held under this temperature for 1 h.

**Oxygen temperature-programmed desorption (O<sub>2</sub>-TPD)**: The reduction process from *h*-BCF to *c*-BCF was also studied by oxygen temperature-programmed desorption (O<sub>2</sub>-TPD), which was performed in pure Ar (15 mL min<sup>-1</sup>) at a temperature up to 930 °C with a temperature ramping rate of 10 °C min<sup>-1</sup> and a holding period at 930 °C for 1.5 h. The sample was sieved into 150-mesh granule and about 0.15 g of the granule was used for the O<sub>2</sub>-TPD experiment. The effluent gases were analyzed by a mass spectrometer (Hiden, QIC-20) to monitor the desorbed oxygen signal.

**Electrical conductivity measurement**: The electrical conductivity of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> was characterized in air at ambient temperature using a four-probe DC method. The BaMoO<sub>4</sub> powder was pressed and sintered into dense bar-shaped specimens with an approximate geometric dimension of  $2 \text{ mm} \times 6 \text{ mm} \times 20 \text{ mm}$ . The BaMoO<sub>3</sub> bar was obtained by reducing the BaMoO<sub>4</sub> bar under conditions identical to

those for the reduction synthesis of BaMoO<sub>3</sub> powder. Two silver wires acting as the current leads were fixed to the top and bottom surfaces of the bar using silver paste and another two silver wires serving as the voltage probes were fixed to the side surfaces of the bar. A constant direct current (DC) was applied to the current leads, and the voltage response at the voltage probes was collected by a source meter (Keithley 2440 5A) using the LabVIEW software (National Instruments). The electrical conductivity was quantified using the relationship given by Equation 4, where l is the shortest distance between the voltage probes, S is the smallest cross-sectional area, and R is the electrical resistance obtained from the current versus voltage plot, respectively.

$$\sigma = \frac{1}{R} \times \frac{l}{s} \tag{4}$$

**Raman spectroscopy**: The crystalline information was also gathered by Raman spectroscopy, which was performed at room temperature on a Horiba LabRAM HR Evolution Raman microscope using 532 nm laser as the radiation source.

**X-ray photoelectron spectroscopy (XPS)**: The surface chemical composition and electronic state were scrutinized by X-ray photoelectron spectroscopy (XPS, Kratos AXIS Ultra DLD) using a monochromatic Al K $\alpha$  source (hv = 1486.6 eV). The electron binding energy scale was calibrated by referencing the C 1s peak to 284.8 eV. The peak fitting of the XPS data was performed by using the public software package XPSPEAK 4.1.

**X-ray absorption spectroscopy (XAS)**: The electronic state of the samples was also analyzed by X-ray absorption spectroscopy (XAS) performed at synchrotron facilities. The XAS experiments for the La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> samples were conducted at the TLS BL11A beamline of the National Synchrotron Radiation Research Center (NSRRC) in Taiwan. The O *K*-edge soft XAS data were taken in the fluorescence yield mode. To calibrate the photon energy, the O *K*-edge spectra of a NiO sample was simultaneously measured.

The XAS experiments for the La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> samples were performed at the Soft Xray (SXR) Beamline at the Australian Synchrotron.<sup>3</sup> The O *K*-edge soft XAS data were collected using a multichannel plate detector in fluorescence yield mode. Data were analyzed using the QANT software package.<sup>4</sup> The photon energy was calibrated by applying the offset required to shift the concurrently measured reference spectra of MnO powder (for O *K*-edge) to its known energy positions.

#### 3.3 Electrode preparations

The working electrode was prepared by casting a certain aliquot of catalyst dispersion onto a 5-mm-diameter glassy carbon electrode (GCE, Pine Research Instrumentation). Prior to electrode preparation, the GCE was polished to a mirror finish using 0.05  $\mu$ m  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> slurries on a polishing cloth and then cleaned by ultrasonication in Milli-Q water.

For BaMoO<sub>4</sub> and BaMoO<sub>3</sub>, the catalyst dispersion was prepared by suspending 10 mg of powder in a mixed solution containing 1 mL of isopropanol and 10  $\mu$ L of 5 wt% Nafion solution (Nafion<sup>®</sup> 117 solution, Sigma-Aldrich), followed by ultrasonication for 30 min. Afterwards, 5  $\mu$ L of this catalyst dispersion was pipetted onto the GCE surface and allowed to dry naturally in air, yielding a loading density of *m* = 0.253 mg cm<sup>-2</sup> for the oxide catalyst. Electrodes modified by commercial molybdenum trioxide (MoO<sub>3</sub>, 99.5%, Sigma-Aldrich) and molybdenum dioxide (MoO<sub>2</sub>, 99.0%, Sigma-Aldrich) were prepared in the same manner to serve as control samples.

For the Fe-based perovskites  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$ , Co-based perovskites  $BaCo_{0.7}Fe_{0.3}O_{3-\delta}$ , and alkali-metal-doped perovskites  $La_{1-x}Na_xFeO_{3-\delta}$ , carbon black (Super P<sup>®</sup>, Alfa Aesar), which serves as a conductive agent, was added to prepare the catalyst dispersion. 10 mg of perovskite powder was mixed with 2 mg of carbon black in a solution containing 900 µL of absolute ethanol and 100 µL of 5 wt% Nafion solution, followed by ultrasonication for 1 h. Afterwards, 5 µL of this catalyst dispersion was pipetted onto the GCE surface and allowed to dry naturally in air, yielding a loading density of m = 0.255 mg cm<sup>-2</sup> for the perovskite catalyst.

#### **3.4 Electrochemical measurements**

#### 3.4.1 Electrochemical data collection

Electrocatalytic properties of the samples were measured at ambient temperature using a rotating disk electrode configuration (RDE, Pine Research Instrumentation) coupled with an electrochemical workstation (CHI760E, CH Instruments). The electrochemical tests were conducted in a standard three-electrode cell using aqueous potassium hydroxide (KOH) solutions as the alkaline electrolytes. The three-electrode

systems consist of a catalyst-modified GCE as the working electrode, a double junction silver/silver chloride (4 M KCl) (Ag/AgCl, Pine Research Instrumentation) as the reference electrode, and a graphite rod (Pine Research Instrumentation) or a platinum wire (Pine Research Instrumentation) as the counter electrode for the evaluation of the electrocatalytic hydrogen evolution reaction (HER) or oxygen evolution reaction (OER), respectively. For the HER, a 1 M KOH solution was employed as the electrolyte, which was purged with ultrahigh purity Ar (>99.999%, BOC) before and during the HER experiments. For the OER, a 0.1 M KOH solution was used as the electrolyte, which was bubbled with ultrahigh purity O<sub>2</sub> (99.995%, BOC) prior to the OER experiments. The KOH solutions were freshly prepared before each experiment by dissolving high-purity KOH pellets (99.99%, Sigma-Aldrich) into Milli-Q water. The electrocatalytic HER activity was evaluated by performing linear sweep voltammetry (LSV) at a 5 mV s<sup>-1</sup> scan rate in the potential window of -1.8-0.9 V vs. Ag/AgCl. The HER stability test was assessed by running 1000 continuous cyclic voltammetry (CV) scans at a 100 mV s<sup>-1</sup> scan rate in the potential range between -1.5and -1.1 V vs. Ag/AgCl. The electrocatalytic OER activity was evaluated by performing CV at a slow scan rate of 10 mV s<sup>-1</sup> in the potential window of 0.2–1.0 or 0.2-1.1 V vs. Ag/AgCl. The OER stability was assessed by running chronopotentiometry with the working electrode held at a constant current density of 5 mA  $cm_{geo}^{-2}$ . Throughout these measurements, the working electrode was maintained at a rotation speed of 2000 revolutions per minute (rpm) to readily remove gaseous H<sub>2</sub> or O<sub>2</sub> product generated on the catalyst surface.

### 3.4.2 Electrochemical data analysis

The measured potentials versus Ag/AgCl were converted to the reversible hydrogen electrode (RHE) by using the following Nernst equation:

$$E_{RHE} = E_{Ag/AgCl}^0 + E_{Ag/AgCl} + 0.0591 \times \text{pH}$$
(5)

where  $E_{Ag/AgCl}^{0}$  is the standard potential of Ag/AgCl,  $E_{Ag/AgCl}$  is the experimentally measured potential versus Ag/AgCl, and  $E_{RHE}$  is the converted potential versus RHE, respectively. To compensate for the effect of electrolyte resistance, the potentials reported in this work were further corrected using the below equation:

$$E_{\rm iR-corrected} = E_{\rm RHE} - iR_{\rm s} \tag{6}$$

where  $E_{iR-corrected}$  is the corrected potential, *i* is the current (in A), and  $R_s$  is the ohmic electrolyte resistance (~8  $\Omega$  for 1 M KOH solution and 45~50  $\Omega$  for 0.1 M KOH) obtained from high-frequency alternating current (AC) impedance, respectively. The overpotential ( $\eta$ ) is defined as the difference between the corrected potential ( $E_{iR-corrected}$ ) and the standard equilibrium potential ( $E^0$ , which is 0 V or 1.229 V vs. RHE for the HER or OER, respectively) according to the following equation:

$$\eta = |E_{\text{iR-corrected}} - E^0| \tag{7}$$

The as-obtained current was normalized by the geometric area of the GCE,  $S_{GCE}$  (0.196 cm<sup>2</sup>), to yield the current density *j* (in mA cm<sup>-2</sup><sub>geo</sub>), as described below:

$$j = 1000 \times i/S_{\rm GCE} \tag{8}$$

The current density was further normalized by the BET surface area of the perovskite oxides,  $S_{\text{BET}}$  (in m<sup>2</sup> g<sup>-1</sup>), to yield the specific activity (*SA*, in mA cm<sup>-2</sup><sub>oxide</sub>), as shown below:

$$SA = j/(10 \times S_{\text{BET}} \times m) \tag{9}$$

where *m* is the mass loading of the perovskite oxide catalyst (0.253 or 0.255 mg cm<sup>-2</sup>).

The polarization data were plotted as the overpotential ( $\eta$ ) versus the logarithm of the current density (log*j*) or the logarithm of the specific activity (log*SA*) to yield the Tafel plots, whose linear portions at the low overpotential regimes were fitted to the Tafel equation as given below to gain the Tafel slope (*b*):

$$\eta = a + b\log j$$
  
(10)  
or  
 $\eta = a + b\log SA$ 

(11)

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# Chapter 4 From scheelite BaMoO<sub>4</sub> to perovskite BaMoO<sub>3</sub>: Enhanced electrocatalysis toward the hydrogen evolution in alkaline media\*

#### 4.1 Abstract

The discovery of new, inexpensive, and efficient electrocatalysts for the hydrogen evolution reaction (HER) in alkaline solutions holds key to the realization of clean hydrogen production through water electrolysis. While molybdenum (Mo)-based inorganic compounds have been extensively investigated as catalyst candidates toward the alkaline HER, Mo-based oxides, in particular, complex oxides, are rarely explored. Here we report a Mo-containing, metallic BaMoO<sub>3</sub> perovskite, which is derived from a scheelite-type, insulating BaMoO<sub>4</sub> oxide through a thermal reduction-induced phase transformation, as a potential electrocatalyst for driving the alkaline HER. The BaMoO<sub>3</sub> perovskite made of interconnected MoO<sub>6</sub> octahedra is found to be more HER-active than the BaMoO<sub>4</sub> scheelite consisting of isolated MoO<sub>4</sub> tetrahedra, showing a significant increase in intrinsic activity by about one order of magnitude, which is due to the stabilized Mo tetravalent state, the increased surface oxygen vacancy concentration, and the improved electrical conductivity of BaMoO<sub>3</sub>. Importantly, BaMoO<sub>3</sub> exhibits a smaller overpotential to deliver a geometric current density of -10 mA cm<sup>-2</sup><sub>geo</sub> when compared with many of the bulk-sized perovskite catalysts comprising other transition metals (e.g., Mn, Fe, Co, and Ni) and the intensively studied Mo-based catalysts (e.g., MoS<sub>2</sub>), making it highly promising as an alternative electrocatalyst for the alkaline HER.

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#### 4.2 Introduction

Water electrolysis is able to convert electricity to chemical energy stored in the form of hydrogen  $(H_2)$ , which, unlike the conventional fossil fuels, is regarded as a clean energy carrier, supplying energy without substantial carbon footprints. One critical step involved in the splitting of water is the hydrogen evolution reaction (HER) at the cathode [1-3], which suffers from sluggish kinetics, especially in alkaline solutions, as described by Equation 1. To drive the HER half-reaction, platinum is considered the most efficient electrocatalyst because of its optimal binding to the hydrogen but is limited in widespread use due to its scarcity and prohibitive cost [4, 5]. Molybdenum (Mo) compounds, such as boride [6], carbide [6], phosphide [7], and sulfide [8-10], represent a large group of inexpensive alternatives that afford a suitable hydrogen binding strength and thus exhibit good HER activity. In particular, molybdenum disulfide (MoS<sub>2</sub>), known as the very first catalyst material that reopened the fundamental research of the HER electrocatalysis in acidic media [11], has been demonstrated with significant progress in terms of the HER activity over the past decade [12]. However, its catalytic capability in the alkaline media cannot compare with that in the acidic media, which, in principle, is primarily a result of the slower HER kinetics in bases than in acids, often by at least two orders of magnitude [13]. In addition, the pristine MoS<sub>2</sub> is a poor electronic conductor, which requires additional post-treatment or alternative synthetic approach to promote the transformation to or stabilization of a more conducting phase showing enhanced catalytic activity [14, 15]. Therefore, the development of new electrocatalytic materials for efficiently catalyzing the alkaline HER is highly desirable.

$$2H_2O + 2e^- \rightarrow H_2 + 2OH^- \tag{1}$$

Transition metal oxides, as an important class of inorganic compounds, have received considerable attention in the field of electrocatalysis (for instance, the oxygen electrocatalysis) [16] owing to their fascinating physicochemical properties with low cost, high stability, and environmental compatibility. While previously considered as HER-inactive resulting from the inappropriate hydrogen adsorption energy and unsatisfactory electrical conductivity, several unary metal oxides have been rationally designed to allow for increased competitiveness as HER electrocatalysts [17-19]. For example, Gong et al. [17] increased the alkaline HER activity of NiO-based nanostructured materials by constructing heterostructures with Ni metal and coupling

with conductive carbon nanotubes. Qiao and co-workers [18] utilized a strain engineering approach to activate the CoO nanorod catalyst through the introduction of abundant surface oxygen vacancies. In addition, Luo and colleagues [19] prepared a nonstoichiometric, mesoporous  $MoO_{3-x}$  oxide using a templating method, which showed favorable alkaline HER performance due to the mesoporous structure, the reduced Mo oxidation state, and the increased electrical conductivity. These endeavors suggest the possibility of making transition metal oxides more catalytically active toward the alkaline HER, both intrinsically and extrinsically, by regulating the electronic structure and/or modifying the material morphology.

Compared to unary metal oxides, multi-metal oxides usually excel in view of the ability to allow for the fine-tuning of their electronic structures and the resultant modulation of the binding with the reaction intermediates, thereby rendering high intrinsic HER activity achievable. Of importance, complex oxides having a perovskite structure, for example, ABO<sub>3</sub> simple perovskites [20] and AA'B<sub>2</sub>O<sub>6</sub>/A<sub>2</sub>BB'O<sub>6</sub> double perovskites [21] where A is an alkaline-earth or rare-earth metal and B is a transition metal, are known for their compositional and structural flexibility and are therefore well suited for elucidating the structure-property relationships in a variety of catalytic processes such as the oxygen electrocatalysis [22-24], and more recently the alkaline HER electrocatalysis [25-34]. The perovskite structure can stabilize transition metals in their unique oxidation states unusually found in other material structures. For example, palladium (Pd) of mixed trivalent/tetravalent states was stabilized in the LaFe<sub>1-x</sub>Pd<sub>x</sub>O<sub>3- $\delta$ </sub> perovskite [23], which led to a more than 80 times higher intrinsic activity toward the oxygen reduction as compared to the zerovalent Pd metal. Furthermore, perovskite oxides typically have oxygen defects, often in the form of oxygen vacancies, associated with the changeable transition metal valences or stoichiometries, and such defects can play a decisive role in the electrocatalysis. For instance, the electrocatalytic oxygen evolution reactivity of a silicon-incorporated  $SrCo_{1-y}Si_yO_{3-\delta}$  system was found to be significantly higher than that of the parent  $SrCoO_{3-\delta}$  [24], due to the formation of extra oxygen vacancies that promoted the lattice oxygen participation during the catalysis. Also importantly, by taking advantage of the nature of the constituent elements in the perovskite structure, the conductivity property of the resultant perovskite oxides can be facilely modulated. This is exemplified by  $Ba_{0.5}Sr_{0.5}Co_{0.8}Fe_{0.2}O_{3-\delta}$ , which was poorly conductive at room temperature but

experienced a surge in the electrical conductivity upon the partial substitution of barium/strontium with praseodymium in the A-site [30], leading to substantially enhanced performance for the alkaline HER. It is believed that the elegant combination of these unique properties within one single perovskite structure, which is often unattainable in other material systems, can contribute to highly efficient HER electrocatalysis in the alkaline solutions.

In this work, we report a Mo-containing, metallic BaMoO<sub>3</sub> perovskite [35-37], which is derived from a scheelite-type, insulating BaMoO4 oxide through a thermal reduction-induced phase transition, as a potential electrocatalyst for facilitating the alkaline HER. While previously investigated as the candidate for the catalytic oxidation of 2-propanol [38] and photocatalytic splitting of water [39], BaMoO<sub>3</sub> has not yet been explored as an electrocatalytic material. When evaluated as the alkaline HER electrocatalyst, BaMoO<sub>3</sub> exhibits a significantly accelerated HER kinetics as compared with BaMoO<sub>4</sub>, showing an increase in intrinsic activity by about one order of magnitude, which is likely due to the fact that the BaMoO<sub>3</sub> perovskite stabilizes the tetravalent state of Mo, possesses a greater quantity of surface oxygen vacancies, and provides faster electron transport. Notably, BaMoO3 requires a smaller overpotential to reach a given geometric current density of  $-10 \text{ mA cm}_{geo}^{-2}$  when compared with many of the bulk-sized perovskite catalysts comprising other transition metals (for example, Mn, Fe, Co, and Ni) and the intensively explored Mo-based catalysts (including MoS<sub>2</sub>), demonstrating its promise as an efficient HER electrocatalyst worthy to be further optimized.

# 4.3 Results and discussion

# 4.3.1 Synthesis and structural characterizations

The synthesis of BaMoO<sub>3</sub> involves a two-step process. As illustrated in **Figure 4.1**, BaMoO<sub>4</sub> was initially prepared through the co-precipitation of Ba<sup>2+</sup> and MoO<sub>4</sub><sup>2-</sup> under mildly alkaline conditions, after which BaMoO<sub>3</sub> was produced by the thermal reduction of BaMoO<sub>4</sub> using H<sub>2</sub> as a reducing agent. Upon thermal reduction, the sample color changes from white for BaMoO<sub>4</sub> to dark red for BaMoO<sub>3</sub>, which, consistent with previous observations [38], suggests that a scheelite-to-perovskite phase transition takes place.



**Figure 4.1** Synthesis of BaMoO<sub>3</sub> perovskite. A schematic showing the synthesis of BaMoO<sub>3</sub> perovskite, involving two steps of co-precipitation synthesis of BaMoO<sub>4</sub> scheelite and its subsequent reduction. The atomic arrangements of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> are viewed along the [010] direction, with *c* axis vertical. In the tetragonal unit cell of the BaMoO<sub>4</sub> scheelite, the tetrahedra corresponding to the MoO<sub>4</sub> units are isolated from each other. In the cubic structure of the BaMoO<sub>3</sub> perovskite, the octahedra corresponding to the MoO<sub>6</sub> units are interconnected with one another (to illustrate this, the cubic unit cell is triplicated in the *c* direction). For simplicity, the Ba–O coordination is not given.

More direct evidence of the phase transformation comes from the XRD characterization. As shown in **Figure 4.2a**, both BaMoO<sub>4</sub> and BaMoO<sub>3</sub> exhibited strong, well-defined XRD peaks, indicative of a high level of crystallinity. The XRD peaks of BaMoO<sub>4</sub> can be perfectly assigned to the scheelite-type tetragonal structure with a space group of  $I4_1/a$ , in accord with the International Centre for Diffraction Data (ICDD) Powder Diffraction File (PDF) No. 00-029-0193 [41]. By comparison, the XRD peaks of BaMoO<sub>3</sub> align well with those of the perovskite-type cubic structure with a crystal symmetry of  $Pm\overline{3}m$  (ICDD PDF No. 01-084-9949 [41]). These phase structures were also verified by a detailed Rietveld refinement analysis (**Figure A.1 and Table A.1, Appendix A**), which gives calculated lattice parameters of a = 0.5582 nm and c = 1.2822 nm for the tetragonal BaMoO<sub>4</sub> and a = 0.4041 nm for the cubic BaMoO<sub>3</sub>. The low-intensity diffraction peak at  $2\theta$  of around 40.5° indicates the minor presence of an impurity phase of Mo metal, due likely to the complete reduction of a

fragment of the Mo species [42]. The weight percentage of this Mo impurity phase was quite low, at about 2.5 wt% as determined from the Rietveld refinement.



**Figure 4.2** Structural characterizations of BaMoO<sub>3</sub> perovskite. (a) XRD patterns of BaMoO<sub>4</sub> and BaMoO<sub>3</sub>. The tick marks below the patterns represent the positions of the Bragg reflections of the standards, i.e., the tetragonal phase for BaMoO<sub>4</sub> scheelite (space group  $I4_1/a$ , ICDD PDF No. 00-029-0193) and the cubic phase for BaMoO<sub>3</sub> perovskite (space group  $Pm\overline{3}m$ , ICDD PDF No. 01-084-9949). The peak marked with an asterisk corresponds to the Mo metal phase. (b) High-resolution TEM image of BaMoO<sub>4</sub> recorded with the electron beam along the [111] zone axis. (c) High-resolution TEM image of BaMoO<sub>3</sub> recorded with the electron beam along the [001] zone axis. Insets in (b) and (c) show the corresponding FFT patterns. (d) SEM image of BaMoO<sub>4</sub>. (e) SEM image of BaMoO<sub>3</sub>.

The phase transition is also corroborated by TEM observations. As depicted in **Figure 4.2b** and **c**, lattice fringes with interplanar spacings of 0.34 and 0.29 nm are observed in the high-resolution TEM images, which match the (112) and (110) planes of tetragonal-structured BaMoO<sub>4</sub> and cubic-structured BaMoO<sub>3</sub>, respectively. The distinct crystalline structures of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> are apparently discernible when one further compares their respective fast Fourier transform (FFT) patterns that reflect the characteristic diffraction spots of the [111] zone axis for BaMoO<sub>4</sub> and [001] zone axis for BaMoO<sub>3</sub> (insets of **Figure 4.2b** and **c**). As demonstrated in **Figure 4.1**, the two phases are different in that in the tetragonal BaMoO<sub>4</sub> scheelite Mo in the hexavalent state (Mo<sup>6+</sup>) is fourfold coordinated to the O anion forming MoO<sub>4</sub> perovskite Mo in the tetravalent state (Mo<sup>4+</sup>) is sixfold coordinated to the O anion forming MoO<sub>6</sub> octahedra that are corner-shared with each other [42].

The XPS survey spectra reveal that both BaMoO<sub>4</sub> and BaMoO<sub>3</sub> are composed of Ba, Mo, and O elements (**Figure A.2**). Further, HAADF-STEM imaging and EDS mapping analysis of BaMoO<sub>3</sub> suggests that these constituent elements are homogeneously distributed throughout the BaMoO<sub>3</sub> sample (**Figure A.3**). The microstructure of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> was examined by SEM imaging (**Figure 4.2d** and **e**), from which particles with a (sub)micrometer-scale size are seen, signifying their bulk nature. A closer look at the SEM results indicates that the BaMoO<sub>3</sub> sample has a somewhat less uniform particle size, which is likely caused by the cracking or sintering of the more uniformly sized BaMoO<sub>4</sub> precursor during reduction at elevated temperatures. Nevertheless, both samples exhibit a similar specific surface area, i.e.,  $0.7 \text{ m}^2 \text{ g}^{-1}$  for BaMoO<sub>4</sub> and  $1.2 \text{ m}^2 \text{ g}^{-1}$  for BaMoO<sub>3</sub>, as measured from the nitrogen sorption experiments using the BET method.

#### **4.3.2** Evaluation of electrocatalytic performance

The electrocatalytic activity of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> toward the HER was assessed using a three-electrode configuration in a 1 M KOH solution. Figure 4.3a displays the LSV curves where the current is normalized to the geometric area of the GCE substrate and the potential is *iR*-corrected to compensate for the electrolyte resistance. As expected, the bare GCE exhibits negligible HER activity over the potential range of 0.0-0.7 V vs. RHE [44]. On the contrary, both BaMoO<sub>4</sub> and BaMoO<sub>3</sub> show a large current response in the same potential range. Noticeably, BaMoO<sub>3</sub> displays an earlier

onset potential, as defined to be the potential required to approach a current density of  $-1 \text{ mA cm}_{\text{geo}}^{-2}$ , than BaMoO<sub>4</sub> does (-0.197 V vs. -0.353 V) and delivers higher current density with the further increase of overpotential (inset of **Figure 4.3a**). When one compares the overpotential required to reach  $-10 \text{ mA cm}_{\text{geo}}^{-2}$  ( $\eta_{10}$ ), a generic metric related to the production of solar fuels [45], BaMoO<sub>3</sub> is found to outperform BaMoO<sub>4</sub>, showing a reduction in  $\eta_{10}$  by more than 200 mV (i.e., 336 mV vs. 561 mV). Furthermore, the  $\eta_{10}$  value of BaMoO<sub>3</sub> is found to be smaller than that of many of the reported bulk-sized, Mo-containing catalysts (e.g., Mo oxide [6] and sulfide [8-10]) and perovskite catalysts (e.g., Mn- [25], Fe- [26, 27], Co- [28-33], and Ni-based [34]) tested under the same alkaline electrolytes (**Figure 4.3b**). This signifies the great promise of BaMoO<sub>3</sub> as an efficient catalyst for the alkaline HER.



**Figure 4.3** Electrocatalytic performance of BaMoO<sub>3</sub> perovskite toward the HER in 1 M KOH. (a) LSV curves of BaMoO<sub>4</sub> and BaMoO<sub>3</sub>, where currents are normalized to

the geometric area of GCE (in mA  $cm_{geo}^{-2}$ ). The LSV curve of GCE is shown for reference. The inset gives an enlargement of the low current density region. (b) A comparison of the HER activity of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> with other reported bulk-sized, Mo-containing catalysts (e.g., Mo oxide and sulfide) and perovskite catalysts (e.g., Mn-, Fe-, Co-, and Ni-based), using the metric of the overpotential needed to obtain a current density of 10 mA  $cm_{geo}^{-2}$ . (c) LSV curves of BaMoO<sub>4</sub> and BaMoO<sub>3</sub>, where currents are normalized to the BET surface area to give the specific activity (in mA  $cm_{oxide}^{-2}$ ). The inset gives a comparison of the specific activity at select overpotentials. (d) Tafel plots of BaMoO<sub>4</sub> and BaMoO<sub>3</sub>. (e) LSV curves of BaMoO<sub>3</sub> before and after 1000 CV cycles.

A comprehensive comparison with literature results is provided in **Table A.2**. It is interesting to note that the BaMoO<sub>3</sub> perovskite oxide shows greater HER activity compared to the Mo simple oxides MoO<sub>3</sub> and MoO<sub>2</sub> (**Figure 4.3b, Figure A.4 and A.5**), suggesting that Mo incorporated in a complex oxide framework may perform better than incorporated in a simple oxide structure. It should also be noted that there is still room for the further activity improvement of the BaMoO<sub>3</sub> perovskite, as the state-of-the-art perovskite oxide catalysts are reported with even smaller  $\eta_{10}$  values, for example, the well-designed, Co-based (Gd<sub>0.5</sub>La<sub>0.5</sub>)BaCo<sub>2</sub>O<sub>5.5+ $\delta$ </sub> double perovskite having a  $\eta_{10}$  of less than 200 mV [46, 47].

The surface area of an HER electrocatalyst is known to affect its apparent catalytic activity. The HER current of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> is therefore normalized to their respective BET surface area to obtain the specific activity (**Figure 4.3c**), which serves as a metric for assessing the intrinsic activity [47]. As is obvious from **Figure 4.3c** inset and **Table A.3**, at the select overpotentials of 350, 400, and 450 mV, BaMoO<sub>3</sub> showed a significantly higher specific activity than BaMoO<sub>4</sub> by approximately one order of magnitude, indicating its greater intrinsic performance.

To elucidate the HER reaction kinetics, Tafel plots were derived from the LSV data and shown in **Figure 4.3d**. The Tafel slope for BaMoO<sub>3</sub> was calculated to be 110 mV dec<sup>-1</sup>, which is much lower than that for BaMoO<sub>4</sub> (189 mV dec<sup>-1</sup>). This manifests the faster HER kinetics on the BaMoO<sub>3</sub> perovskite catalyst with respect to the BaMoO<sub>4</sub> scheelite catalyst, because a catalyst featuring a smaller Tafel slope tends to give increased HER currents at smaller increments of overpotential [30]. Furthermore, the Tafel slope of BaMoO<sub>3</sub> is lower than that of MoO<sub>3</sub> and MoO<sub>2</sub> (**Figure A.6**) and compares favorably to that of the earlier reported Mo-containing catalysts and perovskite catalysts (**Table A.2**), demonstrating the superior HER kinetics of BaMoO<sub>3</sub>.

In alkaline media, the HER could take place through either a Volmer–Heyrovsky pathway or a Volmer–Tafel pathway via the below reactions [48]:

(Volmer reaction) 
$$M + H_2O + e^- \leftrightarrow M - H + OH^-$$
 (2)

(Heyrovsky reaction) 
$$M-H + H_2O + e^- \leftrightarrow H_2 + OH^- + M$$
 (3)

(Tafel reaction) 
$$2M-H \leftrightarrow H_2 + 2M$$
 (4)

where M represents an active site onto which the H atom adsorbs. Both pathways involve a Volmer step, in which electron-coupled water dissociation occurs to form the adsorbed M–H intermediate, followed by a Heyrovsky or Tafel step where M–H is transformed into molecular H<sub>2</sub> through different mechanisms. Previous research suggests that the rate-determining step of the alkaline HER could be assigned using the Tafel slope [1]; a Tafel slope near 120, 40, and 30 mV dec<sup>-1</sup> is anticipated, respectively, for the Volmer, Heyrovsky, and Tafel reaction to be rate-limiting. While the exact catalytic mechanism remains elusive, the Tafel slopes of BaMoO<sub>4</sub> and BaMoO<sub>3</sub>, which are closer to 120 mV dec<sup>-1</sup> than to 40 or 30 mV dec<sup>-1</sup>, reveal that they might catalyze the HER following a Volmer–Heyrovsky pathway where the reaction rate is controlled by the Volmer process.

Apart from the catalytic activity, it is also important to examine the electrochemical stability in the assessment of a new type of HER catalyst. For this purpose, the BaMoO<sub>3</sub> perovskite catalyst was subjected to 1000 continuous potential cycles. As presented in **Figure 4.3e**, negligible decay is observed for the polarization data recorded before and after the cycling, indicating the good HER stability of BaMoO<sub>3</sub> in alkaline electrolytes.

# 4.3.3 Origins of the activity enhancement

Understanding the origins of the enhanced HER activity observed on the BaMoO<sub>3</sub> perovskite relative to the BaMoO<sub>4</sub> scheelite is critical to the design of improved electrocatalysts. In complex transition metal oxide catalysts, the transition metal–oxygen building block is assumed to be responsible for the electrocatalytic process

[30]. Therefore, it is believed that the HER activity difference between BaMoO4 and BaMoO<sub>3</sub> mainly originates from the intrinsic difference in the respective active site, i.e., disconnected MoO4 tetrahedra in a tetragonal structure for BaMoO4 and interconnected MoO<sub>6</sub> octahedra in a cubic structure for BaMoO<sub>3</sub>. From the viewpoint of crystal structure, BaMoO<sub>3</sub> with a higher symmetry and better connection of active sites, which offers a collinear covalent bridge of -Mo-O-Mo-O-, is expected to allow for a shorter reaction path and therefore is considered to be more advantageous to the electrocatalysis [46]. More importantly, BaMoO<sub>3</sub> has a lower valence state of Mo as compared with BaMoO<sub>4</sub> (4+ vs. 6+), which can lead to increased d band filling of Mo and thereby tune the hydrogen adsorption energy in the Volmer process as mentioned earlier [49]. This is directly supported by the similar activity trend of Mo simple oxides in alkaline solutions. As shown in Figure 4.3b and Figure A.5, MoO<sub>2</sub> with a lower Mo oxidation state delivered greater HER activity than MoO<sub>3</sub>, in agreement with literature results [6]. Further evidence comes from the observation that the activity of MoS<sub>2</sub> toward the HER in acidic electrolytes was significantly boosted after a lithium intercalation treatment that caused a reduction in the Mo valence [50].

Considering that the catalyst surface is more relevant to the electrocatalysis [51], highresolution XPS was conducted to verify the reduced valence of the surface Mo cation in BaMoO<sub>3</sub>. Figure 4.4a shows the Mo 3d core-level XPS spectra of BaMoO<sub>4</sub> and BaMoO<sub>3</sub>. A spin-orbit doublet with peaks at the binding energies of about 232.2 and 235.4 eV was observed in BaMoO<sub>4</sub>, which can be ascribed to the 3d<sub>5/2</sub> and 3d<sub>3/2</sub> of the Mo cation being at the highest oxidation state ( $Mo^{6+}$ ) [52]. By comparison, the Mo 3d spectra of BaMoO<sub>3</sub> appears to be more complex and can be deconvoluted into four components. The doublet with peaks at 229.2 and 232.4 eV is attributed to Mo<sup>4+</sup> [50, 53], which, however, only accounts for a small amount of the overall Mo species. This can be explained by the partial oxidation of the BaMoO3 surface during the XPS sample preparation or testing, a phenomenon often encountered on tetravalent Mobased compounds [53, 54], as evidenced by the doublet (at 231.9 and 235.1 eV) sitting in between the regions of Mo<sup>4+</sup> and Mo<sup>6+</sup>. In addition, another doublet with peaks at 227.2 and 230.3 eV is assigned to the metallic molybdenum (Mo<sup>0</sup>) [55], in line with the existence of the minor Mo metal phase as detected by XRD. The last doublet was identified at relatively higher binding energies of 234.3 and 237.5 eV, probably associated with the presence of relaxed surface phase, which is complemented by the

emergence of a pair of shoulder peaks at the higher binding energy region of the Ba 3d core lines (**Figure 4.4b**). According to previous reports [56], the appearance of relaxed surface phase is likely caused by the surface defects such as cation defects and oxygen vacancies. Such kind of defects is not unexpected in the BaMoO<sub>3</sub> sample obtained from the reduction of BaMoO<sub>4</sub>, given that a tiny amount of metallic Mo was produced in the same process, which could result in a departure of the Mo stoichiometry from unity and simultaneously lead to the formation of oxygen vacancies to compensate for any possible charge imbalance. This process can be expressed by the following equation, where  $\delta$  denotes the number of oxygen vacancies.

$$BaMoO_4(s) + (1+\delta)H_2(g) \rightarrow BaMo_{1-\delta/2}O_{3-\delta}(s) + \delta/2Mo(s) + (1+\delta)H_2O(g)$$
(5)



**Figure 4.4** Chemical and electrical properties of BaMoO<sub>3</sub> perovskite. (a–c) Highresolution XPS spectra of BaMoO<sub>4</sub> and BaMoO<sub>3</sub>. (a) Mo 3d, (b) Ba 3d, and (c) O 1s. (d) Electrical conductivity of BaMoO<sub>4</sub> and BaMoO<sub>3</sub> measured under ambient conditions. The inset is a schematic illustration of the scheelite-to-perovskite phase transition, along with a change from insulating to metallic conduction.

The formation of oxygen vacancies is thought to be another important factor that contributes to the enhanced HER performance on BaMoO<sub>3</sub>. Recent theoretical and experimental studies on the transition metal oxide catalysts have suggested that oxygen vacancies on the catalyst surface can facilitate the water dissociation (i.e., the OH-H bond cleavage) [18], a vital step in the Volmer reaction, especially for the alkaline HER [2]. For instance, facile water dissociation was achieved when the surface of a CoO electrocatalyst was enriched with oxygen vacancies by means of strain engineering [18], showing significantly enhanced alkaline HER activity. In our case, the presence of surface oxygen vacancies is also evident in the high-resolution O 1s XPS scans (Figure 4.4c), which can be decomposed into three subpeaks that correspond to the lattice oxygen, defective oxygen (i.e., oxygen vacancy), and chemisorbed oxygen, respectively, from low to high binding energies [57]. In addition, after thermal reduction of BaMoO4, the as-obtained BaMoO3 offers a larger formation of surface oxygen vacancies, as indicated by an obvious increase in the concentration of the defective oxygen, which was calculated based on the relative area of the subpeaks (Table A.4). It is worth noting that the peak positions for the defective and chemisorbed oxygen shifted to somewhat larger binding energies, which is likely a result of the modification in the coordination environment of Mo with O.

Furthermore, the electrical conductivity of an HER electrocatalyst represents another parameter that is crucial to high catalytic activity. Generally, efficient charge transfer is required for the Volmer reaction to occur. In other words, if the catalyst candidate is not conductive enough to allow for the transfer of electrons to the active sites, the Volmer step will be prevented from proceeding. In fact, the important role of electronic conductivity is widely acknowledged in the HER electrocatalysis on the MoS<sub>2</sub> catalyst [14, 15]. For example, MoS<sub>2</sub> with the semiconducting 2H phase shows limited HER activity due to its high electrical resistance, which can be mitigated through phase transformation to the metallic 1T phase, leading to markedly improved performance [14, 15]. In addition, for Mo simple oxides, the higher HER activity of MoO<sub>2</sub> than MoO<sub>3</sub> is likely associated with their difference in electronic conductivity, as the bulk MoO<sub>2</sub> is metallic whereas MoO<sub>3</sub> is insulating [58]. In a similar fashion, the scheelite-to-perovskite phase change from BaMoO<sub>4</sub> to BaMoO<sub>3</sub> could give rise to a transition of the electrical conductivity property from insulating to metallic behavior. As presented in **Figure 4.4d**, four-probe DC measurements revealed an electrical

conductivity as low as  $3.4 \times 10^{-6}$  S cm<sup>-1</sup> for BaMoO<sub>4</sub>, which agrees with Maji et al.'s testing result [59]. In stark contrast, BaMoO<sub>3</sub> shows a drastic increase in the electrical conductivity by more than seven orders of magnitude  $(1.4 \times 10^2$  S cm<sup>-1</sup>). Note that this value could be underestimated (with literature results approaching  $10^3$ – $10^4$  S cm<sup>-1</sup> [35-37]), due likely to the insufficient densification of the BaMoO<sub>3</sub> bar prepared from reducing the relatively more densified BaMoO<sub>4</sub> bar. Indeed, this metallic nature of BaMoO<sub>3</sub> is also supported by its narrow band gap (around 2 eV [39]), much smaller than that of BaMoO<sub>4</sub> (above 4 eV [60]). The metallicity of BaMoO<sub>3</sub> is closely related to the electronic configuration of the Mo<sup>4+</sup> ion stabilized in the perovskite structure, which has two electrons filled in the d band, resulting in a large carrier density [37].

#### 4.4 Conclusions

In summary, we have demonstrated how a facile scheelite-to-perovskite phase transition can lead to tremendously improved electrocatalytic properties in barium molybdate catalysts for the alkaline HER, with a reduction in the overpotential by more than 200 mV and a rise in the intrinsic activity by about one order of magnitude. We further show that the interconnected MoO<sub>6</sub> octahedra in the cubic-structured BaMoO<sub>3</sub> perovskite is intrinsically more active than the disconnected MoO<sub>4</sub> tetrahedra in the tetragonal-structured BaMoO4 scheelite, which offers a reduced oxidation state of Mo, a larger presence of surface oxygen vacancies, and a higher electrical conductivity of the catalyst material, all favoring the proceeding of the Volmer step in the alkaline HER. Importantly, at this current stage, the promise of the target material researched here (i.e., BaMoO<sub>3</sub> perovskite with a bulk particle size) as alkaline HER electrocatalyst is fully showcased, rivaling many of the reported bulk-sized perovskite catalysts containing other transition metals as well as the intensively studied Mo-based catalysts, in particular, MoS<sub>2</sub>. Looking back the history of the MoS<sub>2</sub> catalyst, one would find a dramatic growth in its electrocatalytic HER activity over the last decade or so, which is made possible through materials design strategies such as nanostructuring, elemental doping, defect engineering, and crystal phase tuning [12]. In fact, all these strategies can be implemented on the BaMoO<sub>3</sub> perovskite, given the versatility of the perovskite structure [51]. Therefore, further progress in promoting the alkaline HER performance of the BaMoO<sub>3</sub> perovskite is very much expected in the years to come.

#### 4.5 References

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# Chapter 5 Fe-based perovskites for catalyzing the hydrogen evolution reaction in alkaline solutions

# 5.1 Abstract

The hydrogen evolution reaction (HER) as the reaction occurring at the cathode of a water electrolyzer is important to the overall water splitting efficiency, but is limited by sluggish reaction kinetics. While perovskite-type oxides have seen application as the electrocatalysts to facilitate the HER reaction rate, most of the current research focuses on cobalt-containing perovskites. In this work, a series of Fe-based  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  (x = 0.0, 0.2, 0.5, 0.8, and 1.0) perovskites, designed by substituting the alkaline-earth metals Ba and Sr for the rare-earth metal La, were evaluated as alternative candidates for catalyzing the HER in alkaline solutions. All the Ba/Sr substituted samples exhibited enhanced alkaline HER activity compared to the pristine LaFeO<sub>3</sub>, with La<sub>0.2</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>0.8</sub>FeO<sub>3- $\delta$ </sub> (x = 0.8) delivering the best activity with a 216-mV reduction in the overpotential to afford a current density of -10 mA  $cm_{geo}^{-2}$ . A comprehensive X-ray spectroscopic study indicates that the enhanced HER activity is correlated with the increased oxidation state of the Fe cation and the enhanced covalency of the Fe–O bond, which is closely related to the phase transition induced by Ba/Sr substation. The optimized activity of the Fe-based perovskite compares favorably to that of many other perovskites (e.g., those containing Co and Ni), highlighting the potential of Fe-based perovskites as HER catalysts.

#### **5.2 Introduction**

The electrochemical water splitting has recently been attracting growing attention worldwide because of its potential for large-scale production of clean hydrogen fuels.<sup>1</sup> However, its cathodic half reaction, namely hydrogen evolution reaction (HER), suffers from slow reaction kinetics that leads to inefficient energy conversion, especially in alkaline solutions.<sup>2</sup> To mitigate the energy penalty of this process, platinum group metal-based electrocatalysts, e.g., those containing platinum (Pt),<sup>3</sup> ruthenium (Ru),<sup>4</sup> or iridium (Ir),<sup>5</sup> have been developed with the highest catalytic activity, but the low abundance and high cost of these noble metals restrict their large-scale use. Therefore, research efforts should be devoted to exploring alternative catalytic materials that comprise inexpensive elements and exhibit competitive efficiency.

Over the past decade, a great variety of inorganic compounds have been explored as candidates for catalyzing the HER in alkaline media, including boride,<sup>6</sup> carbide,<sup>7</sup> nitride,<sup>8</sup> oxide,<sup>9</sup> phosphide,<sup>10</sup> sulfide,<sup>11</sup> and selenide.<sup>12</sup> Among these candidates, oxide materials have received increasing interest in the field of HER electrocatalysis due to their cost-effectiveness, simplicity of synthesis, and tunability of physicochemical properties. Of importance, oxides belonging to the perovskite family, for example, such as ABO<sub>3</sub> simple perovskites and AA'B<sub>2</sub>O<sub>6</sub>/A<sub>2</sub>BB'O<sub>6</sub> double perovskites, A (or A') being an alkaline-earth or rare-earth metal and B (or B') a transition metal, have been demonstrated with promise as the alkaline HER catalysts.<sup>13,14</sup> For instance, one seminal work in this area reported that simple perovskite Pr0.5(Ba0.5Sr0.5)0.5Co0.8Fe0.2O<sub>3-δ</sub> as an electrocatalyst for the HER in a 1 M KOH solution required a 237-mV overpotential to produce a geometric current density of 10 mA cm<sup>-2</sup><sub>geo</sub> ( $\eta_{10}$ , a generic metric for comparing catalytic activity),<sup>15</sup> comparing favorably to several other Co-based catalysts, such as metallic cobalt embedded in Nrich carbon nanotubes,<sup>16</sup> cobalt phosphide supported on carbon cloth,<sup>17</sup> and cobalt– cobalt oxide hybridized with N-doped carbon,<sup>18</sup> Taking advantage of the versatility of perovskite oxides in terms of chemical composition and structure, researchers have conducted a great number of investigations to further increase the HER performance of perovskite catalysts.<sup>19-26</sup> For example, Guan and coworkers screened more than ten Co-based perovskites and concluded that the A-site ionic electronegativity (AIE) can be utilized as a viable descriptor for predicting their HER activity, based on which the
double perovskite (Gd<sub>0.5</sub>La<sub>0.5</sub>)BaCo<sub>2</sub>O<sub>5.5+ $\delta$ </sub> having a suitable AIE value of about 2.33 was found to show optimum HER performance with a  $\eta_{10}$  of as low as 185 mV.<sup>25,26</sup>

However, most of the research to date is focused on perovskite oxides containing Co as the major active component, whereas less attention is given to those consisting mainly of Ni,<sup>27</sup> Mn,<sup>28</sup> and Fe.<sup>29</sup> The previous Chapter concerns the use of a Mo-based perovskite as the alkaline HER catalyst. In this Chapter, research attention is directed to a series of perovskite oxides that comprise solely Fe metal in the B-site as potential catalysts for the alkaline HER. The pristine lanthanum ferrite (LaFeO<sub>3</sub>) was selected as the target perovskite host, into which alkaline-earth metals barium (Ba) and strontium (Sr) were dual-doped to replace the A-site La, yielding a continuous solid solution of  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  (x = 0.0, 0.2, 0.5, 0.8, and 1.0; denoted as LFO, LBSF082, LBSF055, LBSF028, and BSF0, respectively). Upon the inclusion of Ba/Sr, the iron-based perovskites experienced a phase transition from orthorhombic to cubic, along with changes in electronic structures including increased Fe valence and enhanced Fe–O covalency, which are correlated with a significant improvement in the HER electroactivity. The best-performing sample LBSFO28 needs a  $\eta_{10}$  value of approximately 300 mV, which surpasses or is on par with many of the reported perovskite electrocatalysts, suggesting its promise as alternative HER catalysts in alkaline solutions.

## 5.3 Results and discussion

### 5.3.1 Formation and characterizations of Fe-based perovskites

The Ba/Sr-substituted La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> perovskites were prepared by a sol–gel process. As alkaline-earth metal-containing perovskites would generally require temperatures of around 1000 °C for phase formation, all the samples in this work are calcined at the temperature of 1100 °C to ensure good phase purity. The product changes color from yellow to dark/black, which provides visual support for the successful incorporation of Ba/Sr into the perovskite lattice. **Figure 5.1a** depicts the X-ray diffraction (XRD) profiles of the La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> series with various doping contents. Well-defined, high-intensity diffraction peaks were observed for all the samples, indicating their high phase purity. The pristine LFO sample exhibited diffraction peaks typical of an orthorhombic structure (space group: *Pnma*), in accord with the standard pattern of ICDD PDF No. 01-088-0641.<sup>30</sup> Once a small proportion of Ba/Sr are doped into the system (*x* = 0.2), the structure evolves into a cubic structure

(space group:  $Pm\overline{3}m$ ), which remains unchanged with further increasing the doping level to x = 1.0. The variation in the phase structure is more obviously evidenced by the absence of the diffraction peak at  $2\theta$  angle of about  $34.2^{\circ}$ , as seen in **Figure 5.1b**. With the increasing number of Ba/Sr dopants for all the doped samples, the main peak at about  $32.3^{\circ}$  first shifted to a higher angle and then to a lower angle, indicating first a lattice shrinkage and then a lattice expansion. This could be explained considering the operation of two major effects: i) substitution of Ba<sup>2+</sup>/Sr<sup>2+</sup> with a larger ionic radius for La<sup>3+</sup> with a smaller ionic radius (1.61/1.44 Å vs. 1.36 Å) leads to expansion of lattice, and thus a shift to lower  $2\theta$  angles; ii) to maintain charge neutrality, increase of the Fe oxidation state (which has a reduced size, i.e., ionic radius of 0.645 Å and 0.585 Å for Fe<sup>3+</sup> and Fe<sup>4+</sup>) leads to shrinkage of lattice, and thus a shift to higher  $2\theta$ angles.<sup>31</sup> A more quantitative analysis regarding the phase structure and lattice parameters was conducted by Rietveld refinement, and the detailed results shown in **Figure 5.2** and **Table 5.1** consist with the discussion made here.



**Figure 5.1** XRD and Raman data of  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  (x = 0.0, 0.2, 0.5, 0.8, and 1.0). (a) XRD data presented in a broad  $2\theta$  range of  $20-80^\circ$ . (b) XRD data presented in a select  $2\theta$  range of  $30-35^\circ$ . (c) Raman data presented in a wavenumber range of  $200-1000 \text{ cm}^{-1}$ .



**Figure 5.2** Rietveld refinement results for the XRD data of  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}(x = 0.0, 0.2, 0.5, 0.8, and 1.0).$  (a) LFO. (b) LBSFO82. (c) LBSFO55. (d) LBSFO28. (e) BSFO.

Perovskite	Space group	Lattice parameter (Å)	$\chi^2$	Rp	$R_{ m wp}$
				(%)	(%)
LFO	Pnma	a = 5.5002, b = 7.8548,	1 877	2.99	3.98
		c = 5.5548	11077	2.99	5.70
LBSF082	$Pm\overline{3}m$	<i>a</i> = 3.9253	2.514	3.16	4.49
LBSF055	$Pm\overline{3}m$	<i>a</i> = 3.9119	2.628	3.08	4.38
LBSFO28	$Pm\overline{3}m$	<i>a</i> = 3.9158	1.945	2.73	3.65
BSFO	$Pm\overline{3}m$	a = 3.9258	1.795	2.59	3.42

**Table 5.1** Rietveld refinement of the XRD data of  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  (x = 0.0, 0.2, 0.5, 0.8, and 1.0), showing results of crystal symmetries, lattice parameters, and reliability factors.

The phase transition of the samples after Ba/Sr substitution was also ascertained by Raman spectroscopy, a powerful tool for differentiating structural phases of perovskite oxides because different crystal symmetries will generally exhibit different Raman bands.<sup>32</sup> **Figure 5.1c** shows the Raman spectra in a wavenumber window of 200–1000 cm<sup>-1</sup> recorded at room temperature. The pristine LFO displays Raman bands at wavenumbers of ~270, ~430, and ~630 cm<sup>-1</sup>, which, consistent with those reported earlier,<sup>33</sup> is characteristic of the orthorhombic phase. In comparison, all the substituted samples exhibit no Raman-active bands, indicative of the presence of the cubic perovskite structure.<sup>34</sup>

The crystalline information of the cubic structure upon Ba/Sr doping was further provided by transmission electron microscopy (TEM) analysis, as exemplified by the LBSFO28 sample. Figure 5.3a and c show the high-resolution TEM (HRTEM) images taken in the zone axes of [100] and [111], respectively. Lattice fringes with interplanar distances of 0.39 and 0.28 nm were clearly detected, corresponding to the (010) and ( $\overline{110}$ ) planes of the cubic-structured perovskite. The selected-area electron diffraction (SAED) patterns associated with these HRTEM images, as illustrated in Figure 5.3b and d, further support the formation of a cubic structure with the  $Pm\overline{3}m$ 

space group. High-angle annular dark-field scanning TEM (HAADF-STEM) and energy-dispersive X-ray spectroscopy (EDS) mapping were conducted to prove the presence of the Ba and Sr dopants in the perovskite lattice. As shown in **Figure 5.3e**, a quite homogeneous distribution of all the constituent elements can be found, demonstrating the successful construction of a multi-element, perovskite-type solid solution.



**Figure 5.3** TEM characterization of the LBSFO28 sample. (a–b) HRTEM image and the associated SAED pattern in the [100] zone axis. (c–d) HRTEM image and the associated SAED pattern in the [111] zone axis. (e) HAADF-STEM image and the corresponding EDS mapping images of La, Ba, Sr, Fe, and O elements.

The morphology of the La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> samples with various Ba/Sr doping contents was studied by scanning electron microscopy (SEM). All the samples possess similar morphological features, consisting of large particles in the size range from a few hundred nanometers to several micrometers (**Figure 5.4**). Due to the high calcination temperature used for phase formation (i.e., 1100 °C), the La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> samples appear to be rather sintered with no presence of any pore structure. Of note, the particle size of the La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> series becomes larger with the increasing amount of the alkaline-earth metal dopants, which is also verified by the decreasing trend of the Brunauer–Emmett–Teller (BET) surface areas (**Table 5.2**), as measured from nitrogen sorption measurements.



**Figure 5.4** SEM images of  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  (*x* = 0.0, 0.2, 0.5, 0.8, and 1.0).

Perovskite	Surface areas $(m^2 g^{-1})$
LFO	4.15
LBSFO82	2.97
LBSF055	2.01
LBSFO28	1.25
BSFO	1.13

**Table 5.2** BET surface areas of  $La_{1-x}(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  (x = 0.0, 0.2, 0.5, 0.8, and 1.0).

## 5.3.2 Electrocatalytic hydrogen evolution performance

The use of Fe-based La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> perovskites as the HER electrocatalysts was evaluated at ambient conditions in an electrolyte of 1 M KOH aqueous solution. Figure 5.5a displays the apparent catalytic activity acquired from linear sweep voltammetry (LSV) collected at a slow scan rate of 5 mV s<sup>-1</sup>, where the *iR*-corrected potential vs. the reversible hydrogen electrode (RHE) is plotted against the current normalized by the geometric area of the working electrode. It is found that upon the co-doping of  $Ba^{2+}$  and  $Sr^{2+}$  cations, the apparent activity showed a significant increase, as evidenced by a positive shift in the potential needed to reach a certain current output. More specifically, to afford an electrode activity of  $-10 \text{ mA cm}_{geo}^{-2}$ , the LFO parent oxide requires a  $\eta_{10}$  value as large as 519 mV, whereas the doped samples require reduced values of 471, 394, 303, and 355 mV for LBSF082, LBSF055, LBSF028, and BSFO, respectively (Figure 5.5b). Remarkably, LBSFO28 was found to be the most active toward the HER, with a drastic drop in  $\eta_{10}$  by 216 mV. Using the same metric, LBSFO28 was found to outperform previously reported Ni-, Mn-, and Febased perovskite-type HER electrocatalysts such as La<sub>0.8</sub>Sr<sub>0.2</sub>Cr<sub>0.69</sub>Ni<sub>0.31</sub>O<sub>3- $\delta$ </sub> ( $\eta_{10}$  = 447 mV),<sup>27</sup> NdBaMn<sub>2</sub>O<sub>5.5+ $\delta$ </sub> ( $\eta_{10} \approx 500$  mV),<sup>28</sup> and LaFe<sub>0.8</sub>Co<sub>0.2</sub>O<sub>3- $\delta$ </sub> ( $\eta_{10} \approx 400$  mV).<sup>29</sup> More importantly, LBSFO28 compares favorably to many of the Co-based perovskite catalysts, including SrCoO<sub>3- $\delta$ </sub> ( $\eta_{10} = 447 \text{ mV}$ ),<sup>23</sup> La<sub>0.5</sub>Sr<sub>0.5</sub>CoO<sub>3- $\delta$ </sub> ( $\eta_{10} \approx 420 \text{ mV}$ ),<sup>22</sup> PrBa<sub>0.5</sub>Sr<sub>0.5</sub>Co<sub>2</sub>O<sub>5+ $\delta$ </sub> ( $\eta_{10} = 393 \text{ mV}$ ),<sup>20</sup> SrCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ </sub> ( $\eta_{10} = 378 \text{ mV}$ ),<sup>24</sup> Ba0.95Co0.4Fe0.4Zr0.1Y0.1O<sub>3- $\delta$ </sub> ( $\eta_{10} = 360 \text{ mV}$ ),<sup>21</sup> and Ba0.5Sr0.5Co0.8Fe0.2O<sub>3- $\delta$ </sub> ( $\eta_{10} = 342$ ) mV).<sup>15</sup> While there is still a gap when compared to the state-of-the-art Co-based perovskites, for instance,  $Pr_{0.5}(Ba_{0.5}Sr_{0.5})_{0.5}Co_{0.8}Fe_{0.2}O_{3-\delta}$  ( $\eta_{10} = 237$  mV) and  $(Gd_{0.5}La_{0.5})BaCo_2O_{5.5+\delta}$  ( $\eta_{10} = 185 \text{ mV}$ ), these comparisons suggest that the Fe-based LBSFO28 catalyst has the potential for alkaline water splitting, especially when one further considers its lower cost relative to the Co-based counterpart.



**Figure 5.5** Electrocatalytic performance of La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> (x = 0.0, 0.2, 0.5, 0.8, and 1.0) toward the hydrogen evolution reaction in a 1 M KOH electrolyte. (a) LSV curves where the current is normalized by the geometric area of the working electrode (in mA cm<sup>-2</sup><sub>geo</sub>). The arrow indicates a decreasing trend in the potential required to deliver a current density of  $-10 \text{ mA cm}_{geo}^{-2}$ . (b) A comparison of the overpotential required to deliver  $-10 \text{ mA cm}_{geo}^{-2}$ . (c) LSV curves where the current is normalized by the BET surface area of the perovskite catalysts (in mA cm<sup>-2</sup><sub>oxide</sub>). The arrow indicates a decreasing trend to deliver  $-5 \text{ mA cm}_{oxide}^{-2}$ . (d) A comparison of the overpotential needed to deliver  $-5 \text{ mA cm}_{oxide}^{-2}$ .

Taking into consideration of the surface area effect, **Figure 5.5c** reports the specific activity of the various Fe-based perovskites as a parameter for comparing their intrinsic activity.<sup>26</sup> Interestingly, the trend for the intrinsic activity follows the same as that for the apparent activity. As shown in **Figure 5.5d**, the LBSFO28 sample remains to be the most intrinsically active, requiring a lowest overpotential of 326 mV to afford a

specific activity of  $-5 \text{ mA cm}_{\text{oxide}}^{-2}$ , lower than that of LBSFO82 (551 mV), LBSFO55 (433 mV), and BSFO (374 mV) and much smaller than that of the pristine LFO (608 mV).

It is noted that a minor cathodic peak was found at a potential preceding the HER, around -0.2 V vs. RHE, especially for the samples LBSFO28 and BSFO. This could be related to some certain electrochemical phenomena inherent to these Fe-based perovskite oxides, similar to that found on the Pr<sub>0.5</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>0.5</sub>Co<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3- $\delta$ </sub> perovskite in which Fe is a minor constituent.<sup>15</sup> Detailed understanding of this electrochemical process is out of the scope of this study.

**Figure 5.6** plots the logarithm of specific activity against the overpotential, from which Tafel slopes can be derived. As can be seen, the LFO parent oxide exhibits a Tafel slope of 137 mV dec<sup>-1</sup>, while all the Ba/Sr doped samples exhibit a somewhat reduced Tafel slope, implying faster reaction kinetics. Again, the most active sample LBSFO28 has the smallest Tafel slope (i.e., 112 mV dec<sup>-1</sup>). Nonetheless, all the samples, regardless of doping, show a Tafel slope value close to 120 mV dec<sup>-1</sup>, which, according to previous research,<sup>35</sup> suggests that a Volmer–Heyrovsky reaction mechanism may be operative during the alkaline HER and that the reaction rate may be determined by the Volmer process. In the Volmer process water molecule is dissociated and electrochemically reduced to form the hydrogen atoms adsorbed on the catalyst surface, as can be described by the equation of  $M + H_2O + e^- \leftrightarrow M-H + OH^-$ , where M denotes a catalytically active surface site.<sup>36</sup>



**Figure 5.6** Tafel plots of  $La_{1-x}(Ba_{0.5}Sr_{0.5})_x FeO_{3-\delta}$  (*x* = 0.0, 0.2, 0.5, 0.8, and 1.0).

## 5.3.3 Electronic origins for the activity enhancement

As the electrocatalytic performance is strongly correlated with the catalyst's electronic structures, a combined investigation of X-ray photoelectron spectroscopy (XPS) and soft X-ray absorption spectroscopy (XAS) was carried out to offer insights into the electronic origins for the enhancement of catalytic activity. **Figure 5.7a** displays the high-resolution XPS spectra of the Fe 2p core levels for the various Fe-based perovskite samples. A doublet at the binding energy of about 710.1 eV for  $2p_{3/2}$  and about 723.8 eV for  $2p_{1/2}$  was found for LFO, which, together with a shake-up contribution at about 718.4 eV, consists with reported Fe 2p features and suggests the dominant presence of trivalent Fe cations.<sup>37</sup> Interestingly, a gradual shift to higher binding energies was observed for samples with an increasing Ba/Sr dopant concentration, as indicated by a dotted line in **Figure 5.7a**. This observation suggests that partial oxidation from Fe<sup>3+</sup> to Fe<sup>4+</sup> occurred for all the doped samples<sup>38</sup> and that the extent of such oxidation strongly correlates with the doping level, that is, the higher the doping level, the greater the oxidation extent.



Figure 5.7 Electronic states of La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> (x = 0.0, 0.2, 0.5, 0.8, and 1.0) as characterized by XPS and XAS. (a) Fe 2p XPS spectra. (b) O *K*-edge XAS spectra.

While the Fe 2p XPS result provides Fe<sup>3+</sup>-to-Fe<sup>4+</sup> oxidation information mainly of the catalyst surface, the O K-edge soft XAS data taken in the fluorescence yield mode, which are highly sensitive to the transition metal valence as well as transition metaloxygen covalency,<sup>39,40</sup> further reveals the Fe valence changes in the bulk of the materials. As shown in Figure 5.7b, once  $Ba^{2+}$  and  $Sr^{2+}$  were incorporated into the LFO lattice, a pre-edge peak at the photon energy of about 528 eV appears, which continuously gains spectral weight and becomes dominant for high Ba/Sr concentrations. According to earlier publications,<sup>25</sup> this pre-edge peak is associated with the covalent mixing between transition metal 3d orbitals and O 2p states. Accompanying this evolution of the pre-edge peak is the suppression of the original pair of peaks sitting at the higher energy side, which merge completely into a shoulder peak for high Ba/Sr contents. These features are consistent with those found in the previously reported Sr single-doped La<sub>1-x</sub>Sr<sub>x</sub>FeO<sub>3- $\delta$ </sub> series,<sup>41,42</sup> and are indicative of an increased overlap between the Fe 3d and O 2p states (i.e., enhanced Fe 3d-O 2p covalency) with the increasing doping of Ba/Sr, which is also correlated with the bulk oxidation of  $Fe^{3+}$  to  $Fe^{4+}$ .

The XPS and soft XAS investigations indicate that upon the inclusion of the Ba/Sr dopants, the oxidation state of the Fe cation increased steadily in the La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta$ </sub> series and the Fe–O covalency enhanced concomitantly. However, the HER reactivity of the series did not increase monotonically. Instead, the best performance was achieved on LBSFO28 with a doping level of x = 0.8. This suggests that the HER performance of the Fe-based samples is optimized at a suitable Fe valence and Fe–O covalency (i.e., neither too high nor too low), which may lead to an appropriate binding state for the reaction intermediates and can thus result in an optimum activity, in line with the Sabatier's principle.<sup>43</sup> Note that a similar conclusion was also drawn for the research on a series of Co-based perovskites with different A-site compositions, in which the most active perovskite (Gd<sub>0.5</sub>La<sub>0.5</sub>)BaCo<sub>2</sub>O<sub>5.5+ $\delta$ </sub> with a suitable AIE value of about 2.33 also exhibited a moderate Co valence and Co–O covalency.<sup>26</sup>

## **5.4 Conclusions**

To summarize, a series of Fe-based La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3- $\delta}$  (x = 0.0, 0.2, 0.5, 0.8, and 1.0) perovskites were obtained by simultaneously doping alkaline-earth metals Ba and Sr into the A-site of LaFeO<sub>3</sub> and evaluated as the electroactive materials for catalyzing the hydrogen evolution under alkaline solutions. The replacement of La by Ba/Sr in LaFeO<sub>3</sub> leads to a phase transition from orthorhombic to cubic, along with electronic structure changes including partial oxidation of Fe valence from 3+ to 4+ as well as enhanced covalency between the Fe and O states, as revealed by a comprehensive X-ray spectroscopic study. Such changes in electronic structures contributed to increased HER kinetics, and the La<sub>0.2</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>0.8</sub>FeO<sub>3- $\delta$ </sub> (LBSFO28) sample with a suitable Fe valence and Fe–O covalency was found to exhibit an optimum HER reactivity, requiring overpotentials of 303 and 326 mV to give a current density of  $-10 \text{ mA cm}_{geo}^{-2}$  and a specific activity of  $-5 \text{ mA cm}_{oxide}^{-2}$ , respectively. These results are expected to offer insights into the future development of cost-effective and efficient electrocatalytic materials for the alkaline HER.</sub>

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# Chapter 6 An unusually stabilized Co-based perovskite for highly efficient oxygen evolution

# 6.1 Abstract

While electrochemical water splitting provides a green route to produce H<sub>2</sub> fuel, its efficiency is largely limited due to the intrinsically slow kinetics of the oxygen evolution reaction (OER) at the anode. Co-based perovskite oxides have been demonstrated excellent electrocatalytic activity toward the OER in an alkaline solution, yet not all of them show sufficient activity. In this work, a novel method based on thermal reduction in an inert atmosphere was applied to convert a hexagonal-structured perovskite (BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ 1</sub>, denoted as *h*-BCF) with poor OER activity into a cubic-structured perovskite (BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ 2</sub>, denoted as *c*-BCF) with highly efficient OER kinetics. This unusually stabilized *c*-BCF perovskite offers a significantly reduced Co valence as well as a greatly enhanced oxygen vacancy concentration, which leads to a twenty times higher intrinsic activity relative to the pristine *h*-BCF. The intrinsic activity of *c*-BCF also surpasses that of the state-of-the-art perovskites and noble metal-based standards. This work indicates that phase transformation can be utilized as an effective means to develop new and efficient OER electrocatalysts.

# 6.2 Introduction

While fossil fuels continue to be the major energy sources in our daily life, their impact on the environment cannot be neglected. To address environmental issues such as the global warming, humanity needs to develop cleaner energy sources to sustainably power our planet Earth. In this regard, hydrogen (H<sub>2</sub>) has long been recognized as an alternative energy carrier with some highly desirable properties for use in the sustainable energy sectors.<sup>1</sup> For instance, H<sub>2</sub> possesses a mass-based energy content higher than any other fuels, i.e., nearly thrice that of gasoline  $(120 \text{ vs. } 44 \text{ MJ kg}^{-1})$ .<sup>2</sup> In the meantime, the consumption of H<sub>2</sub> in an internal combustion engine or a fuel cell generates water as the only product, which significantly reduces carbon emissions. Among various means of hydrogen production, the electrochemical water splitting  $(H_2O \rightarrow 1/2O_2 + H_2)$ , also known as water electrolysis, has received growing interest nowadays owing to the large quantity of water resources on Earth, the simplicity of practical operation, and the high quality of the H<sub>2</sub> product.<sup>3</sup> Despite its high viability, the efficiency of the electrolysis of water is largely impeded by the sluggish kinetics of the electrode reactions, in particular, the oxygen evolution reaction (OER) on the anode side. Associated with the complexity of the four-electron oxidation process, this OER reaction requires a considerable overpotential to occur at moderate rates, leading to a large energy loss.<sup>4</sup> To overcome this energy barrier, electrocatalysts comprising precious metals like ruthenium (Ru) and iridium (Ir) are widely used,<sup>5</sup> which show one of the best catalytic performances. Unfortunately, the scarcity and expensiveness of these catalysts have greatly hindered their industrial-scale use. Therefore, the development of cost-effective and highly efficient alternatives has been a very popular research topic central to the realization of the water splitting technology.

Over the recent years, transition metal-based (e.g., Co, Fe, Ni) materials have been extensively studied for electrocatalyzing the OER in an alkaline solution  $(4OH^- \rightarrow O_2 + 2H_2O + 4e^-)$ , including metal or metal alloys,<sup>6</sup> oxides and (oxy)hydroxides,<sup>7,8</sup> and non-oxides such as nitrides,<sup>9</sup> sulfides,<sup>10</sup> and phosphides.<sup>11</sup> Among these candidates, oxide compounds featuring an ABO<sub>3</sub> perovskite structure have received tremendous research attention due to their cost-effectiveness and high reactivity.<sup>12,13</sup> For example, Ba<sub>0.5</sub>Sr<sub>0.5</sub>Co<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3- $\delta$ </sub> (BSCF, here  $\delta$  denotes oxygen vacancy) was demonstrated with a high intrinsic activity surpassing that of iridium dioxide (IrO<sub>2</sub>) by more than two orders of magnitude.<sup>14</sup> The high activity is correlated with the electronic state of the active Co cation having an  $e_g$  occupancy close to unity (Co valence: ~2.8;  $e_g$  occupancy: ~1.2), which can lead to an optimum binding state between the oxygen intermediates and the surface active sites.<sup>14</sup> This  $e_g$  parameter has led to the discovery of several other Co-based perovskites with superior catalytic activity, for example, SrNb<sub>0.1</sub>Co<sub>0.7</sub>Fe<sub>0.2</sub>O<sub>3- $\delta$ </sub>,<sup>15</sup> BaCo<sub>0.7</sub>Fe<sub>0.2</sub>Sn<sub>0.1</sub>O<sub>3- $\delta$ </sub> (BCFSn),<sup>16</sup> and SrCo<sub>0.9</sub>Ti<sub>0.1</sub>O<sub>3- $\delta$ </sub>,<sup>17</sup> all having a Co valence in the range of 2.8–3.0, leading to near-unity  $e_g$  occupancy. Later research suggested that lowering the Co valence of BSCF could further contribute to enhanced OER performance.<sup>18,19</sup> Notably, nanosized BSCF prepared from a flame spray method delivered an exceptional OER activity, which was closely related to a significantly reduced Co oxidation state.<sup>20</sup> The ability to stabilize low-valent Co state in the BSCF perovskite is strongly associated with its extraordinary structural flexibility to accommodate a large number of oxygen vacancies, with  $\delta$  ranging from 0.2 to 0.8.<sup>21</sup>

In fact, BSCF can be regarded as a derivative of  $BaCo_{1-x}Fe_xO_{3-\delta}$  (BCF). Due to a considerable size mismatch between the A-site Ba cation and the B-site Co/Fe cations, BCF generally crystalizes in the low-symmetry hexagonal phase at room temperature.<sup>22</sup> The partial replacement of A-site Ba with a smaller-sized Sr dopant represents one means to sustain a simple cubic structure, as seen in the example of BSCF.<sup>14,23</sup> On the other hand, the incorporation of cations having a large size and a high valence at the B-site, as seen in the example of BCFSn,<sup>16,24</sup> represents another strategy to stabilize the cubic structure. While capable of promoting the formation of a cubic perovskite structure, these doping strategies cannot not bring about a sufficiently low Co valence, thus limiting the activity enhancement for BCF-based OER catalysts.

In this work, a novel strategy based on thermal reduction under an inert atmosphere was proposed to convert BCF perovskite from the hexagonal phase to cubic phase. As a proof-of-concept, BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ </sub> with a Co/Fe molar ratio of 7:3 was selected as a representative of the BCF series. Through the introduction of a reductive driving force provided by an inert atmosphere (e.g., nitrogen or argon) at elevated temperatures, hexagonal-structured BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ 1</sup> (denoted as *h*-BCF) successfully transitioned to cubic-structured BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ 2</sup> (denoted as *c*-BCF), following the below equation:</sub></sub>

 $BaCo_{0.7}Fe_{0.3}O_{3-\delta I} \text{ (hexagonal)} \rightarrow BaCo_{0.7}Fe_{0.3}O_{3-\delta 2} \text{ (cubic)} + 1/2(\delta 2 - \delta I)O_2$ (1)

where  $\delta l$  and  $\delta 2$  ( $\delta l < \delta 2$ ) are used to represent the different amounts of oxygen vacancies in these two different structures. The formation of the cubic perovskite structure is likely due to the stabilization of low-valent Co<sup>2+</sup> species which has higher ionic radius relative to Co<sup>3+</sup> and Co<sup>4+,25</sup> Simultaneously, the phase transition led to a greatly increased oxygen vacancy concentration, which, along with the considerably reduced Co valence, contributed to a remarkable enhancement in OER reactivity. When evaluated for the OER electrocatalysis in a 0.1 M KOH electrolyte, the cubic-structured *c*-BCF was found to show an intrinsic activity that is about 20-fold higher than the hexagonal structured *h*-BCF. Of significance, *c*-BCF was demonstrated to be one of the most active perovskite-type catalysts reported until now, showing intrinsic activity much better than the state-of-the-art perovskites such as BSCF and BCFSn as well as the noble metal standards IrO<sub>2</sub> and RuO<sub>2</sub>. These results highlight the potential of the unusually stabilized, cubic-phase *c*-BCF perovskite for accelerating the electrocatalytic oxygen evolution.

# 6.3 Results and discussion

## 6.3.1 Stabilization of the cubic-structured *c*-BCF

The pristine hexagonal BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta l$ </sub> oxide (*h*-BCF) was crystallized after calcination of a sol–gel made precursor at 1000 °C in air. To probe any potential phase change of *h*-BCF, in situ X-ray diffraction (XRD) was performed under an air atmosphere at temperatures ranging from room temperature to 900 °C. As displayed in **Figure 6.1a**, the XRD patterns exhibit identical peak features within the temperature window studied, indicating the high thermal stability of *h*-BCF. The diffraction peaks gradually shifted to smaller 2 $\theta$  angels upon heating and then shifted back to the original 2 $\theta$  angels upon cooling (**Figure 6.1b**), implying lattice expansion and shrinkage induced mainly by the thermal reduction. These results suggest that under the air atmosphere the pristine *h*-BCF is rather stable and undergoes no obvious phase transition at temperatures up to 900 °C. Note that phase structure at temperatures higher than 900 °C was not investigated due to the temperature limit of the XRD instrument.



**Figure 6.1** In situ XRD profiles of *h*-BCF. (a) XRD profiles presented in a broad  $2\theta$  range of 10–80°. (b) XRD data presented in a select  $2\theta$  range of 28–33°.

A more reductive condition, i.e., a N<sub>2</sub> atmosphere, was then employed to realize the phase transformation from *h*-BCF to the cubic-structured BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta 2$ </sub> (*c*-BCF). As depicted in **Figure 6.2a**, the pristine *h*-BCF possessed an XRD profile typical of the hexagonal structure as reported earlier.<sup>26</sup> After thermal reduction in N<sub>2</sub> at 900 °C, the structure completely evolved into a new one whose XRD peaks are characteristic of the ideal cubic structure (space group:  $Pm\overline{3}m$ ).<sup>16</sup> This phase change was also verified by Raman spectra recorded at room temperature. As illustrated in Figure 6.2b, the pristine *h*-BCF displays several Raman bands at wavenumbers of  $\sim$ 320,  $\sim$ 400,  $\sim$ 600, and  $\sim 690 \text{ cm}^{-1}$ . In general, these Raman shifts are consistent with those reported for the hexagonal phase,<sup>27</sup> although the peak intensities may appear different, which is likely caused by the inhomogeneity of the *h*-BCF sample in the laser spot area during Raman testing. By comparison, c-BCF exhibits a featureless Raman spectrum, which, according to literature,<sup>28</sup> is associated with the presence of the ideal cubic structure as perovskites with such structure do not present any Raman active modes. The combined XRD and Raman characterizations reveal that with calcination at 900 °C under the N2 atmosphere, the hexagonal-structured BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta$ 1</sub> successfully transitioned into the cubic-structured BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3- $\delta 2$ </sub>. The phase transition is most likely facilitated by the effect of a much lower oxygen partial pressure, as enabled by a more reductive atmosphere (i.e., N<sub>2</sub> versus air), providing a driving force strong enough for the transition to occur.



**Figure 6.2** XRD profiles and Raman spectra of *h*-BCF and *c*-BCF. (a) XRD profiles presented in a  $2\theta$  range of 10–80°. (b) Raman spectra presented in a wavenumber range of 200–1000 cm<sup>-1</sup>.

further investigate the phase transformation of h-BCF, a combined То thermogravimetric and differential scanning calorimetry analysis (TG-DSC) was conducted under an argon (Ar) atmosphere, with the results presented in Figure 6.3a. A progressive weight loss was observed after the temperature reached 400 °C until a more drastic weight loss took place at about 800 °C. Concomitant with this drastic weight loss is an endothermic peak appearing at the temperature of about 825 °C, which can be ascribed to the phase transformation from hexagonal to cubic.<sup>29</sup> The sample weight became unchanged after the settling period at 900 °C, leading to a total weight loss of 2.28 wt%. The phase transition process of h-BCF was also examined by oxygen temperature-programmed desorption (O2-TPD) experiment conducted in an Ar atmosphere. As shown in Figure 6.3b, a broad peak that initiated at about 550 °C and peaked at about 740 °C is assignable to the reduction of tetravalent Co<sup>4+</sup>/Fe<sup>4+</sup> to trivalent Co<sup>3+</sup>/Fe<sup>3+</sup>, and another sharp peak at about 865 °C is related to the further reduction of trivalent Co<sup>3+</sup> to divalent Co<sup>2+</sup>.<sup>24</sup> Note that the overall result of O<sub>2</sub>-TPD accords with that of TG-DSC, while the minor inconsistency in temperatures is likely due to the variations in the sample mass and sample form used in the two different analysis instruments (about 30 mg of powder in TG-DSC and about 0.15 g of 150mesh granule in O<sub>2</sub>-TPD).



**Figure 6.3** TG-DSC and O<sub>2</sub>-TPD profiles of *h*-BCF. (a) TG-DSC profile. (b) O<sub>2</sub>-TPD profile.

The *h*-BCF sample after the O<sub>2</sub>-TPD experiment in Ar atmosphere was further subjected to XRD analysis. As shown in **Figure 6.4**, XRD diffraction peaks identical to those of the *c*-BCF sample obtained in N<sub>2</sub> atmosphere were observed, suggesting the reproducibility of the phase transition in two different inert atmospheres. The above experiments indicate that the stabilization of the cubic structure of *c*-BCF is likely due to the generation of  $Co^{2+}$  species which has higher ionic radius than  $Co^{3+}/Co^{4+}$ .<sup>25</sup> Additional experimental trials on another hexagonal perovskite with a similar composition, namely BaCo<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3- $\delta$ </sub> (BCF82), did not give rise to the stabilization of a pure cubic phase, as revealed in **Figure 6.5**. This suggests that the hexagonal to cubic phase transition could also be dependent on the relevant content of the constituent metals.



**Figure 6.4** XRD profiles of *c*-BCF obtained by reducing *h*-BCF in  $N_2$  (during synthesis) and in Ar (during O<sub>2</sub>-TPD experiment).



Figure 6.5 XRD profiles of the pristine  $BaCo_{0.8}Fe_{0.2}O_{3-\delta}$  (BCF82) sample, BCF82 after reduction in N<sub>2</sub> (during synthesis), and BCF82 after reduction in Ar (during O<sub>2</sub>-TPD experiment).



**6.3.2 Electrocatalytic oxygen evolution performance** 

Figure 6.6 Electrocatalytic performance of *h*-BCF and *c*-BCF toward the oxygen evolution reaction in a 0.1 M KOH electrolyte. (a) OER kinetic currents. The arrow shows a decreasing trend in the potential required to produce a current density of 10 mA  $cm_{geo}^{-2}$ . (b) Tafel plot where the OER currents are normalized by the catalyst surface areas to obtain the specific activity. The arrow shows an increasing trend in the specific activity at an overpotential of 300 mV. (c) Comparisons of the overpotential at a current density of 10 mA  $cm_{geo}^{-2}$  and the specific activity at an (d) of 300 mV. Electrochemical overpotential stability recorded by chronopotentiometry tests at a steady current density of 5 mA  $cm_{geo}^{-2}$ . The arrows indicate the detachment of O<sub>2</sub> bubbles generated on the electrode surface.

The electrocatalytic OER performance was measured at room temperature in an  $O_2$ -saturated 0.1 M KOH electrolyte. Both the pristine *h*-BCF and the reduced *c*-BCF were loaded on a glassy carbon rotating disk electrode to act as the working electrode. **Figure 6.6a** shows the OER kinetic currents based on the geometric area of the working electrode, which were obtained by averaging and *iR*-correcting the as-

recorded cyclic voltammograms to eliminate distractions from the capacitive current and the electrolyte resistance, respectively.<sup>14,30</sup> As is obvious, the OER on the reduced *c*-BCF sample initiated at a much earlier potential than the pristine *h*-BCF did, indicating significantly improved OER activity after the phase transition. More specifically, *c*-BCF produced a current density of 10 mA cm<sup>-2</sup><sub>geo</sub> at an overpotential of 379 mV ( $\eta_{10} = 379$  mV, here  $\eta_{10}$  is a solar-fuel synthesis related parameter used for comparing OER activity),<sup>31</sup> which is approximately 90 mV smaller compared to *h*-BCF ( $\eta_{10} = 467$  mV). These reductions in (over)potentials are indicative of a boost in the geometric electrode activity (also known as the apparent activity) induced by the phase transformation.

To rule out the contribution of the catalyst surface area to the observed electrode activity, the OER kinetic currents were then normalized by the Brunauer-Emmett-Teller (BET) surface area estimated using N<sub>2</sub> sorption measurements (0.62 and 0.38  $m^2 g^{-1}$  for *h*-BCF and *c*-BCF, respectively), which yielded specific activity as a metric for comparing the intrinsic activity.<sup>14,32</sup> Figure 6.6b plots the logarithm of specific activity as a function of the potential. It was found that c-BCF consistently outperformed *h*-BCF in terms of the specific activity within the entire potential window of 1.52-1.58 V vs. the reversible hydrogen electrode (RHE). For example, at an overpotential of 300 mV, c-BCF delivered a specific activity approximately twenty times that of *h*-BCF (1.30 vs. 0.064 mA  $\text{cm}_{\text{oxide}}^{-2}$ ), implying that enhancement in the OER intrinsic activity was also observed after the phase transition. The data in Figure 6.6b were further fitted to obtain the Tafel slope. *c*-BCF exhibited a Tafel slope value that is somewhat higher than that of *h*-BCF (80 vs. 60 mV dec<sup>-1</sup>), which might suggest an alteration in the OER reaction mechanism. Figure 6.6c illustrates the comparisons regarding the discussion made in Figure 6.6a and b, further highlighting the improved OER reactivity resulting from the phase transformation. A comparison was also made with the state-of-the-art perovskite OER catalysts in terms of the specific activity at a 300-mV overpotential, as tabulated in Table 6.1. Remarkably, the c-BCF sample showed a higher intrinsic activity than several other BCF-based perovskites, for example BSCF (~0.53 mA  $\rm cm_{oxide}^{-2}$  )  $^{14}$  and BCFSn (~0.14 mA  $\rm cm_{oxide}^{-2}$  ),  $^{16}$ demonstrating the high efficacy of the unusually stabilized c-BCF perovskite in catalyzing the OER. Of importance, c-BCF was found to exhibit one of the best performances reported to date, surpassing that of single perovskite Cs<sub>0.4</sub>La<sub>0.6</sub>Mn<sub>0.25</sub>Co<sub>0.75</sub>O<sub>3</sub> (~0.79 mA cm<sup>-2</sup><sub>oxide</sub>),<sup>33</sup> double perovskite PrBaCo<sub>2</sub>O<sub>5+ $\delta$ </sub> (~0.74 mA cm<sup>-2</sup><sub>oxide</sub>),<sup>34</sup> Ruddlesden–Popper perovskite La<sub>0.5</sub>Sr<sub>1.5</sub>Ni<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>4+ $\delta$ </sub> (~0.76 mA cm<sup>-2</sup><sub>oxide</sub>),<sup>35</sup> and quadruple perovskite CaCu<sub>3</sub>Fe<sub>4</sub>O<sub>12</sub> (~0.17 mA cm<sup>-2</sup><sub>oxide</sub>).<sup>36</sup> More importantly, *c*-BCF displayed an intrinsic activity almost two orders of magnitude higher than the noble metal-based benchmarking catalysts, IrO<sub>2</sub> (~0.015 mA cm<sup>-2</sup><sub>oxide</sub>) and RuO<sub>2</sub> (~0.011 mA cm<sup>-2</sup><sub>oxide</sub>).<sup>37</sup> These comparisons underscore the good OER activity of the cubic-structured *c*-BCF sample.

Catalyst	Loading (mg cm <sup>-2</sup> )	Catalyst/carbon mass ratio	Specific activity <sup>a</sup> (mA cm <sup>-2</sup> <sub>oxide</sub> )	Ref.
<i>c</i> -BCF	0.255	5:1	1.30	This work
IrO <sub>2</sub>	0.050	No carbon <sup>b</sup>	~0.015 <sup>c</sup>	37
RuO <sub>2</sub>	0.050	No carbon	~0.011	37
$Ba_{0.5}Sr_{0.5}Co_{0.8}Fe_{0.2}O_{3^{-\delta}}$	0.250	5:1	~0.53	14
$BaCo_{0.7}Fe_{0.2}Sn_{0.1}O_{3^{-\delta}}$	0.232	1:1	~0.14	16
$Cs_{0.4}La_{0.6}Mn_{0.25}Co_{0.75}O$	0.168	No carbon	~0.79	33
$PrBaCo_2O_{5+\delta}$	0.250	5:1	~0.74	34
$La_{0.5}Sr_{1.5}Ni_{0.7}Fe_{0.3}O_{4+\delta}$	0.0153	3:7	~0.76	35
$CaCu_3Fe_4O_{12}$	0.250	5:1	~0.17	36

**Table 6.1** A comparison of the OER activity (in terms of the specific activity at an overpotential of 300 mV) of *c*-BCF with other state-of-the-art perovskite catalysts and noble metal oxides tested on a glassy carbon electrode in 0.1 M KOH.

<sup>*a*</sup> The specific activity was compared at an overpotential of 300 mV (i.e., a potential of 1.529 V vs. RHE).

<sup>b</sup> The catalyst was loaded on the glassy carbon electrode without the addition of conductive carbon.

<sup>c</sup> The activity data in this column were obtained from published results using the software WebPlotDigitizer.<sup>38</sup>

The stability of *h*-BCF and *c*-BCF as the OER electrocatalysts was tested by chronopotentiometry at a steady current density of 5 mA  $cm_{geo}^{-2}$  for 16 h. During these tests, O<sub>2</sub> bubbles were accumulated on the electrode surface due to the continuous oxidation of water, which were then detached under the constant rotation of the electrode, as indicated by the arrows in **Figure 6.6d**. For *h*-BCF, the potential to maintain 5 mA  $cm_{geo}^{-2}$  began to increase after a 10-hour period, indicating relatively poor stability. By contrast, a more stable behavior was observed for the *c*-BCF sample, which required an almost unchanged voltage to sustain 5 mA  $cm_{geo}^{-2}$  after the initial O<sub>2</sub> detachment at about 1 h. These chronopotentiometry tests suggest that aside from activity, *c*-BCF also demonstrated better electrochemical stability than *h*-BCF.

# 6.3.3 Understanding the enhancement in catalytic performance

The OER activity of an electrocatalytic is strongly correlated with its electronic structure. As described by Equation (1), the transition from *h*-BCF to *c*-BCF not only alters the phase structure of the material but also changes the oxygen stoichiometry and the transition metal valence. As reported earlier, the pristine *h*-BCF has an average valence of 3.73 for Co and Fe,<sup>24</sup> from which the oxygen non-stoichiometry is calculated to be  $\delta l = 0.135$  based on charge neutrality. In addition, the phase transition led to a total mass loss of 2.28 wt% (**Figure 6.3a**), which can be used to compute the oxygen non-stoichiometry ( $\delta 2 = 0.478$ ) and accordingly the average transition metal valence (3.04). By assuming that the Fe cation has a valence of 4+ or 3+, the lower and upper limit for the Co valence was also approximated, as presented in **Table 6.2**. Overall, an increase in oxygen vacancy concentration as well as a reduction in the transition metal valence were observed after the phase transition.

Perovskite	Oxygen vacancy, $\delta$	Average metal valence	Co valence $(\text{for Fe}^{4+})^a$	Co valence $(\text{for Fe}^{3+})^a$
BaCo <sub>0.7</sub> Fe <sub>0.3</sub> O <sub>3-δ1</sub> ( <i>h</i> -BCF)	<i>δ1</i> = 0.135	3.73 <sup><i>b</i></sup>	3.61	4.04 <sup><i>c</i></sup>
BaCo <sub>0.7</sub> Fe <sub>0.3</sub> O <sub>3-δ2</sub> ( <i>c</i> -BCF)	$\delta 2 = 0.478$	3.04	2.63	3.06

**Table 6.2** Oxygen vacancy, average metal valence, and Co valence of *h*-BCF and *c*-BCF.

<sup>*a*</sup> Lower and upper limit for the Co valence, as estimated by assuming that Fe is of tetravalent or trivalent, respectively.

<sup>b</sup> Data reported earlier, as obtained from chemical titration.<sup>24</sup>

<sup>c</sup> While this value exceeds 4.00, it is just an estimation of the upper limit for the Co valence.

Previous publications on oxygen-deficient perovskites suggest that incorporating oxygen vacancies can promote the OER electrocatalysis.<sup>30,39,40</sup> For instance, A-site Ladeficient La<sub>0.95</sub>FeO<sub>3- $\delta$ </sub> was reported with an increased number of oxygen vacancies as compared to the stoichiometric LaFeO<sub>3</sub>,<sup>39</sup> showing a ~6-fold enhancement in the OER intrinsic activity under the conventional adsorbate evolution mechanism (AEM).<sup>14</sup> In another work, Sr substitution for La in the La<sub>1-x</sub>Sr<sub>x</sub>CoO<sub>3- $\delta$ </sub> series significantly boosted the OER reaction kinetics, and the SrCoO<sub>3- $\delta$ </sub> sample with the highest Sr content possessed the largest oxygen vacancy content and exhibited the best OER activity, which is likely associated with the functioning of a novel lattice-oxygen mediated mechanism (LOM).<sup>40</sup> In contrast to the AEM pathway where the OER takes place primarily on the surface metal site,<sup>14</sup> the LOM mechanism involves the lattice oxygen as an additional active site.<sup>40</sup> Later research further suggests that the extent to which the lattice oxygen participates in the OER is related to the oxygen-ion diffusivity, the higher the oxygen-ion diffusivity, the higher the oxygen vacancy

concentration is critical to the enhanced OER activity of *c*-BCF relative to *h*-BCF. Furthermore, *c*-BCF with a crystal symmetry higher than *h*-BCF is expected to offer faster oxygen-ion mobility and thus facilitate the proceeding of the OER under the LOM reaction scheme.<sup>41</sup>

In addition, the reduced Co oxidation state may also be beneficial to the OER. For perovskites utilizing the AEM mechanism, those that contain transition metal with a suitable  $e_g$  orbital filling number near unity were reported to show optimum OER reactivity, as exemplified by the BSCF perovskite (with a valence of ~2.8 and an  $e_g$  filling of ~1.2 for Co).<sup>14</sup> Based on the assumption that Co in both *h*-BCF and *c*-BCF is in an intermediate spin state, the  $e_g$  occupancy can be estimated from the Co valence to be 0–0.4 for *h*-BCF and 1–1.4 for *c*-BCF, with the latter closer to unity. This approximation suggests that under the AEM scheme, the reduced Co valence in *c*-BCF is more favorable to the OER.

It should be noted that strictly speaking, the determination of the real spin state of the Co cation in these perovskites would require experimental inputs from spectroscopic tools such as X-ray absorption spectroscopy (XAS) and Mössbauer spectroscopy.<sup>42,43</sup> The advantageous role of reduced Co valence for the OER is also supported by two recent studies based on the BSCF catalyst: one modifies BSCF by compositing with reductive carbon and the other by altering the synthetic approach,<sup>18,19</sup> both leading to a lower Co oxidation state and a higher OER performance. In another report, nanosized BSCF was prepared by a flame spray method,<sup>20</sup> which stabilized the Co cation at an even lower valence between 2.13 and 2.38, estimated from the oxygen vacancy of  $\sim 0.75$  utilizing a similar approximation demonstrated in **Table 6.2**. Interestingly, the LOM mechanism is likely operative during the OER on this nanosized BSCF, leading to growth of an oxy(hydroxide) surface layer with high activity, as evidenced by operando XAS measurements.<sup>20</sup> The dynamic generation of the OER-active surface layer is favored by the large quantity of oxygen vacancy, which is generated due to the essential role of the reduced Co valence.<sup>20</sup> While whether the surface of *c*-BCF can undergo a similar reconstruction remains to be an open question, it is believed that the reduced oxidation state of Co is likely to aid the complex OER process.

As the electrochemical reaction occurs mostly near the catalyst surface, X-ray photoelectron spectroscopy (XPS) was performed to probe the surface chemical state

of the samples. **Figure 6.7** compares the XPS spectra of *h*-BCF and *c*-BCF. Due to an overlap between the Co 2p and Ba 3d core levels at the binding energies of about 780 eV for Co  $2p_{3/2}$  and Ba  $3d_{5/2}$  and about 795 eV for Co  $2p_{1/2}$  and Ba  $3d_{3/2}$ ,<sup>44</sup> a quantitative analysis of the Co valence appears to be quite challenging. However, a shift of the doublet to lower binding energies can be found for the *c*-BCF sample compared to *h*-BCF, which according to previous literature,<sup>45,46</sup> may indicate a decrease in the surface Co valence.



Figure 6.7 XPS spectra of the Co 2p and Ba 3d core levels for *h*-BCF and *c*-BCF.

The above discussion suggests that an increase in the oxygen vacancy amount and a decrease in the Co valence, which accompany the phase transition from *h*-BCF to *c*-BCF, may collectively account for the improved OER activity. The observation that compared to the BSCF perovskite, *c*-BCF with a higher oxygen vacancy concentration and a smaller Co valence exhibited a better OER intrinsic activity (**Table 6.1**) may further support this conclusion. It should be noted that while the other transition metal, Fe, could also undergo a reduction after the phase transition, this effect contributes insignificantly to the overall OER electrocatalysis. On the one hand, compared to Co,

Fe in general is less OER-active and constitutes a much smaller fraction of the B-site.<sup>47</sup> On the other hand, tetravalent  $Fe^{4+}$  is often more active than trivalent  $Fe^{3+}$  when incorporated in perovskites,<sup>36,39</sup> although the  $Fe^{4+}$ -to- $Fe^{3+}$  reduction may be more difficult to occur than the Co<sup>4+</sup>-to-Co<sup>3+</sup> reduction.<sup>48</sup>

# 6.4 Conclusions

In conclusion, cubic-structured *c*-BCF was stabilized by reducing hexagonalstructured *h*-BCF in an inert atmosphere at elevated temperatures. The hexagonal-tocubic phase transformation resulted in both a reduction in Co valence and an increase in oxygen vacancy concentration, which contributed to a 20-fold rise in the OER intrinsic activity in alkaline solutions. Importantly, *c*-BCF turned out to be one of the most active perovskite-type electrocatalysts reported till date, comparing favorably to the state-of-the-art perovskites while surpassing the noble metal-based standards. Additionally, *c*-BCF also presented good electrocatalytic stability. These results suggest that the unusually stabilized, cubic-structured *c*-BCF perovskite has the promise for accelerating the electrochemical water splitting kinetics. A next step would be to thoroughly investigate the reaction mechanism by which *c*-BCF catalyzes the OER.

## 6.5 References

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# **Chapter 7 Alkali-metal-doped perovskites for efficient oxygen evolution in alkaline solutions**

# 7.1 Abstract

Perovskite oxides are widely researched as the oxygen evolution reaction (OER) electrocatalysts in alkaline water splitting, due to their cost-effectiveness and high activity. To date, the majority of research concentrates on Co-containing perovskites and a range of highly efficient perovskite catalysts have been developed by applying a simple cation doping strategy. This work reports a doping strategy rarely adopted previously, that is alkali-metal doping. By selecting Fe-containing LaFeO<sub>3</sub> as the model catalyst, aliovalent Na<sup>+</sup> was partially doped into the A-site to replace the La<sup>3+</sup>. While the alkali-metal incorporation did not alter the orthorhombic phase structure, it did lead to changes in the perovskite electronic structure, including an increased Fe oxidation state, an enhanced Fe–O covalency, and an enlarged oxygen vacancy concentration. These changes were further found to promote the OER activity of the Fe-based perovskites, with La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta}$ </sub> (*x* = 0.1) showing a ~90-mV drop in the overpotential to afford a current density of 10 mA cm<sup>-2</sup><sub>geo</sub> and a 8-fold growth in the intrinsic activity. These results suggest that the alkali-metal doping could open up a new avenue for the design of efficient perovskite OER catalysts.

#### 7.2 Introduction

The electrochemical water splitting represents a clean pathway to the production of high-purity hydrogen (H<sub>2</sub>) for powering our planet without carbon emissions into the environment. While the electrolysis of water appears to be a quite simple reaction (H<sub>2</sub>O  $\rightarrow 1/2O_2 + H_2$ ), it does not proceed at its thermodynamic voltage (1.229 V) and requires additional energy input to occur at appreciable rates.<sup>1</sup> Most of this extra energy is used to overcome the large energy barriers of the two half-reactions involved, of which the anodic oxygen evolution reaction (OER), a complex multistep four-electron process also referred to as water oxidation, accounts for a major share.<sup>2</sup> To drive the OER more efficiently, noble metal-based materials, for example, those containing iridium (Ir) and ruthenium (Ru), have been demonstrated with one of the best catalytic activities.<sup>3</sup> Unfortunately, as these noble metals are scarce in natural resources and high in cost,<sup>4</sup> their practical use is largely limited. Therefore, alternative electrocatalysts that are made of Earth-abundant elements and have competitive catalytic capability are highly desirable.

During the past years, a multitude of candidate materials have been screened for catalyzing the OER in alkaline media (40 $H^- \rightarrow O_2 + 2H_2O + 4e^-$ ), among which nonprecious-metal-based perovskite oxides have attracted increasing research attention.<sup>5,6</sup> Having a general chemical formula of ABO<sub>3</sub> (A is often a rare-earth or alkaline-earth metal, B is a transition metal, and O is oxygen), perovskite oxides can offer a high degree of freedom in cation arrangement, allowing the incorporation of foreign elements into both the A- and B-sites. For example, the multi-cation perovskite Ba<sub>0.5</sub>Sr<sub>0.5</sub>Co<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3- $\delta$ </sub> (BSCF) was reported with an excellent intrinsic activity more than two orders of magnitude higher than that of iridium dioxide (IrO<sub>2</sub>).<sup>7</sup> Based on molecular orbital principles, the high intrinsic activity of BSCF is rationalized by the electronic state of the major active Co component which has a suitable near-unity eg filling number  $(e_g^{-1.2})$ , leading to an optimized binding with the oxygen intermediates under the conventional adsorbate evolution mechanism scheme.<sup>7</sup> In addition, substitution of Sr for La in La<sub>1-x</sub>Sr<sub>x</sub>CoO<sub>3- $\delta$ </sub> perovskites contributed to a significant increase in the OER reactivity, due to an increased number of oxygen vacancy in parallel with an enhanced Co-O covalency, which likely promotes the activation of oxygen anions in the perovskite lattice to participate in the OER through a so-called lattice-oxygen mediated mechanism.<sup>8</sup>

Despite these advances, most of the research efforts are focused on perovskite oxides that contain Co as the primary active center and La/Ba/Sr as the partner cations.<sup>7-10</sup> To further increase activity, transition metal Fe, which has a much higher abundance than Co in the Earth's crust, is often doped into the Co-based perovskite electrocatalysts.<sup>11-</sup>

<sup>13</sup> A recent study reveals that Fe serves a major role of stabilizing the Co-based perovskite structure without formation of any impurity oxide phase.<sup>14</sup> However, much less attention is directed to Fe-based perovskite oxides for catalyzing the OER, due likely to their insufficient activity and unsatisfactory stability.<sup>15-17</sup> It was reported that silicon doping at the B-site of SrFeO<sub>3-δ</sub> could lead to a threefold increase in OER reactivity, but the stability was not good enough.<sup>15</sup> Such instability is related to the amorphization of the catalyst surface after OER measurements, as suggested by Han et al.'s work on the Sr<sub>x</sub>Ca<sub>1-x</sub>FeO<sub>3-δ</sub> series.<sup>16</sup> Shao and coworkers reported that A-site Sr doping in LaFeO<sub>3</sub> could increase the OER activity, which, however, still degraded to some extent after a continuous cycling test.<sup>17</sup>

In this work, a new strategy based on alkali-metal doping was utilized to increase the OER performance of perovskite catalysts. As a proof-of-concept, the iron-based LaFeO<sub>3</sub> was selected as the host perovskite and sodium (Na), which has an ionic radius similar to that of La,<sup>18</sup> was chosen as the alkali-metal dopant. The Na substitution was found to modify the electronic structure of the perovskites, leading to a more oxidized Fe state and an increased number of oxygen vacancy, while maintaining the crystalline structure, as described by the following equation:

$$LaFe^{3+}O_{3} + xNa^{+} - xLa^{3+} \rightarrow La_{1-x}Na_{x}Fe^{3+}{}_{1-y}Fe^{4+}{}_{y}O_{3-\delta} + \delta/2O_{2}$$
(1)

In the meantime, the Fe–O covalency was also enhanced to some extent. Such electronic modulation substantially facilitated the OER kinetics, with the optimized sample  $La_{0.9}Na_{0.1}FeO_{3-\delta}$  showing both enhanced activity and stability (i.e., an overpotential of 421 mV at 10 mA cm<sup>-2</sup><sub>geo</sub>, a small Tafel slope of 61 mV dec<sup>-1</sup>, and a stable operation at 5 mA cm<sup>-2</sup><sub>geo</sub> for 10 hours).

# 7.3 Results and discussion

## 7.3.1 Formation and characterizations of Na-doped perovskites

Alkali-metal-doped lanthanum ferrites (La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub>, *x* = 0, 0.05, 0.1, and 0.2) were prepared by a modified sol–gel process with a reduced calcination temperature for phase formation.<sup>19</sup> With the increase of the Na dopant amount, the as-prepared samples

show a gradual color change from yellow to brownish (**Figure 7.1**), which is a direct evidence for the successful incorporation of sodium into the perovskite lattice. As sodium may experience partial volatilization under high-temperature conditions,<sup>20</sup> it is likely that the stoichiometries of the as-synthesized samples can deviate from the intended ones. To evaluate this issue, inductively coupled plasma-optical emission spectrometry (ICP-OES) was carried out to analyze the bulk composition of a select sample, La<sub>0.8</sub>Na<sub>0.2</sub>FeO<sub>3- $\delta$ </sub> (*x* = 0.2), and an atomic ratio of 0.80:0.21:1.00 was obtained for La/Na/Fe. This suggests that sodium volatilization is very much unlikely during the synthesis of Na-doped perovskites, which is not unexpected given the relatively low temperature used for phase formation, i.e., 600 °C vs. 800 °C or even higher.<sup>6,21</sup>



**Figure 7.1** Photographs of  $La_{1-x}Na_xFeO_{3-\delta}$  (x = 0, 0.05, 0.1, and 0.2) powders dispersed in absolute ethanol. The dispersions were prepared by ultrasonicating a mixture of about 6 mg of the perovskite oxide and 3 ml of absolute ethanol for a duration of 5 min.

The formation of Na-substituted perovskites was further corroborated by X-ray diffraction (XRD) studies. As illustrated in **Figure 7.2a**, the samples doped with Na<sup>+</sup> exhibit a similar phase structure to that of the pristine LaFeO<sub>3</sub>, all having a pure orthorhombic structure (space group: *Pnma*) which aligns with the standard pattern of ICDD PDF No. 01-088-0641.<sup>22</sup> In addition, as more La<sup>3+</sup> was replaced by Na<sup>+</sup> (with *x* in La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> ranging from 0.05 to 0.2), a slight shift to higher 2 $\theta$  angles was

observed for the main diffraction peaks (**Figure 7.2b**), indicative of a lattice shrinkage. This observation suggests that the B-site Fe cation is likely to be partially oxidized from 3+ to 4+ (with an ionic radius of 0.645 Å and 0.585 Å, respectively) after Nadoping, because should the Fe oxidation state remain unchanged then a lattice expansion would be expected due to the larger size of Na<sup>+</sup> than La<sup>3+</sup> (1.39 Å vs. 1.36 Å).<sup>18</sup>



**Figure 7.2** XRD data of La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> (x = 0, 0.05, 0.1, and 0.2). (a) XRD data presented in a broad  $2\theta$  range of 20–80°. (b) XRD data presented in a select  $2\theta$  range of 31.5–33.5°.

When the Na-doping level was further increased to 30% (x = 0.3), impurity peaks, associated with a Fe<sub>2</sub>O<sub>3</sub> phase and some unidentified phases,<sup>23</sup> began to appear, as seen in **Figure 7.3**. To avoid any possible interference caused by the effect of impurity phases, the following investigations were carried out using samples with a Na doping range of  $0 \le x \le 0.2$ , i.e., samples having nominal compositions of La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> (x = 0, 0.05, 0.1, and 0.2).



**Figure 7.3** XRD pattern of the sample La<sub>0.7</sub>Na<sub>0.3</sub>FeO<sub>3- $\delta$ </sub> (*x* = 0.3) with an excessive Na doping amount. The asterisk indicates a phase likely of Fe<sub>2</sub>O<sub>3</sub>, whereas the question marks indicate unknown phase(s).

High-resolution transmission electron microscopy (HRTEM) was also used to examine the crystalline structure information. **Figure 7.4** displays the HRTEM images of the undoped LaFeO<sub>3</sub> and the Na-doped La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub>, both captured with the electron beam in the direction of the [ $\overline{111}$ ] zone axis. A similar lattice spacing of 0.39 nm was observed for both structures, in good accord with the (101) plane of the orthorhombic-structured perovskites. It should be noted that while a variation in the (101) interplanar spacing should exist between LaFeO<sub>3</sub> and La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub>, as previously suggested by the XRD analysis, such variation is not large enough to be differentiated by the HRTEM technique. **Figure 7.4** insets show the corresponding fast Fourier transform (FFT) patterns, which are characteristic of the orthorhombic phase structure. Further, **Figure 7.5** displays HRTEM images of La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> recorded in another two different zone axes, i.e., [ $31\overline{1}$ ] and [ $1\overline{21}$ ], providing

additional support to the formation of an orthorhombic perovskite structure after the incorporation of Na into LaFeO<sub>3</sub>.



**Figure 7.4** HRTEM images of La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> (x = 0 and 0.1) in the [ $\overline{111}$ ] zone axis. (a) LaFeO<sub>3</sub> (x = 0). (b) La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> (x = 0.1). The insets show the corresponding FFT patterns.



**Figure 7.5** HRTEM images of La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> (*x* = 0.1) in another two zone axes. (a) In the [311] zone axis. (b) In the [121] zone axis. The insets show the corresponding FFT patterns.

The morphology of the La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> series was revealed by scanning electron microscopy (SEM) observations. As depicted in **Figure 7.6**, all the samples possess

similar morphological features, with chunks of varying sizes from several hundred nanometers to a few micrometers. A closer look at the SEM images (Figure 7.6b, d, f, h) suggests that each large chunk is made of particles of a much smaller size. This is more obviously noticed in the high-angle annular dark-field scanning TEM (HAADF-STEM) imaging of the sample La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> (Figure 7.7a), where nanoparticles in the scale of approximately 30–60 nm agglomerated into larger aggregates. Figure 7.7b shows the energy-dispersive X-ray spectroscopy (EDS) mapping images, which indicate that the Na dopant, along with other constituent elements, was homogeneously distributed within the perovskite framework.



Figure 7.6 SEM images of  $La_{1-x}Na_xFeO_{3-\delta}$  (x = 0, 0.05, 0.1, and 0.2) at two different magnifications. (a–b)  $LaFeO_3$ . (c–d)  $La_{0.95}Na_{0.05}FeO_{3-\delta}$ . (e–f)  $La_{0.9}Na_{0.1}FeO_{3-\delta}$ . (g–h)  $La_{0.8}Na_{0.2}FeO_{3-\delta}$ .



**Figure 7.7** HAADF-STEM image and the corresponding EDS mapping images of La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-δ</sub>. (a) HAADF-STEM image. (b) EDS mapping images of La, Na, Fe, and O elements.

The similarity in the samples' morphology was also validated by their analogous Brunauer–Emmett–Teller (BET) surface areas ( $S_{\text{BET}}$ ), ranging from 11.7 m<sup>2</sup> g<sup>-1</sup> to 16.9 m<sup>2</sup> g<sup>-1</sup>, as determined by nitrogen adsorption-desorption measurements. However, it should be noted that with the introduction of the Na dopant, the surface areas become somewhat smaller, due likely to the fact that the nanoparticles were sintered to a larger extent for doped samples than for the undoped LaFeO<sub>3</sub> (Figure 7.6b, d, f, h). Figure 7.8 presents the nitrogen sorption isotherms for  $La_{1-x}Na_xFeO_{3-\delta}$  (x = 0, 0.05, 0.1, and 0.2), which can be categorized into the Type V isotherms, suggesting the existence of mesopores.<sup>24</sup> The mesoporous structure is also discernible from the SEM and STEM images (Figure 7.6 and 7.7). It is worth mentioning that compared to perovskites prepared from a similar sol-gel method, for instance, BSCF ( $S_{BET} < 2 \text{ m}^2 \text{ g}^{-1}$ ),<sup>25,26</sup> the Na-doped lanthanum ferrites reported here have much larger surface areas ( $S_{\text{BET}} > 10$  $m^2 g^{-1}$ ), which is associated with the nature of the lanthanum-containing samples as well as the reduced calcination temperature during synthesis.<sup>21,27</sup> Overall, the high surface areas as well as the presence of porous structure can increase the amount and accessibility of active sites and are thus expected to facilitate the electrocatalytic oxygen evolution.



**Figure 7.8** Nitrogen adsorption-desorption isotherms of  $La_{1-x}Na_xFeO_{3-\delta}$  (x = 0, 0.05, 0.1, and 0.2). (a) LaFeO<sub>3</sub>. (b) La<sub>0.95</sub>Na<sub>0.05</sub>FeO<sub>3-\delta</sub>. (c) La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-\delta</sub>. (d) La<sub>0.8</sub>Na<sub>0.2</sub>FeO<sub>3-\delta</sub>.

### 7.3.2 Electrocatalytic oxygen evolution performance

The electrochemical measurements were performed in an electrolyte of 0.1 M KOH saturated with oxygen under ambient conditions. The OER activity was assessed by running cyclic voltammetry (CV) experiments at a slow scan rate of 10 mV s<sup>-1</sup>, with the working electrode being held at 2000 revolutions per minute (rpm) to efficiently prevent the accumulation of the O<sub>2</sub> bubbles generated. To eliminate the effects from the capacitive current and the electrolyte resistance, the CV data were taken average and then corrected for *iR* drop to allow the reporting of the OER kinetic current,<sup>7,9</sup> as exemplified by the data processing of the sample La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> (**Figure 7.9**).



**Figure 7.9** An example of the processing of the electrochemical CV data of  $La_{0.9}Na_{0.1}FeO_{3-\delta}$  to allow the reporting of the OER kinetic current.

**Figure 7.10a** shows the kinetic currents normalized by the geometric area of the working electrode, from which it is clearly seen that compared with the pristine LaFeO<sub>3</sub>, all the Na-doped samples required reduced (over)potentials to deliver a certain current output, indicating improved apparent activity toward the OER. This becomes more obvious when comparison is made in regard to the overpotential to reach a 10 mA cm<sup>-2</sup><sub>geo</sub> current density ( $\eta_{10}$ ), a solar-fuel production related metric that is often used for benchmarking different OER catalysts.<sup>28</sup> As presented in **Figure** 

**7.10b**, LaFeO<sub>3</sub> gives a  $\eta_{10}$  value of 512 mV, in consistency with previous reports.<sup>23</sup> By comparison, La<sub>0.95</sub>Na<sub>0.05</sub>FeO<sub>3- $\delta$ </sub>, La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub>, and La<sub>0.8</sub>Na<sub>0.2</sub>FeO<sub>3- $\delta$ </sub> show considerably reduced  $\eta_{10}$  values of 449, 421, and 464 mV, respectively, with La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> demonstrating the highest apparent activity.



**Figure 7.10** Electrocatalytic performance of La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> (x = 0, 0.05, 0.1, and 0.2) toward the oxygen evolution reaction in a 0.1 M KOH electrolyte. (a) OER kinetic current. The arrow indicates a decreasing trend in the potential required to produce a current density of 10 mA cm<sup>-2</sup><sub>geo</sub>. (b) A comparison of the overpotential required to reach 10 mA cm<sup>-2</sup><sub>geo</sub>. (c) Tafel plot where the OER current is normalized by the catalyst surface areas to obtain the specific activity. (d) A comparison of the specific activity at an overpotential of 400 mV.

It is generally acknowledged that the apparent activity is strongly associated with the catalyst surface area, that is, a higher surface area often means a larger number of active sites and thus greater apparent activity.<sup>29</sup> Therefore, to allow for the comparison of the intrinsic activity, the OER kinetic current was also normalized by the catalysts' BET surface areas to obtain specific activity, which has been recommended as a viable

means to represent the intrinsic activity for oxide electrocatalysts.<sup>7,30</sup> **Figure 7.10c** shows the logarithm of specific activity versus the potential, a figure also known as the Tafel plot. Still, all the Na-substituted samples exhibit improved intrinsic activity than the pristine LaFeO<sub>3</sub> does, as evidenced by a larger specific activity at a given (over)potential. Notably, at a 400 mV overpotential, the best-performing sample La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> delivers a specific activity almost one order of magnitude larger than that of LaFeO<sub>3</sub> (0.16 vs. 0.02 mA cm<sup>-2</sup><sub>oxide</sub>), implying its significantly enhanced OER activity (**Figure 7.10d**). In addition, La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> has a smallest Tafel slope (61 mV dec<sup>-1</sup>) among all the samples, further suggesting its increased OER kinetics. These results indicate that the Na substitution for La in La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub> facilitates the proceeding of the electrocatalytic water oxidation and that a suitable level of substitution (i.e., *x* = 0.1) can lead to the best electrocatalytic activity.



**Figure 7.11** Electrochemical stability of LaFeO<sub>3</sub> and La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> recorded by chronopotentiometry tests at a steady current density of 5 mA cm<sup>-2</sup><sub>geo</sub>.

It is of equal importance to appraise the capability for catalysts to sustain prolonged oxidation of water. To address this, the electrochemical stability was characterized by chronopotentiometry during which the electrode was held at a steady current density of 5 mA cm<sub>geo</sub><sup>-2</sup>. As displayed in **Figure 7.11**, the pristine LaFeO<sub>3</sub> quickly lost its activity during the first four-hour test, whereas La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> was able to maintain a rather stable performance for ten hours. This observation suggests that Na incorporation in the LaFeO<sub>3</sub> lattice is also beneficial to the electrochemical stability.

# 7.3.3 Understanding the enhancement in catalytic performance

Understanding the origins of the improved OER activity facilitated by A-site alkalimetal substitution can provide guidelines for the development of improved electrocatalysts. Generally, the pristine LaFeO<sub>3</sub> has a Fe nominal valence of 3+. Once a proportion of trivalent La<sup>3+</sup> is replaced by monovalent Na<sup>+</sup>, the Fe valence would increase to compensate for any likely charge imbalance triggered by the doping and in the meantime oxygen vacancy may be generated to further maintain the charge balance. As shown in **Figure 7.12a**, a pair of 2p doublet, i.e.,  $2p_{3/2}$  at the binding energy (BE) of ~710.2 and  $2p_{1/2}$  at the BE of ~723.9 eV, along with a satellite peak at the BE of ~718.3 eV, was observed for the X-ray photoelectron spectroscopy (XPS) spectrum of the undoped LaFeO<sub>3</sub>, in agreement with the dominance of Fe<sup>3+</sup>.<sup>31</sup> The doublet for the Fe 2p XPS spectrum of La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-δ</sub> was found to shift slightly to more positive BE positions, indicating a partial oxidation of the Fe species.

The change in the Fe electronic state is also verified by the soft X-ray absorption spectra (XAS) at the O K-edge, a highly sensitive technique that can reflect the extent to which the transition metal state hybridizes with the oxygen state in oxide compounds.<sup>32,33</sup> As displayed in Figure 7.12b, when Na was introduced into the LaFeO3 lattice, a pre-edge peak at the photon energy of ~528 eV was detected. This feature, as also found in the divalent alkaline-earth metal-doped La<sub>1-x</sub> $A_x$ FeO<sub>3- $\delta$ </sub> series (A = Ca or Sr),<sup>34-36</sup> indicates an increased mixing between the Fe 3d state and O 2p state and thus an enhanced Fe 3d–O 2p covalency, which is associated with the partial oxidation from Fe<sup>3+</sup> to Fe<sup>4+</sup>. These modifications in the transition-metal valence and transition metal-oxygen covalency are likely beneficial to the OER electrocatalysis. On the one hand, considering that the Fe cations in unsubstituted and substituted LaFeO<sub>3</sub> generally adopt a high spin state at room temperature,<sup>36</sup> the Fe<sup>4+</sup> cation has a preferable electronic configuration of  $t_{2g}^3 e_g^1$  compared to that of Fe<sup>3+</sup> (with a  $t_{2g}^3 e_g^2$ configuration). According to Shao-Horn et al.'s guiding principle, perovskites with transition metal cations having a near-unity eg occupancy can lead to optimum OER activity in alkaline solutions.<sup>7</sup> From this perspective, the Na-substituted La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-δ</sub> with an eg<sup>1</sup> configuration for a fraction of the Fe<sup>4+</sup> species is expected to show improved OER activity than the unsubstituted LaFeO<sub>3</sub> where the Fe<sup>3+</sup> cation is dominant. On the other hand, the enhanced Fe 3d–O 2p covalency can promote the OER kinetics. A previous report suggests that Fe doping in LaCo<sub>1-x</sub>Fe<sub>x</sub>O<sub>3</sub> increased the Co–O hybridization, which brings about improved OER currents.<sup>13</sup> In another research, Sr substitution enhanced the Co–O covalency in the La<sub>1-x</sub>Sr<sub>x</sub>CoO<sub>3-δ</sub> perovskites, which activated the lattice-oxygen in participating in the OER and thus led to significantly increased OER activity.<sup>8</sup> While whether lattice-oxygen participation in the Na-substituted La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3-δ</sub> is possible remains to be testified, the enhanced Fe 3d–O 2p covalency in La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-δ</sub> relative to that of LaFeO<sub>3</sub> likely accounts for the increased activity. In addition, the quadruple perovskite CaCu<sub>3</sub>Fe<sub>4</sub>O<sub>12</sub> with Fe at the tetravalent state was reported with both high activity and stability, due to the Fe<sup>4+</sup>-based covalent bonding network.<sup>37</sup> The enhanced electrochemical stability of the Na-doped La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-δ</sub> may also be related with the enhanced Fe–O covalency.



**Figure 7.12** Electronic states of LaFeO<sub>3</sub> and La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> as characterized by XPS and XAS. (a) Fe 2p XPS spectra. (b) O *K*-edge XAS spectra. (c–d) O 1s XPS spectra.

The presence of oxygen vacancy is supported by the XPS analysis of the O 1s core level. **Figure 7.12 c** and **d** demonstrate the O 1s XPS spectra of LaFeO<sub>3</sub> and La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub>, respectively. Based on previous literature,<sup>19,38</sup> these spectra can be fitted by four major components, namely lattice oxygen (O<sup>2-</sup>) at the BE of ~529 eV, highly oxidative oxygen (O<sub>2</sub><sup>2-</sup>/O<sup>-</sup>) at the BE of ~531 eV, hydroxide or adsorbed oxygen (OH<sup>-</sup>/O<sub>2</sub>) at the BE of ~532 eV, and adsorbed water (H<sub>2</sub>O) at the BE of ~534 eV. As seen from the detailed fitting results shown in **Table 7.1**, a much larger presence of O<sub>2</sub><sup>2-</sup>/O<sup>-</sup> was observed on La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub> than on LaFeO<sub>3</sub>, indicating a higher concentration of the surface oxygen vacancy.<sup>39</sup> Earlier studies have revealed that creating oxygen vacancies on metal oxide surfaces can effectively boost the OER electrocatalysis.<sup>8,9,23,40</sup> It is reasonable to believe that the increased amount of defective oxygen, as induced by the Na incorporation, is another parameter crucial to the improved OER catalysis over La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub>.

Catalyst	O <sup>2-</sup>		O <sub>2</sub> <sup>2-</sup> /O <sup>-</sup>		OH <sup>-</sup> /O <sub>2</sub>		H <sub>2</sub> O	
	BE (eV)	Content	BE (eV)	Content (%)	BE (eV)	Content (%)	BE (eV)	Content
LaFeO <sub>3</sub>	529.2	52.9	531.0	23.7	532.0	17.0	533.4	6.4
La <sub>0.9</sub> Na <sub>0.1</sub> FeO <sub>3-</sub> δ	528.9	17.3	530.5	42.7	532.5	34.9	534.4	5.1

**Table 7.1** XPS peak fitting results of the O 1s core level of LaFeO<sub>3</sub> and La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub>.

### 7.4 Conclusions

To conclude, a series of alkali-metal-doped perovskites  $La_{1-x}Na_xFeO_{3-\delta}$  (x = 0, 0.05, 0.1, and 0.2) were prepared by partially substituting Na for La at the A-site of LaFeO<sub>3</sub> and assessed as the catalytic materials for the water oxidation in alkaline electrolytes. The introduction of alkali-metal dopant did not alter the orthorhombic phase structure but did modify the electronic structure to some extent by oxidizing the Fe species,

enhancing the Fe–O covalency, and increasing the oxygen vacancy concentration. This electronic modulation was found to substantially promote the OER performance, as evidenced by the sample with a suitable level of Na-doping (i.e., La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3- $\delta$ </sub>) which shows an optimum performance with an overpotential of 421 mV at 10 mA cm<sup>-2</sup><sub>geo</sub>, a small Tafel slope of 61 mV dec<sup>-1</sup>, and a stable operation at 5 mA cm<sup>-2</sup><sub>geo</sub> for 10 hours. The results from this research could shed light to the development of other types of electrocatalyst materials by means of alkali-metal doping.

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# **Chapter 8 Conclusions and perspectives**

# 8.1 Conclusions

In this thesis, a range of new perovskite-type oxide materials made of non-precious transition metals Mo, Co, and Fe are designed, synthesized, characterized, and evaluated as the electrocatalysts for facilitating the reaction kinetics of the watersplitting half-reactions, i.e., the hydrogen evolution reaction (HER) at the cathode and the oxygen evolution reaction (OER) at the anode. These perovskite oxides are prepared using facile chemical methods such as high-temperature reduction and solgel process. Their physicochemical properties are investigated using a set of diffraction, microscopy, and spectroscopy characterizations including X-ray diffraction, scanning electron microscopy, transmission electron microscopy, X-ray photoelectron spectroscopy, X-ray absorption spectroscopy, and Raman spectroscopy, as well as a number of testing or analysis methods such as N<sub>2</sub> sorption measurements, inductively coupled plasma-optical emission spectrometry, thermogravimetric and differential scanning calorimetry analysis, oxygen temperature-programmed desorption, and electrical conductivity measurement. The electrocatalytic performance is evaluated in a rotating disk electrode-based, three-electrode setup using electrochemical techniques ranging from cyclic voltammetry, linear sweep voltammetry, to chronopotentiometry. By fine-tuning the chemical compositions and structures, perovskite oxides with improved HER/OER catalytic performance are developed. More importantly, correlations are established between the electrocatalytic activity and the perovskite electronic structure (e.g., crystal symmetry, transition metal oxidation state, oxygen vacancy, and metal-oxygen covalency). Overall, these studies are expected to offer a deepened understanding of the structure–activity relationship of the perovskite oxide electrocatalysts. The general conclusions derived from each study are also summarized as the following.

# **8.1.1** From scheelite BaMoO<sub>4</sub> to perovskite BaMoO<sub>3</sub>: Enhanced electrocatalysis toward the hydrogen evolution in alkaline media

- A Mo-based BaMoO<sub>3</sub> perovskite oxide was synthesized by reducing the BaMoO<sub>4</sub> scheelite oxide under a reductive H<sub>2</sub> atmosphere at elevated temperatures.
- Compared to scheelite BaMoO<sub>4</sub>, perovskite BaMoO<sub>3</sub> showed significantly higher catalytic activity toward the alkaline HER, with the overpotential to

afford a current density of  $-10 \text{ mA cm}_{geo}^{-2}$  lowered by more than 200 mV and the intrinsic activity at the select overpotentials of 350–450 mV increased by about one order of magnitude.

• The improved HER activity is due to the intrinsically higher activity of the interconnected MoO<sub>6</sub> octahedra in the cubic-structured BaMoO<sub>3</sub> perovskite as compared to the disconnected MoO<sub>4</sub> tetrahedra in the tetragonal-structured BaMoO<sub>4</sub> scheelite. The former offers a reduced Mo oxidation state, an increased number of surface oxygen vacancies, and a larger electrical conductivity.

# **8.1.2** Fe-based perovskites for catalyzing the hydrogen evolution reaction in alkaline solutions

- A series of Fe-based La<sub>1-x</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>x</sub>FeO<sub>3-δ</sub> (x = 0.0, 0.2, 0.5, 0.8, and 1.0) perovskites were obtained by simultaneously substituting the alkaline-earth metals Ba and Sr for the rare-earth metal La at the A-site of LaFeO<sub>3</sub>. The substitution leads to a phase transition from orthorhombic to cubic.
- The substituted samples all exhibited enhanced alkaline HER activity compared to the pristine LaFeO<sub>3</sub>, with the best activity observed on La<sub>0.2</sub>(Ba<sub>0.5</sub>Sr<sub>0.5</sub>)<sub>0.8</sub>FeO<sub>3- $\delta$ </sub> (x = 0.8) showing a 216-mV drop in the overpotential to afford a current density of -10 mA cm<sup>-2</sup><sub>geo</sub>. This activity compares favorably to that of many of the other reported perovskite-type HER catalysts.
- A comprehensive X-ray spectroscopic study suggests that the enhanced HER activity is related to the increased oxidation state of the Fe cation and the enhanced covalency of the Fe–O bond, which is closely associated with the phase change induced by Ba/Sr co-doping.

# **8.1.3** An unusually stabilized Co-based perovskite for highly efficient oxygen evolution

- A cubic-structured perovskite (BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3-δ2</sub>, denoted as *c*-BCF) was prepared through the thermal reduction of a hexagonal-structured perovskite (BaCo<sub>0.7</sub>Fe<sub>0.3</sub>O<sub>3-δ1</sub>, denoted as *h*-BCF) under an inert atmosphere.
- This unusually stabilized *c*-BCF perovskite exhibited a twenty times higher OER intrinsic activity relative to the pristine *h*-BCF. *c*-BCF also outperforms many of the state-of-the-art perovskites and noble metal-based benchmark catalysts. Additionally, *c*-BCF presented good electrocatalytic stability.

• The substantial increase in the OER activity is closely related to the stabilized cubic perovskite structure, which provides a significantly reduced Co valence as well as a greatly enhanced oxygen vacancy concentration.

# **8.1.4** Alkali-metal-doped perovskites for efficient oxygen evolution in alkaline solutions

- A series of alkali-metal-doped perovskites La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3-δ</sub> (x = 0, 0.05, 0.1, and 0.2) were prepared by replacing a proportion of rare-earth metal La with alkali metal Na at the A-site of LaFeO<sub>3</sub>. The introduction of alkali-metal dopant did not alter the orthorhombic phase structure.
- The Na-doped samples all displayed enhanced OER activity compared to the pristine LaFeO<sub>3</sub>, with the highest activity observed on La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-δ</sub> (x = 0.1) showing a ~90-mV reduction in the overpotential to afford a current density of 10 mA cm<sup>-2</sup><sub>geo</sub> and a 8-fold increase in the intrinsic activity. La<sub>0.9</sub>Na<sub>0.1</sub>FeO<sub>3-δ</sub> also exhibited improved electrocatalytic stability compared to LaFeO<sub>3</sub>.
- The incorporation of low-valent Na cation into the LaFeO<sub>3</sub> perovskite caused a partially oxidized Fe state, an enhanced Fe–O covalency, and an increased oxygen vacancy content, which are responsible for the enhanced OER activity observed.

# 8.2 Perspectives

Despite the results obtained in this thesis, there is much that can be done to further our understanding in the water-splitting reactions catalyzed by perovskite oxides. In this section personal perspectives are provided as an effort to underline some important areas of research interest in the future.

# 8.2.1 From bulk-sized to nanosized perovskite electrocatalysts

Most of the studies in this thesis are focused on perovskite oxides having a particle size in the (sub-)micron scale. As the electrode activity (i.e., based on the current per electrode surface area) is strongly correlated with the catalyst surface area, developing nanosized perovskite oxides appears to be a promising approach to further increasing catalytic activity. One way to attain nanoscale perovskites is through lowering the calcination temperature in conventional synthesis. For example, in the case of La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3- $\delta$ </sub>, a heating temperature as low as 600 °C was used to produce

perovskites with specific surface area larger than 10 m<sup>2</sup> g<sup>-1</sup>, in contrast to La<sub>1-</sub>  $_x(Ba_{0.5}Sr_{0.5})_xFeO_{3-\delta}$  calcined at a higher temperature of 1100 °C showing surface area smaller than 5 m<sup>2</sup> g<sup>-1</sup>. However, this method has its own limitations. On the one hand, it may only apply to perovskites comprising mainly lanthanides at the A-site which can crystallize at a relatively low temperature,<sup>1,2</sup> whereas alkaline-earth metalcontaining perovskites often require a much higher temperature for phase formation.<sup>3,4</sup> On the other hand, while this method can produce nanosized particles, these particles are prone to agglomerate into larger aggregates (as observed for La<sub>1-x</sub>Na<sub>x</sub>FeO<sub>3-\delta</sub>), which is not beneficial to the electrocatalysis.

Alternatively, the downsizing of perovskite catalysts can be achieved by adopting other chemical synthesis methodologies, such as precipitation method, template-assisted synthesis, and electrospinning, to name a few.<sup>5</sup> With nanosized perovskites, it remains interesting to delve into the size effect on electrocatalysis. For instance, LaCoO<sub>3</sub> with a particle size below 100 nm was found to exhibit a more favorable eg orbital filling compared to that observed in the bulk form of LaCoO<sub>3</sub>, thus leading to an enhanced intrinsic activity.<sup>1</sup> The change in the Co electronic configuration was likely due to the presence of a surface spin-state transition which occurred for smaller-sized LaCoO<sub>3</sub> nanoparticles.<sup>1</sup>

### 8.2.2 From ex-situ characterizations to in-situ/operando analysis

This thesis has correlated the electrocatalytic HER/OER performance collected from electrochemical measurements with the perovskite oxide properties gathered *ex situ* from physicochemical characterizations. A further step to understand the structure–activity relationship is through the utilization of *in-situ*/operando techniques, which can probe real-time changes over the perovskite catalysts during water electrolysis. The *in-situ*/operando analysis is useful in that it could provide a better picture of the real active sites operative in the perovskite electrocatalysts. For example, nanosized Ba<sub>0.5</sub>Sr<sub>0.5</sub>Co<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3-δ</sub> (BSCF) perovskite was found to dynamically self-reconstruct at the surface region during the OER in alkaline solutions, forming an active layer made of (oxy)hydroxide which was proposed to be the real catalytic site.<sup>6</sup> Additionally, studies utilizing *in-situ*/operando characterizations can facilitate a better understanding of the stability of perovskite electrocatalysts under operating conditions,<sup>7</sup> which is critical to the design of both active and stable perovskite catalysts. Currently, a great many *in-situ*/operando techniques have been employed in water-splitting related

electrocatalysis, such as X-ray absorption spectroscopy, X-ray photoelectron spectroscopy, Mössbauer spectroscopy, and transmission electron microscopy, which can provide information about the crystal structure, metal oxidation state, and coordination environment of the catalysts of interest.<sup>8</sup> Very often, collaboration is needed to conduct electrocatalysis research using *in-situ*/operando tools.

## 8.2.3 From fundamental research to practical applications

This thesis provides fundamental understanding of the structure-activity relationship of the perovskite oxide electrocatalysts and proposes materials design strategies toward the development of new perovskite oxides with improved electrocatalytic HER/OER activity. From the perspective of applied research, the as-developed perovskite catalysts are expected to be evaluated for overall water splitting based on practical water electrolyzers. Most of the current research evaluates the overall water splitting performance of an electrocatalyst in a single-chamber electrochemical cell.<sup>9,10</sup> While this practice could allow the assessment of a potential catalyst for water electrolysis, it cannot begin to compare with the conduct involved in real-world water electrolysis. A more realistic configuration for this purpose would be one that is based on the membrane electrode assembly (MEA). Another comment is that practical water splitting operates at a temperature higher than ambient temperature (e.g., around 80 °C) to achieve enhanced kinetics, which in turn places higher requirement on the catalyst stability. A recent report demonstrated that a MEA made of nanosized BSCF perovskite could steadily operate at 50 °C and 200 mA cm<sup>-2</sup> for 5 h, requiring a voltage much lower than that made of the noble metal IrO<sub>2</sub> catalyst.<sup>6</sup> While this appears promising, there remains much to be done to realize the water electrolysis over perovskite electrocatalysts with improved efficiency and for extended durations.

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# Appendix A From scheelite BaMoO<sub>4</sub> to perovskite BaMoO<sub>3</sub>: Enhanced electrocatalysis toward the hydrogen evolution in alkaline media

**Supplementary Information for Chapter 4** 

# A.1 Supplementary figures



Figure A.1 Rietveld refinement analysis of the XRD patterns of (a) BaMoO<sub>4</sub>

scheelite and (b) BaMoO<sub>3</sub> perovskite.



Figure A.2 XPS survey spectra of BaMoO<sub>4</sub> scheelite and BaMoO<sub>3</sub> perovskite.



**Figure A.3** HAADF-STEM image of BaMoO<sub>3</sub> perovskite and the corresponding EDS mapping images of Ba, Mo, and O.



**Figure A.4** SEM images of the commercial molybdenum oxides showing their bulk particle size. (a) MoO<sub>3</sub>, (b) MoO<sub>2</sub>.



Figure A.5 LSV curves of the commercial molybdenum oxides MoO3 and MoO2.



Figure A.6 Tafel plots of the commercial molybdenum oxides MoO<sub>3</sub> and MoO<sub>2</sub>.

# A.2 Supplementary tables

 Table A.1 Rietveld refinement results of the XRD patterns of the as-prepared

Catalyst	Phase composition	Phase structure	Space group	Lattice parameters (Å)	$\chi^2$	Rp (%)	Rwp (%)
BaMoO4	BaMoO <sub>4</sub>	Tetragonal	<i>I</i> 4 <sub>1</sub> / <i>a</i>	a = 5.58234(3)	2 420	7.99	10.37
	(100.0 wt%)	Tettagonai		c = 12.8219(1)	2.420		
BaMoO <sub>3</sub>	BaMoO <sub>3</sub>	Cubic	Pm <del>3</del> m	<i>a</i> = 4.04103(2)	2.560	8.35	10.59
	(97.5 wt%)	Cubie					
	Mo	Cubic	Im <del>3</del> m	<i>a</i> = 3.1468(2)			
	(2.5 wt%)	Cubic					

BaMoO<sub>4</sub> scheelite and BaMoO<sub>3</sub> perovskite.

**Table A.2** A comparison of the HER activity of BaMoO<sub>4</sub> scheelite and BaMoO<sub>3</sub> perovskite with other bulk-sized, Mo-containing catalysts (e.g., Mo oxide and sulfide) and perovskite catalysts (e.g., Mn-, Fe-, Co-, and Ni-based) tested in 1 M KOH.

Catalyst	Substrate	Loading (mg <sub>catalyst</sub> cm <sup>-2</sup> )	Catalyst/carb on mass ratio	$\eta_{10}{}^a$ (mV)	Tafel slope $(mV dec^{-1})$	Ref.
BaMoO <sub>3</sub>	$\mathrm{GCE}^b$	0.253	No carbon	336	110	This work
BaMoO <sub>4</sub>	GCE	0.253	No carbon	561	189	This work
MoO <sub>2</sub>	GCE	0.253	No carbon	465	113	This work
MoO <sub>3</sub>	GCE	0.253	No carbon	530	148	This work
MoO <sub>2</sub>	$CPE^{c}$	$N.A.^d$	N.A.	~440	N.A.	[1]
MoO <sub>3</sub>	CPE	N.A.	N.A.	~660	N.A.	[1]
$MoS_2$	GCE	0.159	5:1	349	109	[2]
$MoS_2$	GCE	2.8	No carbon	~360	153	[3]
$MoS_2$	GCE	0.204	No carbon	370	124	[4]
$NdBaMn_2O_{5.5+\delta}$	GCE	0.4	1:1	~500	138	[5]
$Nd_{0.5}Ba_{0.5}MnO_{3-\delta}$	GCE	0.4	1:1	~610	132	[5]
$Sr_2Fe_{1.5}Mo_{0.5}O_{6^{-\delta}}$	GCE	0.234	4:1	443	105	[6]
$LaFeO_{3-\delta}$	GCE	0.232	1:1	~480	140	[7]
$LaFe_{0.8}Co_{0.2}O_{3\!-\!\delta}$	GCE	0.232	1:1	~400	113	[7]
$SrCoO_{3-\delta}$	CP <sup>e</sup>	1	10:1	447	157	[8]
$SrCo_{0.9}Nb_{0.1}O_{3^{-\delta}}$	СР	1	10:1	427	142	[8]
$SrCo_{0.7}Fe_{0.3}O_{3-\delta}$	GCE	0.362	1:1	378	190	[9]
$Ba_{0.5}Sr_{0.5}Co_{0.8}Fe_{0.2}O_{3^{-\delta}}$	GCE	0.232	1:1	342	75	[10]
$La_{0.5}Sr_{0.5}CoO_{3-\delta}$	GCE	0.385	No carbon	~420	95	[11]
$PrBa_{0.5}Sr_{0.5}Co_2O_{5+\delta}$	GCE	0.226	4:1	393	101	[12]
$\begin{array}{c} Ba_{0.95}Co_{0.4}Fe_{0.4}Zr_{0.1}Y_{0.1}\\ O_{3-\delta}\end{array}$	GCE	0.255	5:1	360	80	[13]
$La_{0.8}Sr_{0.2}Cr_{0.69}Ni_{0.31}O_{3-\delta}$	GCE	0.401	1:1	447	116	[14]

<sup>*a*</sup> The overpotential required to reach a current density of 10 mA  $cm_{geo}^{-2}$ .

<sup>b</sup> Glassy carbon electrode.

<sup>*c*</sup> Carbon-paste electrode.

<sup>*d*</sup> Not available.

<sup>e</sup> Carbon paper.

	Specific activity at select overpotentials (mA $cm_{oxide}^{-2}$ )					
Catalyst	0.35 V	0.40 V	0.45 V			
BaMoO <sub>4</sub>	0.56	0.80	1.41			
BaMoO <sub>3</sub>	4.52	12.98	37.19			

**Table A.3** A comparison of the HER specific activity of BaMoO<sub>4</sub> scheelite and BaMoO<sub>3</sub> perovskite at select overpotentials.

**Table A.4** XPS peak fitting results of the O 1s core levels of BaMoO4 scheelite andBaMoO3 perovskite.

Catalyst	Lattice oxygen		Defective oxygen		Chemisorbed oxygen	
	Binding energy (eV)	Concentrat ion (%)	Binding energy (eV)	Concentrat ion (%)	Binding energy (eV)	Concentrat ion (%)
BaMoO <sub>4</sub>	530.1	79.2	531.1	15.5	532.4	5.3
BaMoO <sub>3</sub>	530.0	53.3	531.5	27.3	533.0	19.4
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